

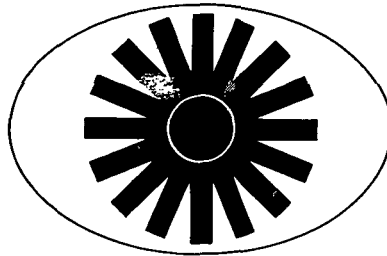
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ANALYTICAL STUDY OF STRIATED NOZZLE FLOW  
WITH SMALL RADIUS OF CURVATURE RATIO THROATS

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by

DAVID J. NORTON AND ROBERT E. WHITE



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**TEES**

TEXAS ENGINEERING EXPERIMENT STATION  
TEXAS A & M UNIVERSITY  
COLLEGE STATION TEXAS 77843

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by

David J. Norton, Principal  
Investigator and Assistant Professor  
of Aerospace Engineering

and

Robert E. White Research Assistant  
of Aerospace Engineering

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Texas A&M University  
Texas Engineering Experiment Station  
Space Technology Division

## FORWARD

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## SUMMARY

An analytical method has been developed which is capable of estimating the chamber and throat conditions in a nozzle with a low radius of curvature throat. The method has been programmed using standard FORTRAN IV language and includes chemical equilibrium calculation subprograms (modified NASA Lewis program CEC71) as an integral part. Program CEC71 is described in Reference 1. The method determines detailed and gross rocket motor characteristics in the presence of striated flows and gives detailed results for the motor chamber and throat plane with as many as 20 discrete zones. The method employs a simultaneous solution of the mass, momentum, and energy equations and allows propellant types, O/F ratios, propellant distribution, nozzle geometry, and injection schemes to be varied so to predict spatial velocity, density, pressure, and other thermodynamic variable distributions in the chamber as well as the throat. Results for small radius of curvature (down to  $R_C/R_T=.25$ ) have shown good comparison to experimental results. Both gaseous and liquid injection may be considered with frozen or equilibrium flow calculations. For parametric studies it is also possible to elect frozen flow with calorically perfect gases in order to conserve computational time. In this case it is possible to study the effects of complete mixing compared to striated flow.

## INTRODUCTION

### Objective

The objective of this study has been to develop a computer program for determining the performance of rocket engines in the presence of striated flows and small radius of curvature throats and to perform parametric studies to determine the influence of engine parameters on mass flow rate, specific impulse, and chamber pressure. The program has been equipped with subprograms (a modified form of CEC71 computer program of Reference 1) to determine the thermochemical composition for steady, inviscid flow in discrete zones. The program has the capability of analyzing the chamber flow field for specified injector schemes with gaseous or liquid propellant injection and of analyzing the inviscid, transonic throat plane flow field. Predictions are made of the chamber operating conditions and the spatial distribution of velocity and thermodynamic variables for the reactants and products of combustion. Parameters which are considered for studies include the propellant types (especially gaseous  $O_2$  and  $H_2$ ), O/F ratios, propellant mass distributions, nozzle geometry, and injection schemes. Approximate two dimensional performance parameters at the throat plane are determined and compared to one dimensional performance results. The philosophy used to develop this computer program is discussed in Appendix A.

## Considerations and Assumptions

In small rocket motors heat transfer can be significant in terms of engine efficiency as well as thermal protection requirements. One method of reducing heat transfer is to reduce the heat transfer coefficient. This can sometimes be accomplished by laminarization of the boundary layer by using a highly convergent subsonic section of a nozzle. Experimental work<sup>2,3</sup> has shown that there is a tendency with a rapidly converging subsonic section to stabilize the boundary layer as a result of the rapid acceleration of the working fluid. This tendency toward laminarization of the boundary layer through the transonic throat region may be continued by employing a low throat radius of curvature ratio throat. In addition to the effect of reducing the heat transfer a decrease in nozzle surface area can be achieved. Further reductions in overall heat transfer to the nozzle walls may be effected by use of barrier cooling. By surrounding the hot core flow with fuel or oxidizer rich flow, temperature gradients to the motor walls are reduced thus the heat transfer is reduced. Striating therefore permits maximum temperature in the core zone and yet permits near maximum overall specific impulse.

In the treatment of striated flow with throat radius of curvature effects no closed form relationship exists between the chamber pressure and the mass flow. This is due to variations of total enthalpy and velocity in the chamber because of striation, as well as, radial pressure gradients at the physical throat due to radius of curvature effects. Thus choking with a given throat radius can only be assured and the flow parameters determined with a coupled solution of the throat and the chamber.

Even for unstriated nozzle flow the solution for the two dimensional flow field with small radius of curvature ratio throats is difficult and time consuming<sup>4</sup>. With inclusion of striation the problem becomes more complex and determination of performance parameters for a parametric analysis may require considerable machine computations. Radial velocities at the physical throat plane are thus assumed to be small and the throat is a revolved circular arc section. Figures 1a and 1b present the flow regime of interest in which mass, momentum, and energy are conserved along streamlines. This analysis is for inviscid, compressible, axially symmetric flow. Each annular flow zone is assumed to flow isentropically after leaving the chamber and satisfy conservation equations of mass and momentum at the throat. Losses are limited to curvature and striation effects and to the degree of equilibrium flow attained (kinetic or energy conversion losses). The energy conversion losses are dependent on the degree of freezing considered for the solution and is restricted to limiting cases. In this analysis it was not necessary to average the mass flow nor to require the isentropic coefficient to be constant in a flow zone or stream tube at the throat.

The chamber static pressure is the pressure at which chamber combustion occurs. This pressure is used for thermochemical calculations for each flow zone. In calculating an individual flow zone total temperature the difference between the kinetic energies of the burned gas and the injected reactants in the chamber zone is not considered since the difference is small compared to the overall energy of the material in the combustion zone. Thus, even for low contraction ratios the stagnation temperature in a flow zone determined with the chamber static pressure differs very little from the exact chamber total temperature for the zone.

## THEORY

### 1.0 Chamber Solutions

The chamber solution depends on the method of mass generation and on the properties of the injected and combustion materials. To obtain choked conditions at the throat one may have to alter the chamber combustion static pressure or the total mass flow and recalculate throat plane parameters. By this technique the coupling is maintained between the chamber solution and the throat plane solution. By multiple iteration the complete solution can be made to simultaneously satisfy chamber and throat requirements.

For a discrete number of stream tube zones as shown in Figure 1a, the mass, momentum, and energy equations for one dimensional, inviscid, compressible flow are:

$$\begin{aligned} \rho_{I_{fu_i}} w_{I_{fu_i}} A_{I_{fu_i}} + \rho_{I_{ox_i}} w_{I_{ox_i}} A_{I_{ox_i}} &= \dot{m}_{I_{fu_i}} + \dot{m}_{I_{ox_i}} = \dot{m}_i \\ &= \rho_{g_i} w_{g_i} A_{g_i} \end{aligned} \quad (1.1)$$

$$\dot{m}_{I_{fu_i}} w_{I_{fu_i}} + \dot{m}_{I_{ox_i}} w_{I_{ox_i}} + A_{g_i} P_I = P_g A_{g_i} + \dot{m}_i w_{g_i} \quad (1.2)$$

$$H_{o_{I_i}} = H_{o_{g_i}} = h_{g_i} + w_{g_i}^2/2 \quad (1.3)$$

where

$$h_{g_i} = \int_{T_o}^{T_{g_i}} c_{p_{g_i}} dT + h_{g_i}^o$$

In addition, it is necessary that

$$\sum A_{g_i} = A_c \quad (1.4)$$

$$\dot{m}_{I_{ox_i}} = (O/F)_i \dot{m}_{I_{fu_i}} \quad (1.5)$$

Further, if the injected propellants are gaseous and perfect gases are assumed

$$\rho_{I_{fu_i}} = P_I / [R_{I_{fu_i}} T_{I_{fu_i}}] \quad (1.6)$$

and

$$\rho_{I_{ox_i}} = P_I / [R_{I_{ox_i}} T_{I_{ox_i}}] \quad (1.7)$$

For a constant chamber static pressure, the propellant distribution in each zone is specified as the fraction of the total mass flow. This case is of interest when it is necessary to compare engine performance at a fixed pressure. The total mass flow is determined by iteration and is not known apriori. An initial estimation of the total mass flow or an adjustment by iteration of the total mass flow permits intermediate calculations and allows determination of parameters in the chamber. Thus, iteration between the chamber solution and the throat plane solution drives the intermediate results to the solution values of parameters. An analysis with a constant chamber static pressure is a practical mode to consider for parametric studies since the chamber static pressure, propellant reactants inputs, and O/F in each zone, once specified, do not change results of chemical equilibrium calculations for the mass flow adjustments required to determine the solution. The solution being that for the chamber and

the throat plane with a specified throat radius of curvature. Equations (1.1) through (1.4) provide a system of equations to which the unknowns  $T_{g_i}$ ,  $W_{g_i}$ ,  $A_{g_i}$  and  $P_I$  may be determined.

For specified mass flow in each zone, there exists a chamber static pressure which simultaneously satisfies Equations (1.1) through (1.4). By application of the governing equations at the throat plane, the throat radius determined is the prescribed throat radius. For this scheme of mass generation, chemical equilibrium calculations would be required at each iteration step. Initial estimates of thermodynamic variables are altered once to provide data for intermediate calculations and a final solution.

For specified injector reservoir pressures, injection equations for mass generation due to the reservoir pressure for the fuel mass flow injected into each zone is determined by

$$\dot{m}_{I_{fu_i}} = C_{D_{I_i}} A_{I_{fu_i}} [2\rho_{I_{fu_i}} (P_{R_{fu_i}} - P_I)]^{1/2} \quad (1.8)$$

and thus

$$\dot{m}_i = \dot{m}_{I_{fu_i}} (1 + O/F_i) \quad (1.9)$$

and

$$\dot{m}_{I_{ox_i}} = \dot{m}_i - \dot{m}_{I_{fu_i}} \quad (1.10)$$

This scheme is limited in the program by the requirement that injector **fuel** areas are required to be specified. Intermediate results are determined by a double iteration since the injector pressure,  $P_I$ , is also determined within the chamber solution iteration loop. Equation (1.8) is not strictly

applicable to gaseous injection but is operational for liquid or gas injection in the computer program .

For cases where frozen, calorically perfect flow is considered, a solution for fully mixed flow may be included. The results give a limiting case for comparison to striated flow. Appropriate thermodynamic and flow variables may be calculated as follows:

$$C_{p_{g_{mix}}} = \sum C_{p_{g_i}} \dot{m}_i / \dot{m}_{total} \quad (1.11)$$

$$MW_{g_{mix}} = 1 / \sum \frac{\dot{m}_i}{\dot{m}_{total} MW_{g_i}} \quad (1.12)$$

$$R_{g_{mix}} = R_{g_c} / MW_{g_{mix}} \quad (1.13)$$

$$\gamma_{g_{mix}} = C_{p_{g_{mix}}} / (C_{p_{g_{mix}}} - R_{g_{mix}}) \quad (1.14)$$

$$T_{o_{g_{mix}}} = \frac{\sum C_{p_{g_i}} T_{o_{g_i}} \dot{m}_i}{C_{p_{g_{mix}}} \dot{m}_{total}} \quad (1.15)$$

Conservation of energy for this case requires

$$C_{p_{g_{mix}}} T_{o_{g_{mix}}} = h_{g_{mix}} + w_{g_{mix}}^2 / 2 \quad (1.16)$$

but

$$\begin{aligned} h_{g_{mix}} &= C_{p_{g_{mix}}} T_{g_{mix}} = C_{p_{g_{mix}}} \frac{P_{g_{mix}}}{\rho_{g_{mix}} R_{g_{mix}}} \\ &= C_{p_{g_{mix}}} \frac{P_{g_{mix}} w_{g_{mix}} A_g}{\dot{m}_{total} R_{g_{mix}}} \end{aligned} \quad (1.17)$$



so

$$C_{p_{g_{mix}}} T_{o_{g_{mix}}} = C_{p_{g_{mix}}} \frac{P_{g_{mix}} w_{g_{mix}} A_g}{\dot{m}_{total} R_{g_{mix}}} + w_{g_{mix}}^2 / 2 \quad (1.18)$$

Conservation of momentum requires

$$P_{g_{mix}} A_g + \dot{m}_{total} w_{g_{mix}} = P_g A_g + \sum \dot{m}_i w_{g_i} \quad (1.19)$$

or

$$P_{g_{mix}} = P_g + \frac{\sum \dot{m}_i w_{g_i}}{A_g} - \frac{\dot{m}_{total} w_{g_{mix}}}{A_g} \quad (1.20)$$

Elimination of  $P_{g_{mix}}$  from Equation (1.18) with Equation (1.20) gives a

quadratic in  $w_{g_{mix}}$ . Equation (1.20) gives  $P_{g_{mix}}$  and  $\rho_{g_{mix}}$  may be

determined by

$$\rho_{g_{mix}} = \dot{m}_{total} / A_g w_{g_{mix}} \quad (1.21)$$

Also,

$$P_{o_{g_{mix}}} = P_{g_{mix}} \left( \frac{T_{o_{g_{mix}}}}{T_{g_{mix}}} \right)^{\frac{\gamma_{g_{mix}}}{\gamma_{g_{mix}} - 1}} \quad (1.22)$$

If only one zone of gas flow for a low temperature or nonreacting gas is the subject of investigation, a simplified calculation option in the program may be used. Injector details are not determined and thermochemical data are input as opposed to determined by chemical equilibrium calculations.

The energy equation, mass equation, and equation of state are simultaneously solved. By elimination of the injector pressure,  $P_I$ , from the list of unknowns, the momentum equation is not required. This option in the program serves to predict radius of curvature effects at the throat plane for low temperature single zone gas flow.

## 2.0 Throat Solution

The properties of the combustor flow field are determined with the combustion chamber calculations prior to the throat solution. Initially, estimates are made followed by iterative corrections until the converged solution results for desired fixed parameters. The momentum and mass equations describe the flow at the throat. These equations together with the requirement that energy be conserved in stream tubes defines the flow. A schematic representation of the geometry of a typical nozzle throat is given in Figure 1b.

The radial momentum equation is:

$$\partial P / \partial r = - \rho [u \partial u / \partial r + w \partial u / \partial z - v^2 / r] \quad (2.1)$$

Considering the throat plane, we expect that the radial velocity will be small everywhere since it must be zero at the throat wall and at the nozzle centerline. Thus, for axially symmetric flow

$$dP/dr = -\rho w \, du/dz \quad (2.2)$$

Since  $dr/dz = u/w$ , then on the throat plane between the circular arc throat wall and the centerline

$$dP/dr = -\rho w^2 d^2 r/dz^2 = -\rho w^2/R \quad (2.3)$$

In the above equation  $R$  refers to the radius of curvature of the streamlines at the throat. The energy equation applied at the throat where  $u = 0$  requires

$$w^2 = 2(H_o - h) \quad (2.4)$$

For frozen, calorically perfect flow, the isentropic coefficient,  $\gamma$ , is constant in each stream tube and it is convenient to express the enthalpy in stream tubes as:

$$h = \frac{\gamma}{\gamma-1} [P]^\gamma [C]^{1/\gamma} \quad (2.5)$$

Where the constant  $C$  for each stream tube is defined by the isentropic process equation as:

$$C = C(\psi) = P/[p]^\gamma \quad (2.6)$$

The equation for mass conservation is:

$$d\psi/dr = \dot{dm}/dr \left( 1/\dot{m}_{total} \right) = \frac{2\pi r \rho w}{\dot{m}_{total}} \quad (2.7)$$

Applying Equation (2.4) to Equations (2.3) and (2.7) it can be seen that a set of two nonlinear total differential equations result. The solution of these equations can be obtained at the throat providing  $C$ ,  $H_o$ ,  $\gamma$ ,  $R$  can be specified as a parametric function of  $\psi$ . Of course the variation of  $C$ ,  $H_o$ , and  $\gamma$  with  $\psi$  is known for the current iteration from the chamber solution (at least for frozen, calorically perfect flow: for equilibrium or frozen flow these parameters are determined as a function of

pressure for a given chamber solution). It remains only to specify a relationship for  $R_v$  to close the formulation at the throat plane. It is clear from experimental and analytical studies that the main functional form for  $R_v$  should be  $R_v = R(R_c, R_T, r)$ . This formulation for  $R_v$  neglects effects due to inlet geometry between the chamber and the throat region; however, experimental evidence indicates this to be a minor variation except for contraction section wall slopes near perpendicular to the nozzle axis and/or  $R_c/R_T \approx 0$ .<sup>5,6,7</sup> The appropriate boundary conditions for  $R_v$  regardless of striation effects are:

$$\begin{aligned} R_v &= R_c & \text{at} & \quad r = R_T \\ R_v &= \infty & \text{at} & \quad r = 0 \end{aligned}$$

A plausible form for  $R_v$  which satisfies these conditions is

$$R_v = R_c \left[ \frac{R_T(1 + R_c/r) - r}{R_c} \right]^n \quad (2.8)$$

Figure 2 presents a number of calculations for  $C_D$  with respect to  $R_c/R_T$  for various values of  $n$ . Based on these results a value of  $n = 3/2$  is indicated. The representation chosen for  $R_v$  can be further evaluated by comparing results for the variation of throat plane Mach number with radius. This will be presented later in the report.

Equations (2.3) and (2.7) thus comprise the necessary equations, expressed in a more general form than previously considered<sup>8</sup>, since  $H_0 = H_0(\psi)$ ,  $h = h(P, \psi)$ ,  $\rho = \rho(P, \psi)$ , and  $w = w(H_0, h) = w(P, \psi)$ . In general,  $H_0(\psi)$  is determined from chamber conditions and is calculated before equations at the throat are solved. If required,  $C(\psi)$  is also determined from chamber conditions. Throat plane variables are determined so that the throat radius

which just chokes the flow must be the prescribed radius. An iteration between the chamber solution and the throat plane solution allows starting estimations to be corrected to assure the final iteration predicts choked flow for the desired geometry and fixed parameters. For simultaneous solution of the throat plane equations, Hamming's prediction-corrector technique<sup>9</sup> was employed. This method proved to be efficient and stable and is initiated with the Range-Kutta method so to be self starting.

### 3.0 Performance Solution

Two types of performance calculations are made. The first type includes the effects of throat radius of curvature and striation. The total mass flow is given by

$$\dot{m}_{total} = \sum \dot{m}_i \quad (3.1)$$

The throat vacuum specific impulse is determined by integrating the velocity and pressure profiles across the throat plane so that

$$I_{sp_{vac}} = \int_{r=0}^{r=R_T} w d\psi + \int_{r=0}^{r=R_T} P dA / \dot{m}_{total} \quad (3.2)$$

The characteristic velocity is

$$c^* = \frac{A_T \sum \left\{ \dot{m}_i P_{o_i} / \dot{m}_{total} \right\}}{\dot{m}_{total}} \quad (3.3)$$

Within the program, intergrations are actually represented as finite summations based on the fraction of the mass or area over which the required thermodynamic variable is representative. In Equation (3.2) the velocity at a point on the throat plane is assigned a mass fraction determined by adjacent values of  $\psi$  and pressure is assigned the area over which it is

representative. Small independent variable step sizes input to the program permit the integration approximation technique used to be accurate.

For comparison, the second type of performance calculations are based on the ideal or optimum distribution of Mach number uniformly equal to one on the throat plane. Although this distribution does not in general occur for one dimensional striated flow<sup>8</sup>, it serves as a limit to which striated flow with radius of curvature effects may be compared. If frozen, calorically perfect flow is considered, the one dimensional mass flow is:

$$\dot{m}_{total\ 1-D} = \sum A_i^* P_{o_{g_i}} (r_{g_i}^t / T_{o_{g_i}})^{1/2} \quad (3.4)$$

where

$$r_{g_i}^t = \frac{\gamma_{g_i}}{R_{g_i}} \left[ \frac{2}{\gamma_{g_i} + 1} \right] \frac{\gamma_{g_i} + 1}{\gamma_{g_i} - 1} \quad (3.5)$$

If frozen or equilibrium flow is considered, the one dimensional mass flow is determined by

$$\dot{m}_{total} = \sum A_i^* P_g / c^*_{1-D_i} \quad (3.6)$$

where  $c^*_{1-D_i}$  is determined by the chemical equilibrium calculations and is based on  $P_g$ .  $A_i^*$  in either case is determined by the throat solution and is the area of a particular flow zone on the throat plane. In a similar manner the one dimensional vacuum specific impulse at the throat is

$$I_{sp\ vac\ 1-D} = \frac{\sum \frac{\dot{m}_i}{\dot{m}_{total}} \left[ \gamma_{g_i} R_{g_i} \frac{T_{o_{g_i}}}{(T_o/T_i)_{1-D}} \right]^{1/2} + \sum P_{o_{g_i}} (P_i/P_{o_{g_i}})_{1-D} A_i^*}{\dot{m}_{total\ 1-D}} \quad (3.7)$$

where

$$(T_{o_{g_i}}/T_i)_{1-D} \equiv \frac{1 + \gamma_{g_i}}{2} \quad (3.8)$$

and

$$(P_i/P_{o_{g_i}})_{1-D} \equiv P_{o_{g_i}} \left[ T_i/T_{o_{g_i}} \right]^{\frac{\gamma_{g_i}}{\gamma_{g_i}-1}} \quad (3.9)$$

for frozen, calorically perfect flow. For frozen or equilibrium flow

$$I_{sp_{vac}1-D} = \sum I_{sp_{vac}}' \dot{m}_i/\dot{m}_{total} \quad (3.10)$$

where  $I_{sp_{vac}}'$  is determined by the chemical equilibrium calculations.

The characteristic velocity for one dimensional calculations is

$$c_{1-D}^* = \frac{A_T \sum (\dot{m}_i/\dot{m}_{total}) (P_{o_{g_i}})}{\dot{m}_{total1-D}} \quad (3.11)$$

#### 4.0 Chamber and Throat Iteration Techniques

A chamber solution iteration is necessary to assure that  $P_I$ ,  $A_{g_i}$ ,  $T_{g_i}$ , and  $w_{g_i}$  satisfy conservation equations. The injector pressure,  $P_I$ , converges after an initial estimate is made by the program. The iteration equation employed is as follows:

$$P_I = P_g + (P_I - P_g) \left( \frac{\sum A_{g_i}^2}{A_C} \right) \quad (4.1)$$

A double iteration was employed to determine  $T_{g_i}$ ,  $A_{g_i}$ , and  $w_{g_i}$ . This technique employs a simultaneous solution of the energy, mass, and momentum equations with the assumed value of  $P_I$  as initially estimated or, after the first chamber solution iteration loop is completed, as determined by

Equation (4.1). Convergence is achieved after the above procedure is complete and the following is determined to be true

$$\sum A_{g_i} = A_C \quad (4.2)$$

The injector pressure,  $P_I$ , is the pressure at each injector surface in the chamber and is the same for each zone. Within the program  $P_I$  is a dimensioned variable and is identical with the variable PIAVG. If convergence fails for some reason, variables  $P_g$ , PIAVG,  $\sum A_{g_i}$ , and  $A_C$  are printed in an error message. Convergence difficulties may be encountered for a single zone of flow of low temperature or non reacting gas. (This is because  $w_g$  becomes large for this case). Special subroutine SPPG has been provided in the program to avoid convergence difficulties should they occur for the above mentioned single zone flow case.

To initiate the throat plane solution an estimate of the centerline pressure is required. The estimation is based on a small perturbation method<sup>10</sup>

$$P_{CL} = P_{o_{g_1}} \left[ \frac{2}{\gamma_{g_1} + 1} \right]^{\frac{\gamma_{g_1}}{\gamma_{g_1} - 1}} \left( 1 + \frac{1}{\frac{4}{\gamma_{g_1}} \frac{R_c}{R_T + 1}} \right) \quad (4.3)$$

With the initial estimate, throat equations are integrated by Hamming's method<sup>9</sup> to determine the throat wall radius corresponding to  $\psi = 1.0$ .

The pressure,  $P_{CL}$ , given by Equation (4.3) is increased and a new wall radius is determined by integration. Following this,  $dr_w/dP_{CL}$  is used to alter  $P_{CL}$  until the minimum radius is determined. The iteration process by which  $dr_w/dP_{CL} = 0$  is sought requires that  $dP_{CL}$  be sufficiently small and that



$r_{w_{min}} = R_T$ . Only seven iterations are permitted by the program once  $r_{w_{min}}$  is bracketed. A convergence message is provided by the program if seven iterations are not sufficient; however, calculations are not halted but proceed to alter  $P_g$  or  $\dot{m}_{total}$  such that  $r_{w_{min}} = R_T$ . The minimum wall radius as determined by the above procedure is used to alter the chamber static pressure by

$$P_g = P_g (r_{w_{min}} / R_T)^2 \quad (4.4)$$

for fixed mass flow or fixed reservoir pressure solutions. For fixed chamber static pressure, the total mass flow is altered to obtain  $r_{w_{min}} = R_T$  by

$$\dot{m}_{total} = \dot{m}_{total} (R_T / r_{w_{min}})^2 \quad (4.5)$$

If attempts to determine  $P_g$  or  $\dot{m}_{total}$  for the solution exceed seven, another convergence message is provided and parameters as described in the program output are, nevertheless, determined. Results may be erroneous but sufficient for parametric studies. The most flagrant error occurs if the  $P_{CL}$  estimation is very inaccurate. This error may occur for  $R_C / R_T \lesssim .25$  so are seldom encountered. This usually causes the pressure,  $P$ , to become zero and internally generated messages occur and machine generated messages may occur. Calculations are not necessarily halted and corrections provided in the program may allow the solution to be determined.

## 5.0 Results and Conclusions

In this section equations which were presented under Throat Solution and Performance Solution will be more thoroughly qualified. Results of the present analysis are discussed and where possible compared with experimental data and with other methods of analysis. The analytical form used for the flow radius of curvature at the throat plane is presented and verified by comparison to experimental data. Results of the many options available in the program will not all be presented; however, several typical results will be presented and discussed. Results of parametric studies are presented as well as performance calculation results.

### 5.1 Effect of Radial Velocity at the Throat Plane

Consider an axisymmetric converging-diverging nozzle shown in Figure 2. An element of mass flow,  $\dot{dm}$ , passes through surface  $dl$  inclined to the axis at angle  $\phi$ . The element of mass has velocity  $V$  inclined at angle  $\sigma$  to the nozzle axis and is  $da$  wide. The elemental mass flow is

$$\dot{dm} = 2\pi r \rho V da \quad (5.1)$$

Since

$$da = \sin(\phi - \sigma) dl \quad (5.2)$$

and

$$dl = dr / \sin \phi \quad (5.3)$$

then,

$$\dot{dm} = \frac{2\pi \rho V \sin(\phi - \sigma) r dr}{\sin \phi} \quad (5.4)$$

On the throat plane  $\phi = \pi/2$  so that

$$\dot{m}_{total} = \int_{r=0}^{r=R_T} 2\pi \rho V \cos \sigma r dr \quad (5.5)$$

Thus, the discharge coefficient is

$$C_D = \frac{\int_{r=0}^{r=R_T} 2\pi\rho w \, r dr}{\dot{m}_{total1-D}} \quad (5.6)$$

The effect of radial velocity on mass flow at the throat plane is exhibited in the density as shown by Equation (5.5). For single flow zone of a frozen, calorically perfect gas the density may be written as

$$\rho = \rho_{0g} \left[ 1 - \frac{\gamma_g - 1}{2} \frac{w^2 + u^2}{(\gamma_g R_g T_{0g})^2} \right]^{\frac{1}{\gamma_g - 1}} \quad (5.7)$$

The radial velocity component,  $u$ , may be assumed to be negligible at the throat plane compared to  $w^2$  since  $u = 0$  at  $r = 0$  and at  $r = R_T$ . Using two dimensional methods of Reference 4 this assumption may be verified for nonstriated flow for values of  $R_C/R_T$  down to .35. It is therefore concluded that this assumption will be useful for the present analysis. Recall, however,  $\partial u / \partial z \neq 0$  on the throat plane.

## 5.2 Streamline Radius of Curvature at the Throat Plane

In the discussion of the throat plane solution the radius of curvature of the streamlines was given by Equation (2.8) as

$$R_C = R_C \left[ \frac{R_T(1+R_C/r) - r}{R_C} \right]^n \quad (5.8)$$

This form satisfies the boundary conditions at  $r = 0$  and at  $r = R_T$  for any  $n$  greater than zero. Figure 3 presents calculation results for  $n = 1.0, 1.5$ , and  $2.0$ . Based on these results a value of  $n = 1.5$  is indicated as the appropriate

exponent. In addition, Figure 4 shows good agreement between the present theory throat plane Mach number distribution and experimental data of Reference 5 for  $R_C/R_T = .625$ . Other theories are also shown for comparison. Figure 5 presents the distribution of throat plane static pressure to chamber pressure ratio of the present method. Results compare favorably to the data taken by Cuffel, Back, and Massier.<sup>5</sup>

### 5.3 Results of Analytical Method

The effects of striating mixtures of gaseous hydrogen and oxygen for nozzles with small throat radius of curvature to throat radius ratio having various amounts of individual flow zone mass flow have been investigated. Figure 6 illustrates the dependence of the mass discharge coefficient with respect to the cooling mass flow ratio for  $R_C/R_T = .5$  and  $P_g = 200$  psia. Results are for equilibrium; frozen; frozen, calorically perfect; and frozen, calorically perfect fully mixed flows. Figure 7 shows similar results for  $R_C/R_T = 2.0$ . Figures 6 and 7 indicate that if striation and equilibrium are maintained, an improved discharge coefficient may be obtained. Improvement in discharge coefficient results for equilibrium flow compared to fully mixed flow especially for a large mass of fuel rich cooling. Both Figures 6 and 7 show that little change in discharge coefficient with fraction of cooling mass flow occurs when chamber flow zones burned gases are fully mixed in the chamber.

Figure 8 presents discharge coefficient,  $C_D$ , versus radius of curvature ratio,  $R_C/R_T$ , for various amounts of cooling with unmixed and fully mixed flows. Input thermochemical data used to calculate results shown in Figure 8 for frozen, calorically perfect flow at the throat plane were determined at 50 psia chamber pressure with constant chamber total enthalpy in flow zones. The core and cooling

zones had O/F ratios of 6.0 and 0.5, respectively. As in Figures 6 and 7 striated flow has higher discharge coefficient than uncooled or fully mixed flow for these propellants.

Figure 9 shows the spatial distribution of Mach number and static pressure on the throat plane for  $R_C/R_T = 0.5, 1.0, 2.0$ , and  $10.0$  with four flow zones. The Mach number discontinuities between flow zones appears for all  $R_C/R_T$  resulting in a discharge coefficient less than 1.0. A discharge coefficient of unity may be obtained only for a Mach number at the throat plane uniformly equal to 1.0. This point will be expanded later in this section. It also appears that striation may improve the discharge coefficient. This is verified by the hydrogen and oxygen propellant combinations used to determine Figures 6, 7, and 8.

#### 5.4 Effect of Throat Plane Mach Number Distribution on Discharge Coefficient

Based on Equation (2.3) the axial velocity may be found by

$$w^2 = - \frac{R_g}{\rho} dP/dr \quad (5.9)$$

Since  $u \approx 0$ , the density is  $\rho = \rho(P, \psi)$  and thus mass flow rate given by Equation (5.5) and discharge coefficient given by Equation (5.6) depend on pressure and the radial pressure gradient on the throat plane, on thermochemical parameters of chamber flow zone gases (on  $\psi$ ), and on the flow radius of curvature,  $R$ . For frozen, calorically perfect flow, the mass flow with radius of curvature and striation effects by the present analysis is

$$\dot{m}_{total} = \frac{2\pi}{\sqrt{Q}} \int_{r=0}^{r=R_T} \frac{PM \sqrt{MW} \sqrt{V_Y}}{\sqrt{T}} r dr \quad (5.10)$$

In the present analysis the one dimensional mass flow for frozen, calorically perfect flow was determined by,

$$\dot{m}_{total 1-D} = \frac{\pi R_T^2 / \sqrt{Q}}{\sum_i \left[ \left( \frac{\dot{m}_i}{\dot{m}_{total}} \right) \frac{\sqrt{T_{0g_i}}}{P_{0g_i} \sqrt{M_{Wg_i}} \sqrt{\gamma_{g_i}} \left[ \frac{2}{\gamma_{g_i} + 1} \right]^{(\gamma_{g_i} + 1)/(\gamma_{g_i} - 1)}} \right]} \quad (5.11)$$

Thus, by taking differential elements of radius with associated thermodynamic variables the discharge coefficient may be written as

$$C_D = \left\{ \sum_i \left[ \left( \frac{\dot{m}_i}{\dot{m}_{total}} \right) \frac{\sqrt{T_{0g_i}}}{P_{0g_i} \sqrt{M_{Wg_i}} \sqrt{\gamma_{g_i}} \left( \frac{2}{\gamma_{g_i} + 1} \right)^{(\gamma_{g_i} + 1)/(\gamma_{g_i} - 1)}} \right] \right\} \cdot \left\{ \sum_j \left[ \frac{P_j \sqrt{M_{Wg_j}} \sqrt{\gamma_{g_j}} M_j}{\sqrt{T_j}} \cdot \frac{r_j^2 - r_{j-1}^2}{R_T^2} \right] \right\} \quad (5.12)$$

For unstrained flow considerable simplification results and the discharge coefficient for frozen, calorically perfect isentropic flow is

$$C_D = \frac{2}{R_T^2} \int_{r=0}^{r=R_T} M \left( 1 + \frac{\gamma_{g_1} - 1}{2} M^2 \right)^{-\frac{\gamma_{g_1} + 1}{2(\gamma_{g_1} - 1)}} \left( \frac{\gamma_{g_1} + 1}{2} \right)^{\frac{\gamma_{g_1} + 1}{2(\gamma_{g_1} - 1)}} r \, dr \quad (5.13)$$

In Equation (5.13) the coefficient is one if the Mach number is uniformly equal to one at the throat plane. For all other Mach number distributions consistent with conservation of mass, momentum, and energy the discharge coefficient is less than one.

That the discharge coefficient of striated flows in the presence of small radius of curvature throats tends to be greater than the discharge coefficient of unstriated flow is not necessarily true for all fuel-oxidizer combinations. Figure 10 presents  $R_C/R_T$  versus discharge coefficient examples for comparison. In Figure 10 the hydrogen-oxygen propellant combination with a core  $O/F = 7.0$  and a sheath  $O/F = 0.0$  shows an improved discharge coefficient for 20% striation over unstriated flow. However, for the hydrazine-nitrogen tetroxide combination, which also assumes frozen, calorically perfect flow, the unstriated flow discharge coefficient is greater than the striated flow discharge coefficient. As in Figure 8, Figure 10 employs thermochemical data determined for a chamber static pressure of 200 psia and constant total enthalpy. For Figures 8 and 10 the isentropic exponent in the chamber core flow zone is not equal to the ratio of specific heats. The significant difference between the flows used to calculate results for Figure 10 is that for striated flow using  $N_2H_4$  and  $N_2O_4$  propellant combinations less throat area is required to accommodate  $N_2H_4$  sheath zone mass flux than is required for the  $H_2$  and  $O_2$  propellant combinations using  $H_2$  as a coolant given the same fraction of coolant mass flow to total mass flow.

## 5.5 Parametric Study Results

Extensive parametric studies have consisted of determining the effect on discharge coefficient due to striation and radius of curvature ratio with frozen, calorically perfect flow. By the direct input of thermochemical data and the use of a frozen, calorically perfect flow analysis, particular sets of thermodynamic variables were fixed and used to generate parametric curves with thermodynamic parameter combinations. Ratios of specific heats, stagnation temperatures,

and molecular weights as well as cooling mass flow to total mass flow appear to be the main parameters required to develop a parametric relationship between striated and unstriated flow discharge coefficients for given throat radius of curvature ratio. Studies have yielded no general parameter combination which correlates striated to unstriated flow discharge coefficient without knowledge of the results of the throat plane solution. However, trends have been observed, namely, there is a significant effect of combustion gas ratios of specific heats in striated flow. Stagnation temperatures and molecular weights of the combustion gasses have only a secondary effect on discharge coefficient. Even for unstriated flow there is a difference between discharge coefficients with different ratios of specific heats. Figure 11 shows that discharge coefficient increases with decreasing ratio of specific heats. In Figure 11 the molecular weight and total temperature of the burned gas remained constant for all curves of  $R_c/R_T$  versus  $C_D$ .

## 5.6 Performance Results

The characteristic velocity,  $c^*$ , versus cooling to total mass flow ratio is shown in Figure 12. Curves are for fully mixed and unmixed flow for radius of curvature ratios,  $R_c/R_T$ , equal to 0.5 and 2.0. Under the same flow mixing conditions, i.e. unmixed or fully mixed, and for the same fraction of cooling to total mass flow the characteristic velocity is greater for  $R_c/R_T = 0.5$  than for  $R_c/R_T = 2.0$ . This is due to the decrease in total mass flow at specified chamber pressure for  $R_c/R_T = 0.5$  compared to the total mass flow for  $R_c/R_T = 2.0$ . Recall that

$$c^* = \frac{\pi R_T^2}{\dot{m}_{total}} \sum_i p_{o_i} g_i \left( \dot{m}_i / \dot{m}_{total} \right) \quad (5.14)$$



In Figure 12, fully mixed flow at a given  $R_C/R_T$  has a characteristic velocity greater than unmixed flow for a fixed chamber pressure for the same reason even though total pressure decreases for fully mixed flow from unmixed flow.

Figure 13 presents the characteristic velocity,  $c^*$ , versus cooling to total mass flow ratio. Curves are for two zone striated and two zone, fully mixed flow with  $R_C/R_T = 2.0$ . Also shown is the resulting chamber static pressure,  $P_g$ , which, for this case, was the same for the striated and mixed flow. Note that the static pressure for this engine drops off as the cooling flow is increased. Results for Figure 13 were obtained by calculations with constant reservoir pressures and may not be compared on the same basis with results shown in Figure 12. Figure 12 and Figure 13 do agree, however, in indicating an improved characteristic velocity of mixed flow over striated flow. Results for curves of Figure 13 show a decreasing total mass flow with increasing cooling to total mass flow ratio which agrees with a decreasing chamber static pressure. At the same mass ratio, the total mass flow for striated flow is greater than the total mass flow for fully mixed flow.

## 5.7 Conclusions

The theory presented here permits an extension to an analysis of one dimensional compressible striated nozzle flow. The throat plane solution gives an approximation to two dimensional axisymmetric flow and has successfully been used for analyzing the throat plane in converging-diverging type nozzles with striated flow for throat radius of curvature to throat radius ratios down to .25. The method has been programmed using standard FORTRAN IV and is fully documented in this report. The program is capable of analyzing the nozzle throat plane and rocket motor chamber with frozen, calorically perfect; equilibrium; or frozen striated flows as well as fully mixed frozen, calorically perfect

flow. By coupling the chamber and throat plane solutions, chamber and throat plane spatial distributions of velocity and other thermodynamic parameters are uniquely determined for specified geometry. Several modes of injector description and mass generation are possible with the program.

Results of the program agree favorably with experimental data and results of other computational methods, especially in predicting the mass discharge coefficient. No experimental results are presently available which permit distinct annular zone or striated flow to be compared to results obtained by this method. The dependence of discharge coefficient is primarily on the radial pressure gradient, the adiabatic or isentropic coefficient, and the amount of mass in each flow zone. Radial velocity is insignificant especially if streamlines on the throat plane have radii of curvature centered on the throat plane as proposed by the present analysis.

It can be concluded that results obtained by this method may offer an advantage over other methods by being in agreement with experimental data and by being in agreement with but requiring less computational time than finite difference methods used to obtain the same data. Further, multizone striated flow solutions may be obtained with the program in only seconds of computer time which permits rapid calculation of parametric performance calculations for candidate engine designs.

## DESCRIPTION OF PROGRAM INPUT

Program input information or data consists of six types. Three of the types are required for all problems and three are optional. The optional inputs allow two kinds of problems. The required types consist of the following:

- (a) Comment Cards (two cards)
- (b) Integer control card (program variable name LETOUT)
- (c) Namelist data which includes input parameters and option integers.

The optional input data include (1) thermochemical data for frozen, calorically perfect flow problems input under nameslist EQU or (2 and 3) modified input data to the chemical equilibrium calculations with formats identical to the formats required for the corresponding in NASA program CEC71.<sup>1</sup>

Table I and II are schematics of input cards containing namelist and other input information or variables required for the two kinds of problems which may be considered. Input format information may be seen in Appendix D and examples of input cards for several typical problems are given in Appendix F.

### Comment Cards

Two comment cards are required for each problem case. Any information may appear on these cards anywhere in the eighty column fields.

### Control Card

One integer control card is required for each problem case. The integer, read by an I5 format provides control for the following:

- (a) An end to all computations
- (b) Printing of variables in namelist NUM
- (c) Supression of printing of namelist NUM variables
- (d) Stacking cases behind an initial case where thermochemical data determined by chemical equilibrium calculations does not change from the initial case.

If the control integer is zero computations are ended and the program ends. For example, if the last three cards on a set of stacked data are blank, the program ends after the next to last data set (the last case) has been used for calculations. Three blank cards should be used to provide a normal exit since each case requires two comment cards. No further printed output results if the integer control card is blank or the integer control variable, LETOUT, is zero. If the integer control is greater than one but not equal to 71, an initial case is considered but variables in namelist NUM are not printed. If thermochemical calculations occurred for a preceding initial case and these data will be used again in the present case, an integer control equal to 71 is input. If this is so (LETOUT equal 71) and thermochemical calculations have been made in a previous initial case, input data in THERMO and REACTANTS sets are not to be input again. If thermochemical data are to be input under namelist EQU and not calculated, LETOUT may be equal to 71 with the only effect being that parameters in namelist NUM will not be output under the namelist write.

#### Namelist NUM

The third type of input data is required for all cases. This data is

read under a namelist read input and includes the following:

- (a) Throat plane integration data (required by Subprogram HPCG)
- (b) Geometry data
- (c) Chamber operation mode data or mass generation data (three modes are possible)
- (d) Initial estimation data
- (e) Option control data
- (f) Injector data

A more complete description of the above is given in Appendix D.

Throat plane integration data are required by subroutine HPCG. These include the arrays or vectors PRMT and ERWT. PRMT are required for the first or an initial case where the throat radius is changed from a preceding initial case. ERWT are optional and if not included in namelist NUM, ERWT are determined internally. PRMT may only be changed by input with namelist NUM where the dependent variable error weights, ERWT, unless specifically designated, are optimized for throat solution iterations. Generally, ERWT are not input.

Geometry data include the throat radius (RT), the throat radius of curvature ratio (RCRT), and the chamber to throat area contraction ratio (EPSC). Unless changed, geometry data for stacked cases remain the same as initial case data.

Chamber operation mode data consist of only one of the three following sets.

- (a) PG, PCTMO (PCTMzero)
- (b) MDTI, AGAMGU, AMWGU, ATOGU (ATzeroGU)
- (c) PRF, ESPG, CDINJ, PRO

The chamber static pressure and the fraction of total mass flow in each flow zone starting with the inner most zone in all cases comprise the first chamber mode data set listed above. The sum of all PCTMO must equal 1.0.

When specified mass flow is considered, not only is the mass flow in each flow zone required but also initial estimations of the isentropic coefficient, the molecular weight, and the total temperature in each flow zone are required. Initial estimations are replaced by equilibrium calculations or data input under namelist EQU during the first chamber solution iteration.

When specified reservoir pressures are considered, the fuel and oxidizer reservoir pressures are required. The O/F ratio in each zone permits the oxidizer injector areas to therefore be determined. An initial estimation of chamber static pressure is required to start the chamber solution and the throat solution iterations. The initial estimate of the chamber static pressure is determined by a fraction of the fuel reservoir pressure in zone one. This estimate, ESPG, is optional in namelist NUM input but  $ESPG = .7$  is set before data is read under namelist NUM. ESPG must be less than one and should be based on experience with rocket motor calculations to avoid extensive iteration calculations in the chamber and throat solutions. Suitable values of ESPG have been determined to be .9 for gaseous injection and .5 for liquid injection to speed convergence some.

Option control data determine the type of problem solved and must be considered carefully to assure proper program operation. Integer variables as opposed to logical variables have been used to give more flexibility. Six integer variables are included in this category and are as follows:

- (a) MODECH
- (b) NCEC71
- (c) NAORW
- (d) MGORLI
- (e) MTOTMX
- (f) NSPPG

MODECH must be input for each initial case and need not be input again for stacked cases where it remains the same. This control allows specified mass flow for MODECH = 1, specified reservoir pressures for MODECH = 2, and fixed chamber static pressure for MODECH = 3. NCEC71 has the value 0 before read by namelist NUM. If NCEC71 = 0, frozen, calorically perfect thermochemical data is read by namelist EQU. NCEC71 = 1 permits frozen, calorically perfect thermochemical data to be determined by chemical equilibrium calculations. NCEC71 = 2 permits equilibrium data to be determined and shifting equilibrium calculations are used for the throat solution. NCEC71 = 3 permits frozen flow data to be determined and used for the throat solution. The program does not presently allow recalculation of thermochemical data during each chamber static pressure iteration loop for MODECH = 1 or 2. Modification of subprograms REACT and EQUILIB would be necessary to reconsider reactants data and solution calculation time would be increased considerably. When the chamber static pressure is fixed, reactants input data cards used for thermochemical data calculations need only be used once by the thermochemical calculation subroutines since mass flow iterations do not affect thermochemical calculations. If thermochemical frozen, calorically perfect data is input under namelist EQU, the data remains unchanged for iterations for the case. NAORW = 2 before being read by namelist NUM and remains unchanged for stacked cases unless read by a namelist NUM read.

NAORW = 1 is used when it is desired to specify fixed injector areas and NAORW = 2 is used to specify fixed injector velocities. MGORLI = 2 before being read by namelist NUM. If MGORLI = 1 is input, the gas constants of gaseous fuel and oxidizer reactants in each zone must be read in an initial case by namelist NUM. This option is useful for gaseous injection where reactant molecular weights are known. If MGORLI = 2 is input or if MGORLI does not appear in an initial case namelist NUM read, fuel and oxidizer reactants densities in each zone must be read in an initial case namelist NUM read. MTOTMX = 0 provides that the burned gas in the chamber is not to be fully mixed for the throat solution calculations. MTOTMX = 1 provides that fully mixed flow of the chamber burned gases be used for the throat solution calculations. For MTOTMX = 1, one flow zone is used for throat solutions and the options NCEC71 = 0 or 1 may be considered. No fully mixed solutions may be considered for NCEC71 = 2 or 3. If only one injector zone is considered for calculations, MTOTMX = 0 must be used. NSPPG = 0 before being read by namelist NUM. If NSPPG = 0, special chamber routine SPPG is not used. If NSPPG = 1, routine SPPG will be used. NSPPG = 1 may only be used for single zone flow of low temperature nonreacting gases. For striated flow analysis of rocket motors or for single zone reacting gas flows, routine SPPG may not be used. Routine SPPG provides a method for cold flow, single zone model analysis found in the laboratory.

Injector data includes the following:

- (a) Number of flow zones; NCHA1 and NCHA2
- (b) Oxidizer to fuel mass ratios; OXFULE
- (c) Injector reactants temperatures; TIFU and TIOX



- (d) Injector area data; AITAC, AIPCT, and AIPCTF
- (e) Injector velocities; WIFU and WIOX
- (f) Injected reactants densities; RHOIFU and RHOIOX
- (g) Injected gaseous reactants gas constants; RIFU and RIOX

Either injector area data or injector velocities and either densities or gas constants are input by namelist NUM. Other injector data required for initial cases and these also need not be changed for stacked cases unless required.

NCHA1 is required for an initial case read and must be greater than zero. NCHA2 = 0 before being read by namelist NUM initially and the sum of NCHA1 and NCHA2 cannot exceed twenty. Two regions of flow zones designated by NCHA1 and NCHA2 have been used to eliminate or change outer flow zones in stacked cases with few changes or to enable the user to modify the throat integration technique in routine HPCG for future adaptations.

Oxidizer to fuel mass ratio is required with all cases and indices accounting starts for the inner most flow zone. It may be necessary to avoid OXFULE = 0.0 or other very small fractions for a flow zone when using chemical equilibrium calculations due to the lower temperature limit on combustion products allowed by modified program CEC71.

Injector fuel temperature, TIFU, and oxidizer temperature, TIOX, must be input in each initial data case with namelist NUM. If OXFULE = 0.0 for any zone, special handling is not required; however, if oxidizer only is injected into a flow zone, the injected material must be designated a fuel and OXFULE is correspondingly set equal to zero for that zone.

If NAORW = 1, AITAC, AIPCT, and AIPCTF are required as initial case data by namelist NUM. AITAC is the ratio of total injector areas to the chamber area. AIPCT are the ratios of fuel plus oxidizer areas for each

flow zone to the total injector area and AIPCTF are the ratios of fuel injector area to the fuel plus oxidizer injector area in each flow zone.<sup>a</sup> If AITAC is not input or is zero, AIPCT then must be the injector areas for each zone. Thus, injector areas as opposed to area ratios may be input directly.

As an alternative to specified injector areas, fuel injector velocities, WIFU, and oxidizer injector velocities, WIOX, may be input. This option is used when NAORW = 2. NAORW = 2 before being read by namelist NUM for the first case being considered.

Injector reactant densities, RHOIFU for the fuels, and RHOIOX for the oxidizers, are required for MGORLI = 2. RHOIFU (1) and RHOIOX (1) correspond to the fuel and oxidizer densities in zone one, etc. MGORLI = 2 before the first case data are read by namelist NUM.

As an alternative to injector densities, fuel gas constants, RIFU, and oxidizer gas constants, RIOX, may be input for gaseous injection. The option is exercised by setting MGORLI = 1 in namelist NUM.

Refer to Appendix D for more information on data read by namelist NUM and to Appendix F for examples.

<sup>a</sup>If MODECH = 2 an exception to injector area input must be made. AITAC must be the ratio of fuel injector areas to the total chamber area and AIPCT is the ratio of fuel injector area for the *i*th zone to the total fuel injector area. For MODECH = 2, AIPCTF is not required input but is internally set equal to 1.0.

### Namelist EQU

If NCEC71 = 0, frozen, calorically perfect thermochemical data is used for chamber and throat calculations. The data required for each flow zone are the total temperature, TOG, the isentropic coefficient, GAMG, the burned gas molecular weight, MWG, and an integer variable NCHANG. Each case requires one set of data read by namelist EQU when NCEC71 = 0 and the data set follows variables read by namelist NUM. Each initial case requires all thermochemical variables described above and NCHANG must be greater than zero. For stacked cases where thermochemical data does not change from the previous case, it is necessary only to input NCHANG = 0. Table I is a schematic of the input and namelist variables required for all problems when NCEC71 = 0. Operation of the program with this input constitutes the first kind of option mentioned at the beginning of this section.

### THERMO Data

When thermochemical data are to be determined by chemical equilibrium calculations, NCEC71 = 1, 2, or 3, two types of data are required. The first type of chemical data required for this kind of problem as indicated by Table II, are THERMO Data. This consists of a THERMO code card, temperature range data, and a library of coefficients for calculating thermodynamic parameters of chemical species. The data used by this program is identical to that used by NASA SP-273.<sup>1</sup> The data may be read by card, tape, or disk and is written on unit 4 for use during a run. A permanent tape or disk containing the data may be made during a run (requiring a THERMO code card) or prior to a run (without THERMO code card) by proper job control cards. Options and changes to the THERMO Data of NASA SP-273<sup>1</sup> are possible with

this program also. The authors have found it convenient to permanently store THERMO data on a disk and use the disk with this program or with NASA program CEC71.

### REACTANTS Data

If NCEC71 = 1, 2, or 3, complete sets of REACTANTS Data must be input for each initial case. There must be as many REACTANTS data sets as there are flow zones; however, for a stacked case after an initial case where the thermochemical data will not change, the REACTANTS data sets need not be input. If cases are to be stacked as indicated above, the Control Card, LETOUT, must have the integer 71 starting in column 4 for each stacked case. The REACTANTS data set consists of three types of cards. The first type in this set has REACTANTS punched in columns one through nine. The second type of cards are reactant cards coded with the same format as the reactant card coding found in NASA SP-273<sup>1</sup> except that only O/F ratios may be used. A blank card follows the reactants cards. The third type of card in each REACTANTS set has NAMELISTS punched in columns one through nine. This card initializes chemical equilibrium calculations.

Additional information on program inputs and options may be seen in Appendixes D and F.

### Units

In this program the English Technical system of units is used with the exception of thermo data and the reactant card inputs which are used by the chemical equilibrium calculations. Thermo data and reactant card inputs form an optional kind of input and do not use the English Technical

system so as to be compatible with the inputs currently used by NASA program CEC71. The English Technical system is as follows:

<u>Physical Quantity</u>	<u>Unit</u>	<u>Symbol</u>
Length	feet	ft
Time	second	sec
Temperature	Rankine	R°
Force	pound	lbf
Pressure	pounds per square foot	psf
Mass Flow	pound seconds per foot	lbf-sec/ft

The Universal gas constant used is 1545.43 lbf-ft/lbmole-°R. Density has the units of lbf-sec<sup>2</sup>/ft<sup>4</sup> and specific impulse has the units of lbf-sec/lbmass. Where required, a conversion constant of 32.174 lbmass-ft/lbf-sec<sup>2</sup> is used. The oxidant to fuel weight ratio is used exclusively if reactant cards are used. Symbols used to represent parameters may be seen in Appendix B and program variable names are given in Appendix C.

## DESCRIPTION OF PROGRAM OUTPUT

The final output of the program is in the form of printed tables that are designed to be self-explanatory. Except where fully mixed flow is considered all output are the same.

### Namelist NUM

For an initial case, parameters in namelist NUM may be printed by a namelist write. The printout option is exercised by setting LETOUT = 1. For LETOUT  $\geq$  2 namelist NUM variables are not printed.

### Heading and Comments

The case number is printed for each case. The numbers are internally generated and not user controlled. Information on the input comment card are printed following the case number.

### Option Data

Option data includes MODECH, MGORLI, NAORW, NCEC71, NSPPG, MTOTMX, LETOUT, and NCHA1 + NCHA2 or the number of zones designated by NINCH. Also included are the number of throat solution iteration loops required for convergence (LOOP) and  $R_C/R_T$ .

### Geometry and Pressure Output

This output includes  $R_T$ , the converged value of the wall radius at the throat as determined by the throat solution, and the chamber contraction ratio, EPSC.  $R_T$  in this output is the specified throat radius. Pressure

data includes the chamber static pressure,  $P_g$ , and the centerline static pressure at the throat,  $P_{CL}$ .

### Injector Parameters

Output includes the zone stream function limits, the flow zone index,  $P_I$ ,  $T_{I_{fu_i}}$ ,  $T_{I_{ox_i}}$ ,  $A_{I_{fu_i}}$ ,  $A_{I_{ox_i}}$ ,  $w_{I_{fu_i}}$ ,  $w_{I_{ox_i}}$ ,  $\rho_{I_{fu_i}}$ ,  $\rho_{I_{ox_i}}$ ,  $R_{I_{fu_i}}$ ,  $R_{I_{ox_i}}$ ,  $\dot{m}_{I_{fu_i}}$ ,  $\dot{m}_{I_{ox_i}}$ ,  $P_{R_{fu_i}}$  and  $P_{R_{ox_i}}$ .

If MODECH = 3, reservoir pressures are set equal to zero and if MGORLI = 2 injector gas constants are set equal to zero. If  $O/F_i$  is zero, oxidizer parameters are zero.

### Burned Gas Parameters

When MTOTMX = 0, striated flow at the throat is considered and combustion product output parameters for the chamber included  $P_{o_{g_i}}$ ,  $T_{o_{g_i}}$ ,

$C_{p_{g_i}}$ ,  $\gamma_{g_i}$ ,  $T_{g_i}$ ,  $A_{g_i}$ ,  $w_{g_i}$ ,  $\rho_{g_i}$ , and  $\dot{m}_i$  for each flow zone.

### Mixed Gas Parameters

For fully mixed flow in the chamber (MTOTMX > 0) only one set of burned gas parameters are output. These parameters are designated by the same symbols as were zone parameters in burned gas outputs. In addition, however, the chamber static pressure of the fully mixed gases and the total pressure of the burned gases in each flow zone prior to mixing are included.

### Throat Plane Output

Spatial distributions of  $r$ ,  $P$ ,  $\psi$ ,  $T$ ,  $w$ ,  $M$ , and  $\gamma$  are included in throat plane output. Values at the throat wall for the converged solution are also given in the output.

### Performance Output

Vacuum specific impulse at the throat, characteristic velocity, total mass flow rate for radius of curvature effects and one dimensional flow are performance outputs. In addition, the ratios of mass flows (discharge coefficient), vacuum specific impulses, and characteristic velocities are printed. Output units are given.

Units for all outputs which appear in the other outputs are found in the UNITS section of this report.



## PROGRAM MODULES

The program consists of two modules as depicted in Appendix G. The first module was developed specifically for striated nozzle flow with throat radius of curvature effects. The second module is an adaption of NASA Lewis program CEC71 documented in NASA SP-273<sup>1</sup>. The original version of CEC71 has been modified to be compatible with requirements of the first module.

### Striated Nozzle Flow

This module consists of subprograms which read comments, control data, and namelist data. If subprogram DRIVCE is made a dummy subprogram, the striated nozzle flow module may be operated without chemical equilibrium subprograms for frozen, calorically perfect gas flows. In this form, the program would consist of a main program and fourteen subprograms: two of which, LOAD1 and TAB, may also be made dummy subprograms. The purpose of this module is to determine and write injector, chamber burned gas, and throat parameters.

### Chemical Equilibrium Calculations

This module, depicted in Appendix G, is used to determine thermochemical parameters for use by the first module. Linkage between the first module and this module is by common block and conversions within subprogram LOAD1 and entry to LOAD1, LOAD2. This module consists of sixteen subprograms and a block data subprogram. General output of program CEC71 has been suppressed; however, error message output has been retained.

The chemical equilibrium calculations module reads THERMO data and REACTANTS data inputs with formats and units of the unmodified form of program CEC71. Removal of comments from data output cards in modified CEC71 in this program would cause data output to appear after the heading and comments unless a stacked case with LETOUT = 71 is being run.

## ROUTINES

The first module of this program will be described in this section whereas Reference 1 describes in detail routines of module two (modified CEC71). Limitations on inputs to module two are described in the DESCRIPTION OF PROGRAM INPUT section.

### Main Program

A flow chart of the main program is given in Appendix H. Generally, the routine performs the following functions:

- (1) Initializes inputs and constants.
- (2) Reads namelist NUM. Writes NUM if LETOUT = 1.
- (3) Calculates chamber geometry.
- (4) Initializes  $P_g$  for MODECH = 1 or 2.

One dimensional equations are used to estimate initial values of  $P_g$  or  $\dot{m}_i$ . For fixed mass flow in zones, initial estimates of  $\gamma_{g_i}$ ,  $MW_{g_i}$ , and  $T_{og_i}$  are required. For fixed reservoir pressures, the chamber pressure is initially estimated to be a fraction of the fuel reservoir pressure in the first flow zone. The chamber static pressure is initially estimated if required in the main program.

- (5) Calls subroutine THROAT.

The purpose of the main program is to serve as a driver for the remainder of the program.

### Subroutine THROAT

The purpose of subroutine THROAT is to control the throat plane iteration technique, determine performance parameters, and write results. A flow chart of subroutine THROAT is given in Appendix H. This subroutine performs throat plane calculations prior to performance parameter calculations and so the two types of calculations may be discussed separately.

Initially, the number of iterations performed to satisfy choking at the throat is checked to determine whether more than seven iterations have been performed to determine the total mass flow or chamber static pressure required. If LOOP = 8 then results of the seventh loop are used to determine output parameters. If mass flows are specified or if reservoir pressures are specified,  $P_g$  is being sought in the throat solution. For these modes, MODECH = 1 or 2, alterations of  $P_g$  on the seventh loop is made by interpolation when  $P_g$  has been bracketed by previous iteration values of the chamber static pressure. If it has not been bracketed, the sixth iteration is used for output parameters. If specified reservoir pressures are considered, an additional requirement is that  $P_g$  must be less than one percent smaller than any fuel reservoir pressure. Very seldom more than four iteration loops are required for a converged throat solution.

The chamber solution is determined and then throat plane centerline static pressure estimated and altered to determine the throat radius corresponding to maximum mass flux. Integrations performed by subroutine HPCG require boundary conditions for both dependent variables at the nozzle centerline. These are  $P = P_{CL}$  and  $\psi = \text{PSI01}(1) = 0.0$ . After integration to  $\psi=1.0$  is complete, the corresponding wall radius is determined by subroutine AITKEN. Radii are ordered monotonically upward by subroutine UPORD. Successful determination of a minimum radius consists of two criteria which permit checks to be made as to (1) whether the radius is a minimum based on  $(dr/r)_w < .05\%$  and  $dP_{CL}/P_{CL} < 1\%$  and (2) whether the minimum radius determined is within .05% of  $R_T$ .

If the first of the above is satisfied but not the second,  $P_g$  or  $\dot{m}_{total}$  is altered and iteration starts again by indexing LOOP. Subroutine UPORD is used to order the  $P_{CL}$  during a loop once the minimum radius is bracketed for that loop. A second order curve fit by subroutine PLYCF is made to determine  $P_{CL}$  for  $(dr_w/dP_{CL}) = 0.0$ . The first criteria stated above must be satisfied

or the process is repeated with the three smallest radii of the loop.

With the first and second criteria stated above satisfied, remaining parameters except throat plane parameters and performance are output. Performance calculations are made as described in Performance Solution. Throat plane and performance parameters are printed as described in Throat Plane Output and Performance Output, respectively.

### Subroutine CHAMBR

The purpose of subroutine CHAMBR is to determine chamber parameters for striated or fully mixed flow. A flow chart for subroutine CHAMBR is given in Appendix H. This routine performs calculations shown in Chamber Solutions and calls other subroutines which cause thermochemical data to be calculated or read.

Upon being called by subroutine THROAT, subroutine CHAMBR initializes the iteration indexes NOAI and LOOPC and begins iteration loops by initializing the injector static pressure,  $P_I$ . For MODECH = 2, subroutine PRSPFD is called to determine zone mass flows and oxidizer injector areas. Both fuel and oxidizer reservoir pressures are input and zone O/F ratios must be specified. If MODECH = 3, subroutine PGFIX is called to determine thermochemical data and to determine zone mass flows from the total mass flow. Chamber parameters  $T_{g_i}$ ,  $A_{g_i}$ , and  $w_{g_i}$  are next initialized for the iterations and, for MODECH = 1 or 2, thermochemical data are determined by a direct call to subprogram EQUILIB. Special routine SPPG is called to provide the chamber parameters if option parameter NSPPG = 1 is in effect. Injector parameters are determined and chamber burned gas parameters  $T_{g_i}$ ,  $\rho_{g_i}$ ,  $w_{g_i}$ , and  $A_{g_i}$  for iteration loop LOOPC are calculated. The primary iteration with index NOAI is used for MODECH=2 which, after a

complete iteration with index LOOPC, alters the mass flow by repeated calls to PRSPFD. Index NOAI also serves to control the injector pressure iteration calculations and a convergence error message is provided when  $NOAI > 20$ . For  $MODECH = 2$ , iteration is complicated by the fact that mass flow must satisfy reservoir equations and chamber equations. Thus, for specified reservoir pressures, one equation set is added and one set of unknowns,  $\dot{m}_i$ , must exist to determine a chamber solution.

Convergence of the chamber solution permits dividing streamlines to be determined and corresponding radii in the chamber and total pressures to be determined. If  $MTOTMX > 0$ , fully mixed flow parameters are determined by equations given in the section Fully Mixed Flow.

#### Subroutine PGFIX

This subroutine is called by CHAMBR when  $MODECH = 3$ . The purpose of this routine is to call subroutine EQUILIB for thermochemical parameters. It also serves to provide an initial estimate of the total and zone mass flows and to calculate zone mass flows during iterations with index LOOP.

#### Subroutine PRSPFD

This routine provides an initial estimate for  $P_i$  for  $NOAI = 1$ . It also provides intermediate calculations for zone mass flows and oxidizer injector areas. PRSPFD is used when  $MODECH = 2$ .

#### Subroutine SPPG

Subroutine SPPG is used for single zone low temperature or non-reacting gas flow chamber calculations when  $MODECH = 1$  or  $3$ . Its use is optional and occurs when  $NSPPG = 1$ . The iteration index LOOPSP permits simultaneous solution

of chamber equations to satisfy convergence requirements. Convergence requirements are that burned gas static temperature for loop LOOPSP + 1 be within .05% of the temperature of loop LOOPSP.

#### Subroutine EQU LIB

This routine serves three purposes. These are:

- (1) Read frozen, calorically perfect thermochemical data under name-list NUM when NCEC71 = 0.
- (2) Call subprogram DRIVCE (formerly the main program for CEC71) for NCEC71 = 1, 2, or 3.
- (3) Store chamber thermochemical data for reuse during iterations. This is necessary when MTOTMX = 1.

Logical IF statements in subprogram EQU LIB determine the order of operations so to satisfy option and iteration loop requirements.

#### Subroutines LOAD1 and LOAD2

Subroutine LOAD1 (LOAD2 is an ENTRY to LOAD1) contain COMMON blocks POINTS and PERF which permit data transfer. These two blocks appear in NASA Lewis program CEC71. In addition, COMMON blocks ZONE, ONE, and ACSTAR have been included to permit data transferral between the two calculation modules which make up this program. LOAD1 and LOAD2 apply conversion units and store thermodynamic parameters for chamber and throat calculations. Each flow zone is assigned an index, KZONE, and two dimensional arrays permit interpolation in a flow zone at the throat for an internally generated pressure schedule. Ten pressure ratios are generated

for each flow zone in subprogram ROCKET when NCEC71 = 2 or 3. In addition, one dimensional sonic pressure and chamber pressure are stored. Thus, thermochemical calculations are performed for twelve pressures for each flow zone when NCEC71 = 2 or 3. When NCEC71 = 1, only data corresponding to the chamber and sonic pressure are determined; however, data corresponding to sonic pressure are not used for calculations since NCEC71 = 1 is for frozen, calorically perfect flow.

#### Subroutine HPCG

This subroutine uses Hamming's modified predictor-corrector method for the solution of throat plane equations which are of the initial-value type. This subroutine is discussed and listed with operating instructions in Reference 9. HPCG uses two external subprograms, FCT and OUTP. FCT provides the right hand side of two first order equations and OUTP stores the solution vectors of HPCG. Few changes have been made to the original version of HPCG. Comment cards have been removed and statements which have been added are so indicated by alphabetic characters in card sequences replacing last character zeros. Look to the program listing of HPCG to see the changes.

#### Subroutine FCT

Subroutine FCT provides the right hand side of the two first order ordinary differential equations for  $P$  and  $\psi$  with  $r$  as the independent variable. In the call to FCT from HPCG three parameters are transferred;  $R$  is the independent variable,  $Y$  are the solutions  $P$  and  $\psi$ , and  $DERY$  are the first two error weights for the dependent variables which are saved in



THROAT under variable name ERWT. FCT provides a check of option NCEC71 to determine if frozen, calorically perfect flow is being considered or if frozen or equilibrium flow is being considered. Determination is made as to which flow zone integrations are being performed in and provides the corresponding thermochemical variables. For NCEC71 = 0 or 1, the index K determines the thermochemical variables to be used. For NCEC71 = 2 or 3, subroutine TAB is called to interpolate on the current value of K and Y(1). Y(1) is the current pressure, P, and K corresponds to KZONE. KZONE is generated in DRIVCE and is the index on two dimensional arrays developed in LOAD1. Equations used for dependent variables are described in the THEORY section under Throat Solution.

#### Subroutine OUTP

Subroutine OUTP is called by HPCG. This routine stores dependent variables with index J. If NCEC71 = 0 or 1, temperature (T(J)) Mach number (YPSAV(J,4)), and velocity (YSAVE(J,3)) are determined in OUTP. OUTP also causes PRMT(5) to be set equal to 1.0 when  $\psi$  (YSAVE(J,2)) becomes  $\geq 1.0$ . PRMT(5)  $\neq 0.0$  causes return to subroutine THROAT from subroutine HPCG.

#### Subroutine TAB

TAB is an interpolation routine used by subroutine FCT for determination of thermochemical data when NCEC71 = 2 or 3.

### Subroutine AITKEN

This subroutine is called by subroutine THROAT to determine the throat wall radius after return to THROAT from HPCG. It also provides wall values of throat plane parameters which are determined in the performance section of subroutine THROAT.

### Subroutine UPORD

This subroutine is called by subroutine THROAT to order a pair of real array variables. The parameter list for this subroutine contains two array variables and two integers. The first integer gives the number of pairs and the second integer, MORDER, determines which array will be ordered up.  $MORDER \neq 0$  orders the first array upward with corresponding variables in the second carried along.  $MORDER = 0$  orders the second array.  $MORDER = 1$  for this program.

### Subroutine PLYCF

Subroutine PLYCF is a least squares polynomial curve fit routine called by subroutine THROAT to predict  $P_{CL}$  for  $r_{w_{min}}$ .

Subroutine DRIVCE is the modified main program of NASA Lewis program CEC71. Subroutines REACT, SEARCH, HCALC, SAVE, EQLBRM, CPHS, MATRIX, GAUSS, OUT1, VARFMT, EFMT, THERMP, ROCKET, RKTOUT, FROZEN, and BLOCK DATA are subprograms used by the program CEC71 and are described in NASA SP-273<sup>1</sup>. Differences between these routines and the routines of CEC71 may be seen by card sequence numbers. A / symbol after the sequence name indicates a comment card has been made and an alphabetic character and a repeated sequence

number after the sequence name indicates a statement has been added.

Changes to CEC71 occur in DRIVCE (CEC71 program Main), ROCKET, and RKTOUT.

Subroutines SHCK and DETON of CEC71 have been removed for this modification.

## APPENDIX A

### PHILOSOPHY

The philosophy used in developing this program has been to define where possible, subprograms or variables with names which are appropriate and representative of the purpose they serve or the commonly used symbol they represent, respectively. Use of the same variable name to represent different variables has been avoided. Subprograms which have been written and documented by others which serve as utility subprograms may have changes; however, changes which have been necessary have been made so as to be easily detectable. Individual card sequence numbers expose the changes made. The program has been written to be as machine independent as possible. The FORTRAN IV language (FORTRAN G level 20) has been used and the program is constructed so that user modifications are possible, particularly where a change in the units for input and output is desired. Transferral of variables between subprograms is by common block where possible and algorithms have been used which are logical and easy to follow. Computation time for typical cases are small (approximately one minute on the IBM 360/65). The main input data set is by namelist to simplify checking input cards and to simplify stacked case input data sets.

The program is intended to provide a capability for rapid analysis with detailed chamber operating conditions and spatial distributions of thermodynamic flow properties on the nozzle throat plane. An important aspect of the program is that it permits throat plane calculations with a variable adiabatic or isentropic coefficient and is not limited to a constant stagnation pressure in the chamber. The computer program for calculation of chemical equilibrium compositions as found in NASA SP-273<sup>1</sup> has been

incorporated as subprograms. Changes to this program, CEC71, may easily be seen in the program listing and compared to the original version of the program by the sequence code found in the last eight columns of the computer card. The SHCK and DETON subprograms of CEC71 were removed and references to them have been made comment cards. Input data to the modified form of CEC71 in this program are simplified somewhat but, where required, have the same form and units used by program CEC71. Standard output of the modified CEC71 calculations have been suppressed by commenting output in the manner described above; however, error messages from this program have not been suppressed.

## APPENDIX B

### SYMBOLS

$A$	area, $\text{ft}^2$
$A_C$	chamber area, $\text{ft}^2$
$A_T$	throat area, $\text{ft}^2$
$C$	$P/\rho^\gamma$ , polytropic equation of state constant (isentropic)
$C_D$	discharge coefficient
$C_p$	constant pressure specific heat, $\text{ft}^2/\text{sec}^2\text{-}^\circ\text{R}$
$c^*$	characteristic velocity, $\text{ft}/\text{sec}$
$g_c$	32.174 $\text{lbmass}\text{-ft}/\text{lbf}\text{-sec}^2$
$H_o$	total enthalpy, $\text{ft}^2/\text{sec}^2$
$h$	enthalpy, $\text{ft}^2/\text{sec}^2$
$I_{sp_{vac}}$	throat vacuum specific impulse, $\text{lbf}\text{-sec}/\text{lbmass}$
$M$	Mach number
$MW$	molecular weight, $\text{lbmass}/\text{lbmole}$
$\dot{m}$	mass flow rate, $\text{lbf}\text{-sec}/\text{ft}$
$O/F$	oxidant to fuel mass ratio
$P_o$	stagnation pressure, $\text{lbf}/\text{ft}^2$
$P$	pressure, $\text{lbf}/\text{ft}^2$
$R$	gas constant, $\text{ft}^2/\text{sec}^2\text{-}^\circ\text{R}$
$R_C$	throat wall radius of curvature, $\text{ft}$
$R_T$	throat radius, $\text{ft}$ .
$R_v$	flow radius of curvature at throat, $\text{ft}$
$R_u$	universal gas constant, $1545.43 \text{ lbf}\text{-ft}/\text{lbmole}\text{-}^\circ\text{R}$
$r$	radius; radial coordinate, $\text{ft}$
$T$	temperature, $^\circ\text{R}$

$T_o$	stagnation temperature, °R
$u$	radial velocity component, ft/sec
$v$	tangential velocity component, ft/sec
$w$	axial velocity component, ft/sec
$z$	axial coordinate, ft
$\gamma$	isentropic exponent or adiabatic coefficient
$\pi$	3.14159265
$\rho$	density, lbf-sec <sup>2</sup> /ft <sup>4</sup>
$\psi$	stream function = $\int_0^{\dot{m}(r)} [d\dot{m}/\dot{m}_{total}]$

#### Subscripts:

CL	centerline value on or near the throat plane
fu	fuel
g	combustion product or burned gas
I	injector
min	minimum value
mix	fully mixed
ox	oxidizer
R	reservoir
total	total or whole amount
w	wall value on or near the throat plane
1-D	one dimensional

#### Superscripts:

'	modified
*	critical throat condition

#### Indices:

i	striation zone (inner most zone is 1)
j	local value on the throat plane

# APPENDIX C

## COMMON VARIABLES

All common variables are given in this appendix except those developed in the original unmodified program CEC71, which is documented in NASA SP-273.

Variable	Dimension	Common Label	Description and Comments
AC	1	THR	$A_C$ .
AG	20	THR	$A_g$ .
AIFU	20	THR	$A_{I_{fu_i}}$ .
AIOX	20	THR	$A_{I_{ox_i}}$ .
AIPCTF	20	THR	Fraction of injector fuel area assigned to each zone. <sup>a</sup>
AMAC	20,13	LOTAB	Mach number array in each zone corresponding to APRES values.
APRES	13	LOTAB	$P_g/P$ array used for interpolation at the throat plane for frozen or equilibrium flow.
ARHO	20,13	LOTAB	Density array in each zone corresponding to APRES values.
ASON	20,13	LOTAB	Sonic velocity array in each zone corresponding to APRES values.
AUX	16,4	blank	Auxiliary storage array (See HPCG subprogram description).
AVEL	20,13	LOTAB	Velocity array in each zone corresponding to APRES values.
C	1	CALC	$P_g/P_o, Y_{g_i}$ , used for frozen, calorically perfect flow only.
CDINJ	20	THR	Injector discharge coefficients for MODECH = 2.

<sup>a</sup>For MODECH = 2, AIPCT becomes the ratio of fuel injector areas to chamber area and AIPCTF is not required.



CLP	10	blank	$P_{CL}$ .
CPG	20	TWO	$C_{p_{g_i}}$ .
CST	20	LOAD	$c^*_i$ from chemical equilibrium calculations.
CSTAR	13	ACSTAR	$c^*$ corresponding to $P_g$ for each zone
DERY	4	blank	Input error weights, dependent variable derivatives (see FCT and HPCG subprograms descriptions).
DIACH	1	THR	Chamber diameter.
EPSC	1	ONE	Chamber contraction ratio.
ERWT	4	blank	Error weights for dependent variables in subprogram HPCG.
GAM	1	CALC	Local value of $\gamma$ on the throat plane.
GAMG	20	TWO	$\gamma_{g_i}$ .
GAMR	20,13	LOTAB	Isentropic coefficient array in each zone corresponding APRES values
GAMSAV	200	CALC	$\gamma$ array on the throat plane.
HO (Hzero)	1	CALC	Local value of total enthalpy, $H_0 = C_{p_{g_i}} T_{0_{g_i}}$ .
ICASE	1	ONE	Solution case index.
IHLF	1	ONE	Step size bisection parameters used by subroutine HPCG.
J	1	TWO	Step index for local throat plane parameters
K	1	CALC	Index parameter for zone designation.
KZONE	1	ZONE	Zone index.

LETOUT	1	ZONE	Integer control constant. See input data for LETOUT options.
LOOP	1	blank	Index counter designating the number of throat solution iteration loops.
MDTI	20	THR	$\dot{m}_i$
MDTIFU	20	THR	$\dot{m}_{I_{fu_i}}$
MDTIOX	20	THR	$\dot{m}_{I_{ox_i}}$
MGORLI	1	ONE	Input option parameter indicating injector gas constant input (=1) or injector density input (=2). MGORLI = 2 initially.
MODECH	1	blank	Input option parameter indicating the mass injector scheme. See input data for MODECH options.
MORDER	1	blank	= 1, describes the method for ordering variables in subroutine UPORD.
MTOTMX	1	THR	Input option parameter. MTOTMX = 0 for striated flow, MTOTMX=1 for fully mixed flow. MTOTMX=0 initially.
MWG	20	THR	$MW_{g_i}$
MO (Mzero)	1	TWO	$\dot{\Sigma m}_i$ , total mass flow.
MOCH (MzeroCH)	7	blank	$\dot{\Sigma m}_i$ corresponding to LOOP.
NAORW	1	THR	Input option parameter indicating whether injector areas are fixed (=1) or injector velocities are fixed (=2). Initially NAORW = 2.
NCEC71	1	ONE	Input option indicating the degree of chemical equilibrium. See Input data for NCEC71 options.

NCHA1	1	TWO	The number of flow zones in an arbitrary chamber region ( $1 \leq \text{NCHA1} \leq 10$ ). NCHA1 is an input option.
NCHA2	1	TWO	The number of flow zones in an arbitrary chamber region ( $0 \leq \text{NCHA2} \leq 10$ ). NCHA2 is an input option.
NDIM	1	ONE	= 2. See HPCG subprogram description
NSPPG	1	ONE	Special input option for single zone nonreacting flow calculations. Initially NSPPG = 0. See input list.
OXFUL	20	ZONE	$O/F_i$ for chemical equilibrium calculations.
OXFULE	20	THR	$O/F_i$ .
PCTM0 (PCTMzero)	20	THR	Fraction of total flow in the <u>i</u> th flow zone.
PG	1	THR	$P_g$ .
PGCH	7	blank	$P_g$ corresponding to LOOP.
PGPSIA	1	ZONE	$P_g$ internally converted to psia for chemical equilibrium calculations.
PI	20	THR	$P_I$
PMIX	1	MIXED	$P_{g_{\text{mix}}}$
PRF	20	THR	$P_{R_{fu_i}}$
PRO	20	THR	$P_{R_{ox_i}}$
PRMT	6	blank	Input and output array for HPCG (see input description).
PSI01	10	TWO	$\psi_i$ in the first flow region.
PSI02	10	TWO	$\psi_i$ in the second flow region.

PSI12	1	TWO	$\psi$ corresponding to the streamline between the first and second flow regions.
P0 (Pzero)	20	MIXED	Total pressure in each zone before full mixing occurs.
POCL (PzeroCL)	7	blank	$P_{o_{g_i}}$ corresponding to LOOP.
POG (PzeroG)	20	TWO	$P_{o_{g_i}}$
RAD	20	THR	Radius corresponding $\psi_i$ in the chamber.
RCRT	1	ONE	$R_C/R_T$
RCWALL	1	TWO	$R_C$
RGAS	20	THR	$R_{g_i}$
RHOG	20	THR	$\rho_{g_i}$
RHOIFU	20	THR	$\rho_{I_{fu_i}}$
RHOIOX	20	THR	$\rho_{I_{ox_i}}$
RIFU	20	THR	$R_{I_{fu_i}}$
RIOX	20	THR	$R_{I_{ox_i}}$
RLIM	1	blank	not used.
RMIN	7	blank	$r_w$ corresponding to LOOP.
RMINSQ	7	blank	$r_w^2$ corresponding to LOOP.
RT	1	TWO	$R_T$
RW	10	blank	Wall radius vector corresponding to LOOP.

T	200	ONE	T on the throat plane.
TEMPE	20,13	LOTAB	Temperature array in each zone corresponding to APRES values.
TG	20	THR	$T_{g_i}$ .
TIFU	20	THR	$T_{I_{fu_i}}$ .
TIOX	20	THR	$T_{I_{ox_i}}$ .
TWOPI	1	TWO	$2\pi$
TOG (TzeroG)	20	THR	$T_{o_{g_i}}$ .
UNIVR	1	THR	$\mathcal{Q}$
URMNSQ	7	blank	$1/r_w^2$ corresponding to LOOP.
VACIDI	20	LOAD	$I'_{sp_{vac}}$ .
VACSPI	20,13	LOTAB	Vacuum specific impulse array in each zone corresponding to APRES values.
WG	20	THR	$w_{g_i}$ .
WIFU	20	THR	$w_{I_{fu_i}}$ .
WIOX	20	THR	$w_{I_{ox_i}}$ .
WMR	20,13	LOTAB	Molecular weight array in each zone corresponding to APRES values.
XSAVE	200	TWO	r on the throat plane. The index is J.
Y	4	blank	Y(1)=P and Y(2)= $\psi$ on the throat plane corresponding to XSAVE. Y(3) and Y(4) are not used.

YPSAV	200,4	TWO	YPSAV(J,1) is the pressure derivative array on the throat plane. YPSAV (J,2) is the derivative of $\psi$ . YPSAV(J,3) is $T_0 / T$ on the throat plane. YPSAV(J,4) is the Mach number array on the throat plane.
YSAVE	200,4	TWO	YSAVE(J,1) = p on the throat plane. YSAVE(J,2) = $\psi$ on the throat plane. YSAVE(J,3) = w on the throat plane. YSAVE(J,4) is dA corresponding to YSAVE(J,1).
ZCH	1	THR	not used.

# DIMENSIONED VARIABLES

Variable	Dimension	Routines where used	Description and Comments
A	11	PLYCF	polynomial coefficients.
ACO	11	THROAT	polynomial coefficients.
AGAMGU	20	MAIN	initial $\gamma_{g_i}$ estimates.
AIPCT	20	MAIN	fraction of total injector area for zone i. <sup>a</sup>
AMACH	200	THROAT	Mach number on the throat plane.
AMWGU	20	MAIN	initial $MW_{g_i}$ estimates.
ATOGU (ATzeroGU)	20	MAIN	initial $T_{o_{g_i}}$ estimates.
AUX	16,2	HPCG	Auxiliary storage array (see HPCG subprogram description).
CLP	10	UPORD	$P_{CL}$ .
DERY	2	FCT, OUTP, HPCG	input error weights, dependent variable derivatives (see FCT subprogram description).
DRDPSV	10	THROAT	$dr_w/dP_{CL}$ .
DUM1	3	THROAT	independent dummy variable for AITKEN interpolation.
DUM2	3	THROAT	dependent dummy variable for AITKEN interpolation.
PII	20	CHAMBR	stored $P_I$ array during CHAMBR iteration.
PRMT	6	OUTP, HPCG	input and output array for HPCG (See input description).
PSI	200	THROAT	$\psi$ on throat plane.

<sup>a</sup>For MODECH = 2, AIPCT is the ratio of fuel injector area to total fuel injector area for the ith zone.

RADT	20	THROAT	radius of stream tube shell boundary at the throatplane.
RW	10	UPORD	$r_w$ .
SAVGAM	20	EQUILIB	$\gamma_{g_i}$ , values stored to prevent destruction in fully mixed flow cases.
SAVMWG	20	EQUILIB	$MW_{g_i}$ values stored to prevent destruction in mixed flow cases.
SAVTOG (SAVTzeroG)	20	EQUILIB	$T_{o_{g_i}}$ values stored to prevent destruction in fully mixed flow cases.
SUMAGG	20	CHAMBR	$\Sigma A_{g_i}$ .
TGA	15	SPPG	$T_{g_1}$ .
TGA	20,10	CHAMBR	$T_{g_i}$ .
WHAT1	20	MAIN	first input comment card required for each case (20A4).
WHAT2	20	MAIN	second input comment card required for each case (20A4).
X	variable	AITKEN, PLYCF	general independent variable.
Y	2	FCT,OUTP, HPCG	dependent variable in HPCG (see FCT subroutine description).
Y	variable	AITKEN, PLYCF	general dependent variable.



## APPENDIX D

### INPUTS AND OPTIONS

#### Comment Cards (2):

<u>Order</u>	<u>Contents</u>	<u>Format</u>	<u>Card Columns</u>
First <sup>a</sup>	Any information pertinent to the case being run.	20A4	1 to 80

#### Control Card (Variable name LETOUT):

<u>Order</u>	<u>Contents</u>	<u>Format</u>	<u>Card Columns</u>
Second <sup>b</sup>	Integer Control (LETOUT in Common label ZONE)	I5	1 to 5

- (1) If LETOUT = 0, program computations stop and program output begins.
- (2) If LETOUT = 1, any initial case input follows and variables in namelist NUM will be output by namelist write.
- (3) If LETOUT > 1, but  $\neq 71$ , any initial case<sup>c</sup> or a stacked case<sup>d</sup> using input thermochemical data follows. Variables in namelist NUM will not be output.
- (4) Stacked cases which require thermochemical calculation results be used for solutions as opposed to input thermochemical data must have LETOUT = 71 in columns 4 to 5. This stacked case option is used as when the chamber static pressure, flow zone O/F ratios, and reactants data for each flow zone will not change for the stacked cases. Nozzle geometry and/or propellant distributions may be changed when LETOUT=71 for stacked cases which meet requirements stated above.

<sup>a</sup>Two comment cards are required for all cases.

<sup>b</sup>The control card must be preceded by two comment cards.

<sup>c</sup>More than one initial case may be run at one time. Any initial case is a case where a complete set of thermochemical input data is required.

<sup>d</sup>Stacked cases refer to cases where thermochemical data need not be calculated (NCEC71 = 1, 2, or 3) or read (NCEC71 = 0).

Namelist NUM Variables:

<u>Variable</u>	<u>Dimension</u>	<u>Type</u>	<u>Common Label</u>	<u>Value before read by first case</u>
PRMT	6	R	blank	undefined
ERWT	4	R	blank	0.
PG	1	R	THR	0.
MDTI	20	R	THR	0.
RT	1	R	TWO	undefined
RCRT	1	R	ONE	undefined
EPSC	1	R	ONE	undefined
OXFULE	20	R	THR	0.
PRF;PRO	20;20	R	THR	0.
ESPG	1	R	-	.7
AITAC	1	R	-	0.
AIPCT	20	R	-	0.
AIPCTF	20	R	THR	0.
RHOIFU	20	R	THR	0.
RIFU	20	R	THR	0.
TIFU	20	R	THR	0.
WIFU	20	R	THR	0.
RHOIOX	20	R	THR	0.
RIOX	20	R	THR	0.
TIOX	20	R	THR	0.
WIOX	20	R	THR	0.
PCTMO	20	R	THR	0.
AGAMGU	20	R	-	0.
AMWGU	20	R	-	0.
ATOGU	20	R	-	0.
CDINJ	20	R	THR	.7

Namelist NUM Variables (cont'd.)

<u>Variable</u>	<u>Dimension</u>	<u>Type</u>	<u>Common label</u>	<u>Value before read by first case</u>
MTOTMX	1	I	THR	0
MODECH	1	I	blank	undefined
NAORW	1	I	THR	2
MGORLI	1	I	ONE	2
NCHA1	1	I	TWO	undefined
NCHA2	1	I	TWO	2
NSPPG	1	I	ONE	0
NCEC71	1	I	ONE	0

Variable in NUM

Option exercised

MTOTMX = 0	Striated flow solution.
MTOTMX = 1	Fully mixed flow solution (only for NCEC71 = 0 or 1).
MODECH = 1	Input zone mass flows.
MODECH = 2	Input zone fuel and oxidizer reservoir pressures.
MODECH = 3	Input chamber static pressure.
NAORW = 1	Input injector areas.
NAORW = 2	Input injector velocities (only for MODECH=1 or 3).
MGORLI = 1	Input injector gas constants.
MGORLI = 2	Input injector densities.
NSPPG = 0	Complete chamber solution.
NSPPG = 1	Special chamber solution (only for NCHA1=1, NCHA2=0).
NCEC71 = 0	Input thermochemical data by namelist EQU.
NCEC71 = 1	Calculates thermochemical data for frozen, caloric perfect flow.
NCEC71 = 2	Calculates thermochemical data for equilibrium flow.
NCEC71 = 3	Calculates thermochemical data for frozen flow.

Namelist EQU Variables (used only when NCEC71 = 0):

<u>Variable</u>	<u>Dimension</u>	<u>Type</u>	<u>Common label</u>	<u>Value before read by first-initial case</u>
TOG <sup>a</sup>	20	R	THR	undefined
GAMG	20	R	TWO	undefined
MWG	20	R	THR	undefined
NCHANG	1	I	-	0

NCHANG must be read for each case under namelist EQU when NCEC71=0. If an initial case is being considered NCHANG must be greater than zero and thermochemical data variables for each flow zone starting from the innermost flow zone must be input under namelist EQU. For stacked cases when NCEC71=0 and new thermochemical data are not to change from the preceding initial case, only NCHANG=0 need be read under namelist EQU. For stacked cases when NCEC71=0, control card LETOUT may be input with any integer greater than one in columns 1 to 5 and parameters in namelist NUM will not be output by a namelist write.<sup>b</sup>

<sup>a</sup>TzeroG

<sup>b</sup>Namelist NUM print out for cases after the first case will not be completely applicable to the cases since variable parameters in NUM from the previous case will be seen.

Thermo Data:

<u>Card Order</u>	<u>Contents</u>	<u>Format</u>	<u>Card Column</u>
1	THERMO	3A4	1 to 6
2	Temperature range for 2 sets of coef- ficients: lowest, common, and highest T, °K	3F10.3	1 to 30
3	Species name, Date Atomic symbols and formula Phase of species (S,L, or G for solid, liquid, or gas respec- tively) Temperature range Integer 1	3A4, 2A3 4(A2,F3.0)  A1  2F10.3 I15	1 to 12, 19 to 24 25 to 44  45  46 to 65 80
4	Coefficients $a_i$ ( $i=1$ to 5) (for upper temperature interval) Integer 2	5(E15.8)  I5	1 to 75  80
5	Coefficients $a_i$ ( $i=6$ and 7) (for upper temperature interval) and $a_i$ ( $i=1$ to 3) (for lower temperature interval) Integer 3	5(E15.8)  I5	1 to 75  80
6	Coefficients $a_i$ ( $i=4$ to 7) (for lower temperature interval) Integer 4	4(E15.8)  I20	1 to 60  80
(a) repeat cards 3 to 6 for each different species			
(Final Card)	END	3A4	1 to 3

### Reactants Data:

<u>Order</u>	<u>Contents</u>	<u>Format</u>	<u>Card Columns</u>
1	REACTANTS	3A4	1 to 9
2	One card for each reactant species (maximum 15). Each card contains: (1) Atomic symbols and formula numbers (maximum of 5 sets) <sup>a</sup> (2) Relative weight <sup>b</sup> (3) Enthalpy <sup>a</sup> , cal/mole (4) State: ,L, or G for solid, liquid, or gas, respectively (5) Temperature associated with enthalpy in (3), °K (6) F if fuel or 0 if oxidant (7) Density in g/cm <sup>3</sup> (optional)	5(A2,F7.5)  F7.5 F9.5 A1  F8.5 A1 F8.5	1 to 45  46 to 52 54 to 62 63  64 to 71 72 73 to 80
3	blank		
4	NAMELISTS	3A4	1 to 9
(c)	repeat cards 1 to 4 for each flow zone		

<sup>a</sup> Program will calculate the enthalpy (3) for species in THERMO data at the temperature (5) if zeros are punched in card columns 37 and 38.

<sup>b</sup> Relative weight of fuel in total fuel or oxidant in total oxidant.

# APPENDIX E PROGRAM LISTING

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10 ALL INPUT DATA HAVING UNITS EXCEPT INPUTS IN THE REACTANTS AND
20 THERMO DATA CARDS TO THE CHEMICAL EQUILIBRIUM SUBPROGRAMS (FORMERLY
30 CEC71) MUST USE AN ENGLISH TECHNICAL SYSTEM OF UNITS.
40 THE ENGLISH TECHNICAL SYSTEM OF UNITS REQUIRED EMPLOYS
50 ONLY FOUR BASIC UNITS. THESE UNITS ARE POUNDS FORCE, SECONDS,
60 FEET, AND DEGREES RANKINE.
70 ALL OUTPUT DATA HAVING UNITS ARE IN THE ENGLISH TECHNICAL SYSTEM
80 OF UNITS DESCRIBED ABOVE UNLESS INDICATED.
90
100 REAL MDTI,MO,MUCH,MDTIFU,MDTIOX,MWG
110 DIMENSION WHAT1(20),WHAT2(20),AGAMGU(20),AMWGU(20),ATOGU(20)
120 1,AIPCT(20)
130 COMMON
140 1 PRMT(6),DERY(4),AUX(16,4),Y(4),RW(10)
150 2 ,POCL(7),ERWT(4),RMIN(7),MODECH,RMINSQ(7)
160 3 ,PGCH(7),CLP(10),RLIM,MORDE,LOOP,MOCH(7),URMNSQ(7)
170 4 ,NDIM,IHLF,RCRT,EPSC,MGORLI,NSPPG,ICASE,NCEC71,T(200)
180 5 COMMON/TWO/YSAVE(200,4),XSAVE(200),J,CPPG(20),POG(20),YPSAV(200,4),
190 1 RT,RCWALL,GAMG(20),NCHAL,NCHAZ,PSIO1(10),PSIO2(10),TWOP1,PSI12,MO
200 2 COMMON/THR/OXFULE(20),PG,TOG(20),RGAS(20),UNIVR,WIFU(20),
210 3 AIFU(20),RHOIFU(20),RIFU(20),TIFU(20),WIOX(20),AIOX(20),
220 4 RHOIOX(20),RIOX(20),TIOX(20),AIPCTF(20),ZCH,PI(20),DIACH,
230 5 TG(20),AG(20),WG(20),RHOG(20),RAD(20),MDTI(20),PRF(20),
240 1 PCTMO(20),MDTIFU(20),MDTIOX(20),MWG(20),AC,NAORW,MTOTMX
250 2 ,CDINJ(20)
260 3 COMMON/ZONE/KZONE,PGPSIA,OXFUL(20),LETOU
270 4 NAMELIST/NUM/PRMT,ERWT,PG,MDTI,RT,RCRT,EPSC,OXFULE,PRF,PRO,ESPG,
280 5 AITAC,AIPCT,AIPCTF,RHOIFU,RIFU,TIFU,WIFU,RHOIOX,RIOX,TIOX,WIOX,
290 1 PCTMO,CDINJ,AGAMGU,AMWGU,ATOGU
300 2 MTOTMX,MODECH,NAORW,MGORLI,NCHAL,NCHAZ,NSPPG,NCEC71
310
320 LETOUT=0 STOPS CALCULATIONS.
330 LETOUT=1 WRITES VARIABLES IN NAMELIST NUM.
340 LETOUT=71 DOES NOT REQUIRE NEW INPUTS FOR DRIVE WHICH IS USEFUL
350 WITH STACKED CASES AS WHERE CHAMBER STATIC PRESSURE REMAINS THE
360 SAME AS THE PREVIOUS CASE. LETOUT.GT.1 ALLOWS STACKED CASES AND
370 VARIABLES IN NUM ARE NOT PRINTED.
380
390 NCHAL PLUS NCHAZ ARE THE NUMBER OF FLOW ZONES CONSIDERED.
400
410 MODECH=1 CORRESPONDS TO FIXED MASS INJECTION.
420 MODECH=2 CORRESPONDS TO SPECIFIED RESERVOIR PRESSURES.
430 MODECH=3 CORRESPONDS TO FIXED CHAMBER STATIC PRESSURE.
440
450 MGORLI=1 IS FOR GAS INJECTION. MGORLI=2 IS FOR LIQUID OR GAS
460 INJECTION. INJECTOR GAS CONSTANTS ARE REQUIRED WHEN MGORLI=1.
470 FUEL AND OXIDIZER DENSITIES ARE REQUIRED WHEN MGORLI=2.
480
490 NAORW=1 IS FOR FIXED AREAS. NAORW=2 IS FOR FIXED VELOCITIES.

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TWOPI=6.2831853  
NCEC71=1,2,OR 3 INITIATES MODIFIED EQUILIBRIUM PROGRAM CEC71.  
NCEC71=0 USES A SPECIAL INPUT DATA SET AND ASSUMES FROZEN,  
CALORICALLY PERFECT FLOW.  
FOR NCEC71=0, THE SPECIAL INPUT DATA SET UNDER NAMELIST EQU IS  
REQUIRED AND CONSISTS OF ONE SET FOR EACH ZONE OF TOG, GAMG, MWG  
STARTING WITH THE INNER ZONE. IN ADDITION, AN INTEGER OPTION  
NUMBER, NCHANG, WHICH IS GREATER THAN ZERO, MUST BE READ IN THE CASE  
DESCRIBED ABOVE. HOWEVER, IF CASES ARE TO BE STACKED BEHIND THE CASE  
NCHANG EQUAL ZERO NEED BE READ IN FOR THE STACKED CASES  
WITH NCEC71=0.  
NCEC71=0 INPUT FROZEN, CALORICALLY PERFECT DATA.  
NCEC71=1 CEC71 CALCULATES FROZEN, CALORICALLY PERFECT DATA.  
NCEC71=2 CEC71 CALCULATES EQUILIBRIUM DATA.  
NCEC71=3 CEC71 CALCULATES FROZEN DATA.

UNIVR=1545.43  
NDIM=2  
ICASE=0  
DO 111 I=1,20  
PRF(I)=0.  
PRO(I)=0.  
OXFULE(I)=0.  
MDTIFU(I)=0.  
MDTIOX(I)=0.  
AIPCT(I)=0.  
AIPCTF(I)=0.  
RHOIFU(I)=0.  
RHOIOX(I)=0.  
RIFU(I)=0.  
RIOX(I)=0.  
TIFU(I)=0.  
TIOX(I)=0.  
WIFU(I)=0.  
WIOX(I)=0.  
AGAMGU(I)=0.  
AMWGU(I)=0.  
ATOGU(I)=0.  
CDINJ(I)=7  
CDTMO(I)=0.  
ERWT(1)=0.  
ERWT(2)=0.  
ERWT(3)=0.

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ERWT(4)=0.
ESPG=.7
AITAC=0.
NCHAZ=0.
NSPPG=0
NAORW=2
MGORLI=2
NCEC71=0
MTOTMX=0
1 READ(5,101)WHAT1,WHAT2,LETOU
101 FORMAT(20A4,/,20A4,/,I5)
IF(LETOU.EQ.0)GOTO 999
ICASE=ICASE+1
READ(5,NUM)
IF(LETOU.GE.2) GOTO 110
WRITE(6,666)
WRITE(6,100)
100 FORMAT(37H PARAMETERS IN NAMELIST NUM VARIABLES)
110 CONTINUE
DIACH=SQRT(EPSC)*2.*RT
AC=EPSC*TWOPI*RT/2.
NINCH=NCHAI+NCHAZ
IF(NAORW.EQ.2) GOTO 108
IF(AITAC.EQ.0.) AITAC=1./AC
DO 109 I=1,NINCH
IF(MODECH.EQ.2) AIPCTF(I)=1.0
AIFU(I)=AC*AITAC*AIPCT(I)*AIPCTF(I)
AIOX(I)=AC*AITAC*AIPCT(I)*(1.-AIPCTF(I))
109 CONTINUE
RCWALL=RCRT*RT
WRITE(6,102)ICASE,WHAT1,WHAT2
102 FORMAT(1H1,60X,6H CASE ,I2,///,20X,20A4,/,20X,20A4,////)
MORDER = 1
LOOP=0
IF(ESPG.NE.1.)AND(MODECH.EQ.2)PG= ESPG*PRF(1)
IF(ESPG.EQ.1.) PG=.9*PRF(NINCH)
IF(MODECH.EQ.1) GOTO 103
GOTO 888
103 CONTINUE
WRITE(6,105)
105 FORMAT(1X,4HZONE,3X,9HEST.GAMMA,6X,6HEST.MW,9X,6HEST.TO,/)
WRITE(6,106) (I,AGAMGU(I),AMWGU(I),ATOGU(I),I=1,NINCH)
106 FORMAT(2X,I2,1X,3E15.6)
WRITE(6,107)
107 FORMAT(////)
ASTAR=TWOPI*RT*RT/2.
UNIV=SQRT(UNIVR*32.174)
SUM=0.

```

```

DO 104 I=1,NINCH
  MDTIFU(I)=MDTI(I)/(1.+OXFULE(I))
  MDTIOX(I)=MDTI(I)-MDTIFU(I)
  FOFGAM=SQRT(AGAMGU(I))*2./(AGAMGU(I)+1.))*((AGAMGU(I)+1.))/
    1(2.*AGAMGU(I)-2.))
  104 SUM=SUM+MDTI(I)/FOFGAM*SQRT(ATOUGU(I)/AMWGU(I))
  PG=UNIV*SUM/ASTAR
888 CONTINUE
  IF(NINCH.EQ.1) MTOTMX=0
  CALL THROAT
  GOTQ 1
999 CONTINUE
666 WRITE(6,666)
  FORMAT(IH1)
  STOP
  END

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SUBROUTINE THROAT
REAL MO1,MO2,MO,MDTI,MDTIFU,MDTIOX,ISPVAC,ISPVLD,MOLD,MOCH,MWG
DOUBLE PRECISION ACO(11)
DIMENSION PSI(200),AMACH(200),DUM1(3),DUM2(3),DRDPSV(10)
COMMON
  ,POCL(7),ERWT(4),RMIN(7),MODECH,RMINSQ(7)
  ,PGCH(7),CLP(10),RLIM,MORLI,NSPPG,ICASE,NCEC71,T(200)
  ,COMMON/ONE/NDIM,IHLF,RCRT,EPSC,MGORLI,NSPPG,ICASE,NCEC71,T(200)
  ,COMMON/TWO/YSAVE(200,4),XSAVE(200,4),CPG(20),YPSAV(200,4),MO
1 RT,RCWALL,GAMG(20),NCHAL,NCHAZ,PSI01(10),PSI02(10),TWOP,PSI12,MO
2 COMMON/THR/OXFULE(20),PG,TOG(20),RGAS(20),UNIVR,WIFU(20),
1 AIFU(20),RHOIFU(20),RIFU(20),TIFU(20),WIOX(20),AIOX(20),
2 RHOIOX(20),RIOX(20),TIOX(20),AIPCTE(20),ZCH,PI(20),DIACH,
3 TG(20),AG(20),WG(20),RHOG(20),RAD(20),MDTI(20),PRO(20),PRF(20),
4 PCTMO(20),MDTIFU(20),MDTIOX(20),MWG(20),AC,NAORW,MTOTMX
5 ,CDINJ(20)
  ,COMMON/CALC/HO,C,GAM,GAMSAV(200),K
  ,COMMON/LOAD/CST(20),VACIDI(20)
  ,COMMON/ZONE/KZONE,PGPSIA,OXFUL(20),LETOUT
  ,COMMON/MIXED/PMIX,PO(20)
EQUIVALENCE (YSAVE(201),PSI(1)),(YPSAV(601),AMACH(1))
EXTERNAL FCT,OUTP
RTSQ=RT*RT
URTSQ=1./RTSQ
NINCH=NCHAL+NCHAZ
IF(MTOTMX.GT.0) NCHAL=NINCH
IF(MTOTMX.GT.0) NCHAZ=0
NCHALP=NCHAL+1
NCHAZP=NCHAZ+1
NINCHP=NINCH+1
NCH1P2=NCHAL+2
K=0
MBRKPG=0
2 LOOP=LOOP+1
NINCH=NCHAL+NCHAZ
IF(MTOTMX.GT.0) NCHALP=2
IPLY=0
IF(MODECH.EQ.3,AND,LOOP.GT.7) GOTO 6
IF(MODECH.EQ.3) GOTO 21
IF(LOOP.LE.6) GOTO 446
PNOW=PG
IF(LOOP.GT.6) PG=PGCH(LOOP-1)
IF(MODECH.EQ.2,AND,LOOP.GT.7) PG=PNOW
IF(LOOP.GT.7) WRITE(6,445)
445 FORMAT(/,IX,80HCONVERGENCE ON PG DID NOT OCCUR IN 7 LOOPS. PARAM
1 ETERS DETERMINED NEVERTHELESS.,/)
IF(LOOP.GT.6) MBRKPG=MBRKPG+1
DO 448 I=2,6
DO 450 I=2,6

```

THRO 10  
 THRO 20  
 THRO 30  
 THRO 40  
 THRO 50  
 THRO 60  
 THRO 70  
 THRO 80  
 THRO 90  
 THRO 100  
 THRO 110  
 THRO 120  
 THRO 130  
 THRO 140  
 THRO 150  
 THRO 160  
 THRO 170  
 THRO 180  
 THRO 190  
 THRO 200  
 THRO 210  
 THRO 220  
 THRO 230  
 THRO 240  
 THRO 250  
 THRO 260  
 THRO 270  
 THRO 280  
 THRO 290  
 THRO 300  
 THRO 310  
 THRO 320  
 THRO 330  
 THRO 340  
 THRO 350  
 THRO 360  
 THRO 370  
 THRO 380  
 THRO 390  
 THRO 391  
 THRO 400  
 THRO 401  
 THRO 410  
 THRO 420  
 THRO 430  
 THRO 440  
 THRO 450  
 THRO 460  
 THRO 470

```

IGTRT=I
IGTRTM=11
IF(II.EQ.1) GOTO 450
IF(RMIN(I).GT.RY.AND.RMIN(II).LT.RT) GOTO 449
450 CONTINUE
448 CONTINUE
449 PG=PGCH(IGTRT)+(RT-RMIN(IGTRT))*(PGCH(IGTRT)-PGCH(IGTRTM))/
1 (RMIN(IGTRT)-RMIN(IGTRTM))
GOTO 447
446 CONTINUE
447 IF(LOOP.GT.6) GOTO 6
CONTINUE
IF(MODECH.EQ.1)GOTO 21
DO 20 I=1,NINCH
20 IF(LOOP.GT.1.AND.PRFL(I).LT.1.01*PG) PG=PRFL(I)-.01*PRFL(I)
21 NCLP=3
CALL CHAMBR
IF(MTOTMX.GT.0) NINCH=1
PGCH(LOOP)=PG
MOCH(LOOP)=MO
POCL(LOOP)=POG(1)*((1.+1./((4.*RCRT/GAMG(1)+1.))*2./((GAMG(1)+1.)))
1 *((GAMG(1))/(GAMG(1)-1.)))
1 RGAM=1.-2./((4.*RCRT+GAMG(1))+1./((16.*RCRT*RCRT+8.*GAMG(1))*RCRT
1 +GAMG(1)*GAMG(1)))
1 CLPDEC=POG(1)*((1.-((GAMG(1)-1.)/(GAMG(1)+1.))*RGAM)
1 *((GAMG(1))/(GAMG(1)-1.)))
IF(ERWT(4).NE.0.) CLP(1)=.5*(CLP(1)+CLPDEC)
L=0
IF(ERWT(3).GT.0.) GOTO 11
ERWT(1)=1./CLP(1)
ERWT(2)=1.-ERWT(1)
11 L=L+1
Y(1)=CLP(L)
Y(2)=PSI01(1)
DERY(1)=ERWT(1)
DERY(2)=ERWT(2)
J=0
CALL HPCG(PRMT,Y,DERY,NDIM,IHLF,FCT,OUTP,AUX)
DUM1(3)=PSI(J)
DUM1(2)=PSI(J-1)
DUM1(1)=PSI(J-2)
DUM2(3)=XSAVE(J)
DUM2(2)=XSAVE(J-1)
DUM2(1)=XSAVE(J-2)
CALL AITKEN(DUM1,DUM2,3,2,1.,RWALL)
RW(L)=RWALL
IF(L.EQ.2)GOTO 552
CLP(2)=1.05*CLP(1)
THRO 480
THRO 490
THRO 491
THRO 500
THRO 510
THRO 520
THRO 521
THRO 530
THRO 540
THRO 550
THRO 560
THRO 570
THRO 580
THRO 590
THRO 600
THRO 610
THRO 620
THRO 630
THRO 640
THRO 650
THRO 660
THRO 670
THRO 680
THRO 690
THRO 691
THRO 692
THRO 693
THRO 694
THRO 695
THRO 700
THRO 710
THRO 720
THRO 730
THRO 740
THRO 750
THRO 760
THRO 770
THRO 780
THRO 790
THRO 800
THRO 810
THRO 820
THRO 830
THRO 840
THRO 850
THRO 860
THRO 870
THRO 880
THRO 890
THRO 900

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```

552 GOTO 11
    MCUE=0
    CALL UPORD(RW,CLP,2,MORDER)
553 NCLPM1=NCLP-1
    NCLPM2=NCLP-2
    NCLPM3=NCLP-3
    PP=1.
    DRDP=(RW(2)-RW(1))/(CLP(2)-CLP(1))
    DRDPSV(NCLPM2)=DRDP
    IF(DRDP.GT.0.)PP=-1.
    CLP(NCLP)=CLP(1)+PP*.05*CLP(1)
    IF(NCLP.EQ.3) CLP(3)=(CLP(2)+CLP(1))*0.5
    IF(NCLP.EQ.3) GOTO 554
    IF(ABS(DRDP(NCLPM2)/ABS(DRDP(NCLPM3)))*.GT.1.) MCUE=1
    IF(ABS(DRDP(NCLPM2)/ABS(DRDP(NCLPM3)))*.GT.1.) GOTO 557
1   IF(MCUE.EQ.1) CLP(NCLP)=CLP(1)-PP*.02*CLP(1)
554 Y(1)=CLP(NCLP)
    Y(2)=PSI(1)
    DERY(1)=ERWT(1)
    DERY(2)=ERWT(2)
    J=0
    CALL HPCG(PRMT,Y,DERY,NDIM,IHLF,FCT,OUTP,AUX)
    DUM1(3)=PSI(J)
    DUM1(2)=PSI(J-1)
    DUM1(1)=PSI(J-2)
    DUM2(3)=XSAVE(J)
    DUM2(2)=XSAVE(J-1)
    DUM2(1)=XSAVE(J-2)
    CALL AITKEN(DUM1,DUM2,3,2,1.,RWALL)
    RW(NCLP)=RWALL
    IF(MCUE.EQ.0) GOTO 555
    CALL UPORD(RW,CLP,NCLP,MORDER)
    GOTO 556
555 DRDPN=(RW(NCLP)-RW(1))/(CLP(NCLP)-CLP(1))
    DRDP2=(RW(2)-RW(1))/(CLP(2)-CLP(1))
    IF(ABS(DRDPN/ABS(DRDPN)-DRDP2/ABS(DRDP2))*GT.1.) GOTO 557
    CALL UPORD(RW,CLP,NCLP,MORDER)
    NCLP=NCLP+1
    GOTO 553
557 RW(3)=RW(NCLP)
    CLP(3)=CLP(NCLP)
556 NCLPM1=3
    NCLP=4
    GOTO 10
3   NCLP=NCLP+1
    NCLPM1=NCLP-1
10  IPLY=IPLY+1
    CALL UPORD (CLP,RW,NCLPM1,MORDER)
    CALL PLYCF(CLP,RW,NCLPM1,ACO,2,NSTOPD)
    CLP(NCLP)=-ACO(2)/ACO(3)*.5

```

```

THRO 910
THRO 920
THRO 930
THRO 940
THRO 950
THRO 960
THRO 970
THRO 980
THRO 990
THRO 1000
THRO 1010
THRO 1020
THRO 1030
THRO 1040
THRO 1050
THRO 1060
THRO 1070
THRO 1080
THRO 1090
THRO 1100
THRO 1110
THRO 1120
THRO 1130
THRO 1140
THRO 1150
THRO 1160
THRO 1170
THRO 1180
THRO 1190
THRO 1200
THRO 1210
THRO 1220
THRO 1230
THRO 1240
THRO 1250
THRO 1260
THRO 1270
THRO 1280
THRO 1290
THRO 1300
THRO 1310
THRO 1320
THRO 1330
THRO 1340
THRO 1350
THRO 1360
THRO 1370
THRO 1380
THRO 1390
THRO 1400

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THRO1410  
THRO1420  
THRO1430  
THRO1440  
THRO1450  
THRO1460  
THRO1470  
THRO1480  
THRO1490  
THRO1500  
THRO1510  
THRO1520  
THRO1530  
THRO1540  
THRO1550  
THRO1560  
THRO1570  
THRO1580  
THRO1590  
THRO1600  
THRO1610  
THRO1620  
THRO1630  
THRO1640  
THRO1650  
THRO1660  
THRO1670  
THRO1680  
THRO1690  
THRO1700  
THRO1710  
THRO1711  
THRO1712  
THRO1713  
THRO1714  
THRO1715  
THRO1716  
THRO1717  
THRO1718  
THRO1720  
THRO1730  
THRO1740  
THRO1750  
THRO1760  
THRO1770  
THRO1780  
THRO1790  
THRO1800  
THRO1810  
THRO1820

```

Y(1)=CLP(NCLP)
Y(2)=PSI01(1)
DERY(1)=ERWT(1)
DERY(2)=ERWT(2)
J=0
CALL HPCG(PRMT,Y,DERY,NDIM,IHLF,FCT,OUTP,AUX)
DUM1(3)=PSI(J)
DUM1(2)=PSI(J-1)
DUM1(1)=PSI(J-2)
DUM2(3)=XSAVE(J)
DUM2(2)=XSAVE(J-1)
DUM2(1)=XSAVE(J-2)
CALL AITKEN(DUM1,DUM2,3,2,1.,RWALL)
RW(NCLP)=RWALL
CALL UPORD(RW,CLP,NCLP,MORDER)
IF(IPLY.GT.6) GOTO 7
GOTO 558
7 WRITE(6,701) LOOP
701 FORMAT(/,44H IPLY=7. UNSATISFACTORY CONVERGENCE IN LOOP=,I2,/)
GOTO 4
558 CONTINUE
NCLP=3
IF(IPLY.LT.2) GOTO 3
RWCHK=RW(1)+.0005*RW(1)
IF(RWCHK.LT.RW(2)) GOTO 3
IF(ABS(CLP(1)-CLP(2))/CLP(1).GT..010) GOTO 3
IF(ABS(RW(1)-RT)/RT.LE.0.0005) GOTO 6
4 RMIN(LOOP)=RW(1)
RMINSQ(LOOP)=RMIN(LOOP)*RMIN(LOOP)
URMNSQ(LOOP)=1./RMINSQ(LOOP)
IF(MODECH.EQ.3) GOTO 5
IF(MODECH.EQ.2.AND.LOOP.GT.4) GOTO 14
IF(MODECH.EQ.2.AND.LOOP.GE.3) PG=PG*(RW(1)/RT)**2
IF(MODECH.EQ.2.AND.LOOP.GE.3) GOTO 2
IF(MODECH.EQ.2.AND.LOOP.EQ.2) PG=PG*(RT-RW(1))*(PG-PGCH(1))/
1 (RW(1)-RMIN(1))
IF(MODECH.EQ.2.AND.LOOP.EQ.2) GOTO 2
IF(MODECH.EQ.2) PG=PG*RW(1)/RT
IF(MODECH.EQ.2) GOTO 2
IF(LOOP.GT.5) GOTO 14
PG=PG*(RW(1)/RT)**2
GOTO 2
14 CALL UPORD(RMINSQ,PGCH,LOOP,MORDER)
CALL AITKEN(RMINSQ,PGCH,LOOP,2,RTSQ,APGCH)
PG=APGCH
GOTO 2
5 IF(LOOP.GT.5) GOTO 8
M0=M0*(RT/RW(1))**2
GOTO 2
8 CALL UPORD(URMNSQ,MOCH,LOOP,MORDER)

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CALL AITKEN(URMNSQ,MOCH,LOOP,2,URTSQ,AMO)
MO=AMO
GOTO 2
6 RWCALC=RW(1)
PGCALC=PG
CLPCAL=CLP(1)
444 CONTINUE
NNINCH=NCHAL+NCHAZ
WRITE(6,222) LOOP,RCRT,MODECH,MGORLI,VAORW,NCEC71, NSPPG
1 MTOTMX=LETOUT,NNINCH
222 FORMAT(2X,5HLOOP=,I2,4X,6HRC/RT=,E15.6,4X,7HMODECH=,I2,4X,7HMGORLI
1=,I2,4X,6HNAORW=,I2,4X,7HNCEC71=,I2,/,38X,
2 6HNSPPG=,I2,5X,7HMTOTMX=,I2,4X,7HLETOUT=,I2,3X,6HNNINCH=,I2,
3/)
WRITE(6,111) RT,RWCALC,PGCALC,EPSC,CLPCAL
111 FORMAT(//,5H RT=,E15.6,5X,7HRTCALC=,E15.6,5X,3HPG=, E15.6,5X,
1 5HSPSC=,E15.6,5X,4HCLP=, E15.6,/)
WRITE(6,300)
300 FORMAT(//,54X,24HINJECTOR PARAMETERS,/)
223 FORMAT(2X,18HZONE PSI LIMITS =,20E10.4)
IF(NCHAZ.EQ.0) GOTO 225
WRITE(6,223) (PSIO2(I),I=1,NCHAZP)
225 CONTINUE
WRITE(6,226)
226 FORMAT(//,5H ZONE,6X,2HPI,12X,4HTIFU,10X,4HAIFU,10X,4HWIFU,10X,
1 6HHRHOFU,8X,4HRIFU,10X,6HMDTIFU,8X,3HPRF,/,25X,4HTIOX,10X,
2 4HAIIOX,10X,4HWIOX,10X,6HHRHIOX,8X,4HRIOX,10X,6HMDTIOX,8X,3HPRO,/)
DO 301 I=1,NNINCH
301 WRITE(6,302) I,PI(I),TIFU(I),AIFU(I),WIFU(I),RHOIFU(I),RIFU(I),
2 MDTIFU(I),PRF(I),I,TIOX(I),WIOX(I),RHOIOX(I),RIOX(I),
2 MDTIOX(I),PRO(I)
302 FORMAT(15,8E14.6,/,15,14X,7E14.6,/)
305 IF(MODECH.EQ.1) WRITE(6,305)
FORMAT(1H1)
IF(MTOTMX.EQ.0) WRITE(6,303)
IF(MTOTMX.GT.0) WRITE(6,304)
303 FORMAT(//,53X,25HBURNED GAS PARAMETERS,/)
304 FORMAT(//,54X,24H MIXED GAS PARAMETERS,/)
WRITE(6,221)
221 FORMAT(//,6X,3HPOG,11X,3HTOG,11X,3HCPG,11X,4HGAMG,10X,2HTG,12X,2HAG,
1 12X,2HWG,12X,4HRHOG,10X,4HMDTI,/)
IF(MTOTMX.GT.0) NNINCH=1
IF(LOOP.LE.7) GOTO 18
TOTMO=0
DO 230 I=1,NNINCH
230 TOTMO=TOTMO+MDTI(I)
MO=TOTMO
18 CONTINUE
DO 227 I=1,NNINCH

```

THRO1830  
 THRO1840  
 THRO1850  
 THRO1860  
 THRO1870  
 THRO1880  
 THRO1890  
 THRO1900  
 THRO1910  
 THRO1920  
 THRO1930  
 THRO1940  
 THRO1950  
 THRO1960  
 THRO1970  
 THRO1980  
 THRO1990  
 THRO2000  
 THRO2010  
 THRO2020  
 THRO2030  
 THRO2040  
 THRO2050  
 THRO2060  
 THRO2070  
 THRO2080  
 THRO2090  
 THRO2100  
 THRO2110  
 THRO2120  
 THRO2130  
 THRO2140  
 THRO2150  
 THRO2151  
 THRO2152  
 THRO2160  
 THRO2170  
 THRO2180  
 THRO2190  
 THRO2200  
 THRO2210  
 THRO2220  
 THRO2230  
 THRO2240  
 THRO2250  
 THRO2260  
 THRO2270  
 THRO2280  
 THRO2290  
 THRO2300

```

DTI=MDTI(I)
IF(MTOTMX.GT.0) DTI=MO
227 WRITE(6,228)POG(I),TOG(I),CPG(I),GAMG(I),TG(I),AG(I),WG(I),RHOG(I)
1 DTI
228 FORMAT(9E14.6)
IF(MTOTMX.GT.0) WRITE(6,443) PMIX
443 FORMAT(//,2X,29HSTATIC PRESS. OF MIXED GASES=E15.6)
IF(MTOTMX.GT.0) WRITE(6,442)
442 FORMAT(2X,51HTOTAL PRESS. OF PRODUCTS IN EACH ZONE BEFORE MIXING)
IF(MTOTMX.GT.0) WRITE(6,441) (PO(I), I=1,NNINCH)
441 FORMAT(10E15.6)
*****
C **PERFORMANCE SECTION.**
C *****
C Y(1)=CLP(1)
Y(2)=PSIOI(1)
DERY(1)=ERWT(1)
DERY(2)=ERWT(2)
J=0
CALL HPCG(PRMT,Y,DERY,NDIM,IHLF,FCT,OUTP,AUX)
DUM1(3)=PSI(J)
DUM1(2)=PSI(J-1)
DUM1(1)=PSI(J-2)
DUM2(3)=XSAVE(J)
DUM2(2)=XSAVE(J-1)
DUM2(1)=XSAVE(J-2)
CALL AITKEN(DUM1,DUM2,3,2,1.,RWALL)
JM1=J-1
JM2=J-2
I=1
YSAVE(1,4)=TWOPI*XSAVE(2)*XSAVE(2)/8.
DO 50 I=2,JM2
YSAVE(1,4)=TWOPI/8.*((XSAVE(I+1)+XSAVE(I))*2-(XSAVE(I)+XSAVE(I-1))
1 )#2)
YSAVE(JM1,4)=TWOPI*RWALL*RWALL/2.-TWOPI/8.*(XSAVE(JM1)+XSAVE(JM2)
1 )#2)
ISPVAC=YSAVE(2,2)/2.*YSAVE(1,3)+YSAVE(1,1)*YSAVE(1,4)/MO
DO 51 I=2,JM2
IPI=I+1
IM1=I-1
51 ISPVAC=ISPVAC+YSAVE(IP1,2)-YSAVE(IM1,2))/2.*YSAVE(I,3)
+YSAVE(I,1)*YSAVE(I,4)/MO
ISPVAC=ISPVAC+(1.-.5*YSAVE(JM1,2) -.5*YSAVE(JM2,2))*YSAVE(JM1,3)
1 +YSAVE(JM1,1)*YSAVE(JM1,4)/MO
RADT(1)=0.
RADT(2)=RWALL
IF(MTOTMX.GT.0) GOTO 59
IF(NCHAL.EQ.1.AND.NCHA2.EQ.0)GOTO 59
DO 56 I=1,NCHALP
DO 55 I=1,J

```

THRO2310  
 THRO2320  
 THRO2330  
 THRO2340  
 THRO2350  
 THRO2360  
 THRO2370  
 THRO2380  
 THRO2390  
 THRO2400  
 THRO2410  
 THRO2420  
 THRO2430  
 THRO2440  
 THRO2450  
 THRO2460  
 THRO2470  
 THRO2480  
 THRO2490  
 THRO2500  
 THRO2510  
 THRO2520  
 THRO2530  
 THRO2540  
 THRO2550  
 THRO2560  
 THRO2570  
 THRO2580  
 THRO2590  
 THRO2600  
 THRO2610  
 THRO2620  
 THRO2630  
 THRO2640  
 THRO2650  
 THRO2660  
 THRO2670  
 THRO2680  
 THRO2690  
 THRO2700  
 THRO2710  
 THRO2720  
 THRO2730  
 THRO2740  
 THRO2750  
 THRO2760  
 THRO2770  
 THRO2780  
 THRO2790  
 THRO2800



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55  IF(YSAVE(I,2).GE.PSI01(II)) RADT(II)=XSAVE(I)
56  IF(YSAVE(I,2).GE.PSI01(II)) GOTO 56
    CONTINUE
    IF(NCHA2.EQ.0) RADT(NCHA1P)=RWALL
    IF(NCHA2.EQ.0) GOTO 59
    RADT(NCHA1P2)=RWALL
    IF(NCHA2.EQ.1)GOTO 59
    DO 58 II=2,NCHA2P
    III=NCHA1P+II-1
    DO 57 I=1,J
    IF(YSAVE(I,2).GE.PSI02(III))RADT(III)=XSAVE(I)
    IF(YSAVE(I,2).GE.PSI02(III))
        GOTO 58
    CONTINUE
    CONTINUE
    RADT(II)=RWALL
    CONTINUE
    MOLD=0.
    DO 64 I=1,NINCH
    IP=I+1
    ASTAR=TWOPI/2.*(RADT(IP)*RADT(IP)-RADT(I)*RADT(I))
    PIR=GAMG(I)/RGAS(I)*(2./(GAMG(I)+1.))*((GAMG(I)+1.)/(GAMG(I)-1.))
    IF(NCECT1.GE.2) MOLD=MOLD+ASTAR*PG/CST(I)
    IF(NCECT1.LT.2) MOLD=MOLD+ASTAR*POG(I)*SQRT(PIR/TOG(I))
    CONTINUE
    CD=MO/MOLD
    WTP0=0.
    DO 52 I=2,NCHA1P
    IM1=I-1
    WTP0=POG(IM1)*(PSI01(I)-PSI01(IM1))+WTP0
    IF(NCHA2.EQ.0)GOTO 54
    DO 53 I=2,NCHA2P
    IM1=NCHA1+I-1
    WTP0=POG(IM1)*(PSI02(I)-PSI02(I-1))+WTP0
    CONTINUE
    CSTAR=WTP0*TWOPI*RWALL*RWALL/2./MO
    CSTID=WTP0*TWOPI*RWALL*RWALL/2./MOLD
    ISPVLD=0.
    IF(NCECT1.GT.1) GOTO 70
    NCHA1=NCHA1
    IF(MTOTMX.GT.0)NCHA1=NINCH
    DO 60 I=1,NCHA1
    TOT0=1./I.*(GAMG(I)-1.)/2.)
    TEMP=TOG(I)*TOT0
    U=SQRT(GAMG(I)*RGAS(I)*TEMP)
    P=POG(I)*TOT0*(GAMG(I)/(GAMG(I)-1.))
    IK=I+1
    DPSI=PSI01(IK)-PSI01(I)
    DAREA=TWOPI/2.*(RADT(IK)*RADT(IK)-RADT(I)*RADT(I))
    ISPVLD=ISPVLD+DPSI*U*P*DAREA/MOLD
60

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THRO2810
THRO2820
THRO2830
THRO2840
THRO2850
THRO2860
THRO2870
THRO2880
THRO2890
THRO2900
THRO2910
THRO2920
THRO2930
THRO2940
THRO2950
THRO2960
THRO2970
THRO2980
THRO2990
THRO3000
THRO3010
THRO3020
THRO3030
THRO3040
THRO3050
THRO3060
THRO3070
THRO3080
THRO3090
THRO3100
THRO3110
THRO3120
THRO3130
THRO3140
THRO3150
THRO3160
THRO3170
THRO3180
THRO3190
THRO3200
THRO3210
THRO3220
THRO3230
THRO3240
THRO3250
THRO3260
THRO3270
THRO3280
THRO3290
THRO3300

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```

IF(NCHA2.EQ.0)GOTO 62
IK=1
DO 61 I=NCHAIP,NINCH
IKE=I+1
TOT0=1./((1.+(GAMG(I)-1.)/2.))
TEMP=TOG(I)*TOT0
U=SQRT(GAMG(I)*RGAS(I)*TEMP)
P=POG(I)*TOT0*(GAMG(I)/(GAMG(I)-1.))
IK=IK+1
IKM=IK-1
DPSI=PSIO2(IK)-PSIO2(IKM)
DAREA=TSWOI/2.*(RADT(IKE)*RADT(IKE)-RADT(I)*RADT(I))
ISPVID=ISPVID+DPSI*U+P*DAREA/MO1D
61 CONTINUE
GOTO 71
DO 72 I=1,NINCH
ISPVID=ISPVID+VAC1DI(I)*MDTI(I)/MO*32.174
72 CONTINUE
VAQVID=ISPVID+ISPVID
FORMAT(IH1,59X,12HTHROAT PLANE,///)
68 WRITE(6,68)
CSOCID=CSSTAR/CSTID
WRITE(6,65)
65 FORMAT(
1 13X,3HGAM,/)
WRITE(6,66) (XSAVE(I),YSAVE(I,1),YSAVE(I,2),T(I),YSAVE(I,3),
1 YPSAV(I,4),GAMSAV(I),I=1,J)
66 FORMAT(7E15.6)
DUM2(3)=YSAVE(J,1)
DUM2(2)=YSAVE(JM1,1)
DUM2(1)=YSAVE(JM2,1)
CALL AITKEN(DUM1,DUM2,3,2,1.,PWAL)
DUM2(3)=T(J)
DUM2(2)=T(JM1)
DUM2(1)=T(JM2)
CALL AITKEN(DUM1,DUM2,3,2,1.,TWAL)
DUM2(3)=YSAVE(J,3)
DUM2(2)=YSAVE(JM1,3)
DUM2(1)=YSAVE(JM2,3)
CALL AITKEN(DUM1,DUM2,3,2,1.,WWAL)
DUM2(3)=YPSAV(J,4)
DUM2(2)=YPSAV(JM1,4)
DUM2(1)=YPSAV(JM2,4)
CALL AITKEN(DUM1,DUM2,3,2,1.,EMWAL)
DUM2(3)=GAMSAV(J)
DUM2(2)=GAMSAV(JM1)
DUM2(1)=GAMSAV(JM2)
CALL AITKEN(DUM1,DUM2,3,2,1.,GAMWAL)
PSIWAL=1.
WRITE(6,69)

```

```

THRO3310
THRO3320
THRO3330
THRO3340
THRO3350
THRO3360
THRO3370
THRO3380
THRO3390
THRO3400
THRO3410
THRO3420
THRO3430
THRO3440
THRO3450
THRO3460
THRO3470
THRO3480
THRO3490
THRO3500
THRO3510
THRO3520
THRO3530
THRO3540
THRO3550
THRO3560
THRO3570
THRO3580
THRO3590
THRO3600
THRO3610
THRO3620
THRO3630
THRO3640
THRO3650
THRO3660
THRO3670
THRO3680
THRO3690
THRO3700
THRO3710
THRO3720
THRO3730
THRO3740
THRO3750
THRO3760
THRO3770
THRO3780
THRO3790
THRO3800

```

```

69 FORMAT(IX,11HTHROAT WALL)
WRITE(6,66)RWALL,PWAL,PSIWAL,TWAL,WWAL,EMWAL,GAMWAL
WRITE(6,67)
67 FORMAT(1H1,60X,11HPERFORMANCE,///)
ISPVAC=ISPVAC/32.174
ISPVID=ISPVID/32.174
WRITE(6,63)ISPVAC,CSTAR,ISPVID,CSTID,MO,M01D,CD,VAQVID,CSOCID
63 FORMAT(//,48X,39HTHROAT ISPVAC,LBF-SEC/LBM CSTID,FT/SEC,/,53X,
12E17.6,/,48X,39HTHROAT ISPVAC,LBF-SEC/LBM CSTID,FT/SEC,/,53X,
22E17.6,/,48X,13HMO,LBF-SEC/FT,9X,15HMOID,LBF-SEC/FT,/,46X,E16.6,
36X,E16.6,/,48X,25HCD,DISCHARGE COEFFICIENT=,E15.6,/,48X,21HTHROA
4T ISPVAC/ISPVID=,E15.6,/,48X,12HCSTAR/CSTID=,E15.6,/,1H1)
RETURN
END
THRO3810
THRO3820
THRO3830
THRO3840
THRO3841
THRO3842
THRO3850
THRO3860
THRO3870
THRO3880
THRO3890
THRO3900
THRO3910
THRO3920

```

```

SUBROUTINE CHAMBR
REAL M01,M02,M0,MDTI,MWG,MOCH,MDTIFU,MDTIOX
DIMENSION TGA(20,10),SUMAGG(20),PII(20)
COMMON PRMT(6),DERY(4),AUX(16,4),Y(4),RW(10)
      ,POCL(7),ERWT(4),RMIN(7),MODECH,RMINSQ(7),URMNSQ(7)
      ,PGCH(7),IHLF,RCRT,EPSC,MGORLI,NSPPG,ICASE,NCEC71,T(200)
      ,COMMON/ONE/NDIM,IHVE(200,4),XSAVE(200),J,CPG(20),POG(20),YPSAV(200,4),
1      ,RCWALL,GAMG(20),NCHAL,NCHAZ,PSI01(10),PSI02(10),TWOP1,PSI12,M0
2      ,COMMON/THR/OXFULE(20),PG,TGG(20),RGAS(20),WIOX(20),AIOX(20),
1      ,AIFU(20),RHOIFU(20),RIFU(20),TIFU(20),UNIVR,WIFU(20),
2      ,RHOIOX(20),RIOX(20),TIOX(20),AIPCTF(20),ZCH,PI(20),DIACH,
3      ,TG(20),AG(20),WG(20),RHOG(20),RAD(20),MDTI(20),PRO(20),PRF(20),
4      ,PCTMO(20),MDTIFU(20),MDTIOX(20),MWG(20),AC,NAORW,MTOTMX
5      ,CDINJ(20)
      ,COMMON/CALC/HO,C,GAM,GAMSAV(200),K
      ,COMMON/MIXED/PMIX,P0(20)
      ,NINCH=NCHAL+NCHAZ
      ,FNINCH=NINCH
      ,NCHALP=NCHAL+1
      ,NCHAZP=NCHAZ+1
      ,NINCHP=NINCH+1
      ,LOOPC=1
      ,NOAI=1
      ,IF(MODECH.EQ.1)PIAVG=1.01*PG
      ,IF(MODECH.EQ.2)CALL PRSPFD(NOAI,NINCH,PIAVG)
      ,IF(MODECH.EQ.3)CALL PGFIX
      ,IF(MODECH.EQ.3)PIAVG=1.01*PG
      ,M0=0.
32 DO 32 I=1,NINCH
      MO=MDTI(I)+MO
      DO 1 I=1,NINCHP
      YG(I)=0.
      WG(I)=0.
      AG(I)=0.
      IF(MODECH.EQ.1)PRF(I)=0.
      IF(MODECH.EQ.1)PRO(I)=0.
      IF(RHOG(I)=0.
1      ,IF(MODECH.EQ.3)GOTO 3
      ,CALL EQUILB(NINCH)
3      DO 4 I=1,NINCH
      ,IF(NINCH.GT.1)NSPPG=0
      ,IF(NSPPG.EQ.1.AND.MODECH.EQ.1)CALL SPPG(PIAVG)
      ,IF(NSPPG.EQ.1.AND.MODECH.EQ.3)CALL SPPG(PIAVG)
      ,PI(I)=1.01*PG
      ,IF(MODECH.EQ.2)PI(I)=PIAVG
      ,IF(MGORLI.EQ.2)GOTO 40
      ,RHOIFU(I)=PI(I)/RIFU(I)/TIFU(I)
      ,IF(OXFULE(I).EQ.0.)RHOIOX(I)=0.

```

CHAM 10  
 CHAM 20  
 CHAM 30  
 CHAM 40  
 CHAM 50  
 CHAM 60  
 CHAM 70  
 CHAM 80  
 CHAM 90  
 CHAM 100  
 CHAM 110  
 CHAM 120  
 CHAM 130  
 CHAM 140  
 CHAM 141  
 CHAM 150  
 CHAM 160  
 CHAM 170  
 CHAM 180  
 CHAM 190  
 CHAM 200  
 CHAM 210  
 CHAM 220  
 CHAM 230  
 CHAM 240  
 CHAM 250  
 CHAM 260  
 CHAM 270  
 CHAM 280  
 CHAM 290  
 CHAM 300  
 CHAM 310  
 CHAM 320  
 CHAM 330  
 CHAM 340  
 CHAM 350  
 CHAM 360  
 CHAM 370  
 CHAM 380  
 CHAM 390  
 CHAM 400  
 CHAM 410  
 CHAM 420  
 CHAM 430  
 CHAM 440  
 CHAM 450  
 CHAM 460  
 CHAM 470  
 CHAM 480  
 CHAM 490

```

40 IF(OXFULE(I).EQ.0.) GOTO 40
   RHOIOX(I)=PI(I)/RIOX(I)/TIOX(I)
   CONTINUE
   IF(NAORW.EQ.1)WIFU(I)=MDTIFU(I)/AIFU(I)/RHOIFU(I)
   IF(NAORW.EQ.2)AIFU(I)=MDTIFU(I)/WIFU(I)/RHOIFU(I)
   IF(OXFULE(I).EQ.0.) WIOX(I)=0.
   IF(OXFULE(I).EQ.0.) AIOX(I)=0.
   IF(OXFULE(I).EQ.0.) GOTO 4
   IF(NAORW.EQ.1)WIOX(I)=MDTIOX(I)/AIOX(I)/RHOIOX(I)
   IF(NAORW.EQ.2)AIOX(I)=MDTIOX(I)/WIOX(I)/RHOIOX(I)
   CONTINUE
4 GOTO 5
10 DO 2 I=1,NINCH
2 PI(I)=PG+(PI(I)-PG)*(SUMAG/AC)**2
   IF(MODECH.NE.2) GOTO 22
   DO 23 I=1,NINCH
   IF(PRF(I).LE.PI(I)) PI(I)=.91*PRF(I)
23 CONTINUE
22 PIAVG=PI(I)
   IF(NINCH.EQ.1)GOTO 27
   DO 25 I=2,NINCH
25 PIAVG=PIAVG+PI(I)
   PIAVG=PIAVG/FNINCH
251 IF(PIAVG.LT.PG)PIAVG=PG+.002*PG
26 DO 26 I=1,NINCH
27 PI(I)=PIAVG
   CONTINUE
   IF(NINCH.EQ.1.AND.PIAVG.LE.PG)PI(I)=PG+.002*PG
   PIAVG=PI(I)
   DO 24 I=1,NINCH
   IF(MGORL.EQ.2) GOTO 41
   RHOIFU(I)=PI(I)/RIFU(I)/TIFU(I)
   IF(OXFULE(I).EQ.0.) RHOIOX(I)=0.
   IF(OXFULE(I).EQ.0.) GOTO 41
   RHOIOX(I)=PI(I)/RIOX(I)/TIOX(I)
41 CONTINUE
   IF(NAORW.EQ.2)AIFU(I)=MDTIFU(I)/WIFU(I)/RHOIFU(I)
   IF(OXFULE(I).EQ.0.) AIOX(I)=0.
   IF(OXFULE(I).EQ.0.) GOTO 24
   IF(NAORW.EQ.2)AIOX(I)=MDTIOX(I)/WIOX(I)/RHOIOX(I)
24 CONTINUE
   IF(MODECH.EQ.2) CALL PRSPFD(NOAI,NINCH,PIAVG)
   DO 20 I=1,NINCH
   IF(NAORW.EQ.1)WIFU(I)=MDTIFU(I)/AIFU(I)/RHOIFU(I)
   IF(NAORW.EQ.2)WIOX(I)=0.
   IF(OXFULE(I).EQ.0.) GOTO 20
   IF(NAORW.EQ.1)WIOX(I)=MDTIOX(I)/AIOX(I)/RHOIOX(I)
20 CONTINUE
5 DO 6 I=1,NINCH

```

```

CHAM 500
CHAM 510
CHAM 520
CHAM 530
CHAM 540
CHAM 550
CHAM 560
CHAM 570
CHAM 580
CHAM 590
CHAM 600
CHAM 610
CHAM 620
CHAM 630
CHAM 631
CHAM 632
CHAM 633
CHAM 634
CHAM 635
CHAM 640
CHAM 650
CHAM 660
CHAM 670
CHAM 680
CHAM 690
CHAM 700
CHAM 710
CHAM 720
CHAM 730
CHAM 740
CHAM 750
CHAM 760
CHAM 770
CHAM 780
CHAM 790
CHAM 800
CHAM 810
CHAM 820
CHAM 830
CHAM 840
CHAM 850
CHAM 860
CHAM 870
CHAM 880
CHAM 890
CHAM 900
CHAM 910
CHAM 920
CHAM 930
CHAM 940

```

```

TG(I)=TGA(I)-WG(I)*WG(I)/2./CPG(I)
TGA(I,LOOPC)=TG(I)
RHOG(I)=PG/RGAS(I)/TG(I)
BOB=-(WIFU(I)+OXFULE(I)*WIOX(I))/(1.+OXFULE(I))
COC=(PG-PI(I))/RHOG(I)
WG(I)=(-BOB+SQRT(BOB*BOB-4.*COC))*0.5
6 AG(I)=MDTI(I)/RHOG(I)/WG(I)
IF(LOOPC.GT.1)GOTO 7
LOOPC=LOOPC+1
GOTO 5
16 LOOPC=LOOPC+1
GOTO 5
7 LOOPCM=LOOPC-1
DO 8 I=1,NINCH
IF(ABS(TGA(I,LOOPC)-TGA(I,LOOPCM))/TGA(I,LOOPC).GT..0010)GOTO 16
8 CONTINUE
SUMAG=0.
DO 9 I=1,NINCH
SUMAG=SUMAG+AG(I)
IF(ABS(SUMAG-AC)/AC.LT..0010)GOTO 11
SUMAGG(NOAI)=SUMAG
PII(NOAI)=PIAVG
31 NOAI=NOAI+1
LOOPC=1
IF(NOAI.GT.20)GOTO 17
GOTO 10
11 CONTINUE
M01=0.
M02=0.
CONVERGENCE ACHIEVED ON TG AND SUMAG
C
C
C
DO 12 I=1,NCHAI
M01=RHOG(I)*AG(I)*WG(I)+M01
IF(NCHAI2.EQ.0)GOTO 28
DO 13 I=NCHAI2,NINCH
M02=RHOG(I)*AG(I)*WG(I)+M02
28 M02=0.
DO 34 I=1,NINCH
M0=MO+MDTI(I)
34 RAD(1)=SQRT(2.*AG(1)/TWOPI)
IF(NINCH.EQ.1)GOTO 29
DO 14 I=2,NINCH
IM1=I-1
14 RAD(I)=SQRT(2.*AG(I)/TWOPI+RAD(IM1)*RAD(IM1))
29 CONTINUE
DO 18 I=1,NINCH
GOGM1=GAMG(I)/(GAMG(I)-1.)
IF(MODECH.GT.1)GOTO 21
PRF(I)=PIAVG+.5*(MDTI(I)/AIFU(I)/.7)**2/RHOIFU(I)

```

CHAM 950  
 CHAM 960  
 CHAM 970  
 CHAM 980  
 CHAM 990  
 CHAM1000  
 CHAM1010  
 CHAM1020  
 CHAM1030  
 CHAM1040  
 CHAM1050  
 CHAM1060  
 CHAM1070  
 CHAM1080  
 CHAM1090  
 CHAM1100  
 CHAM1110  
 CHAM1120  
 CHAM1130  
 CHAM1140  
 CHAM1150  
 CHAM1160  
 CHAM1170  
 CHAM1180  
 CHAM1190  
 CHAM1200  
 CHAM1210  
 CHAM1220  
 CHAM1230  
 CHAM1240  
 CHAM1250  
 CHAM1260  
 CHAM1270  
 CHAM1280  
 CHAM1290  
 CHAM1300  
 CHAM1310  
 CHAM1320  
 CHAM1330  
 CHAM1340  
 CHAM1350  
 CHAM1360  
 CHAM1370  
 CHAM1380  
 CHAM1390  
 CHAM1400  
 CHAM1410  
 CHAM1420  
 CHAM1430  
 CHAM1440

```

IF( OXFULE(I).EQ.0.) PRO(I)=0.
IF( OXFULE(I).EQ.0.) GOTO 21
PRO(I)=PIAVG+.5*(MDTIOX(I)/AIOX(I)/.7)**2/RHOIOX(I)
21 POG(I)=PG*(TOG(I)/TG(I))*GOGMI
18 PO(I)=POG(I)
PSIO1(I)=0.
DO 15 I=2,NCHAIP
15 PSIO1(I)=PSIO1(I-1)+RHOG(I-1)*AG(I-1)*WG(I-1)/MO
PSI12=PSIO1(NCHAIP)
PSIO2(I)=PSIO1(NCHAIP)
IF(NCHA2.LT.1)GOTO 17
DO 19 I=2,NCHA2P
19 NCHAIM=NCHAI+I-1
PSIO2(I)=PSIO2(I-1)+RHOG(NCHAIM)*AG(NCHAIM)*WG(NCHAIM)/MO
17 CONTINUE
33 IF(NOA1.GT.20) WRITE(6,33) PG,PIAVG,SUMAG,AC
33 FORMAT(IX,41HCONVERGENCE FAILED. PG,PIAVG,SUMAG,AC ARE,/,4E15.6,/)
RETURN
50 CPMIX=0.
WMMIX=0.
TOMIX=0.
VMIX=0.
PSIO1(1)=0.
PSIO1(2)=1.
PSI12=1.
PSIO2(1)=1.
AG(1)=SUMAG
DO 51 I=1,NINCH
51 CPMIX=CPMIX+CPG(I)*MDTI(I)/MO
VMIX=VMIX+MDTI(I)*WG(I)/MO
WMMIX=WMMIX+MDTI(I)/MO/MWG(I)
WMMIX=1./WMMIX
RGAS(1)=UNIVR*32.174/WMMIX
GAMG(1)=CPMIX/(CPMIX-RGAS(1))
REW=GAMG(1)
MWG(1)=WMMIX
DO 52 I=1,NINCH
52 TOMIX=TOMIX+CPG(I)*TOG(I)*MDTI(I)
CPG(1)=CPMIX
TOG(1)=TOMIX/CPMIX/MO
GOGMIX=REW/(REW-1.)
B=-VMIX-PG*SUMAG/MO
A=.5*(REW+1.)/REW
C=TOG(1)*RGAS(1)
VMIX=(-B-SQRT(B*B-4.*A*C))/A*.5
WG(1)=VMIX
RHOG(1)=MO/SUMAG/VMIX
TG(1)=TOG(1)-VMIX*VMIX/CPMIX*.5
PMIX=RHOG(1)*TG(1)*RGAS(1)

```

```

CHAM1450
CHAM1460
CHAM1470
CHAM1480
CHAM1490
CHAM1500
CHAM1510
CHAM1520
CHAM1530
CHAM1540
CHAM1550
CHAM1560
CHAM1570
CHAM1580
CHAM1590
CHAM1600
CHAM1610
CHAM1620
CHAM1630
CHAM1640
CHAM1650
CHAM1660
CHAM1670
CHAM1680
CHAM1690
CHAM1700
CHAM1710
CHAM1720
CHAM1730
CHAM1740
CHAM1750
CHAM1760
CHAM1770
CHAM1780
CHAM1790
CHAM1800
CHAM1810
CHAM1820
CHAM1830
CHAM1840
CHAM1850
CHAM1860
CHAM1870
CHAM1880
CHAM1890
CHAM1900
CHAM1910
CHAM1920
CHAM1930
CHAM1940

```

POG(1)=PMIX\*(TOG(1)/TG(1))\*GOGMIX  
RETURN  
END

CHAM1950  
CHAM1960  
CHAM1970



```

SUBROUTINE PGFIX
REAL MOCH, MO, MDTI, MDTIFU, MDTIOX, MWG
COMMON
  , PRMT(6), DERY(4), AUX(16,4), Y(4), RW(10)
  , POCL(7), DERWT(4), RMIN(7), MODECH, RMINSQ(7), URMSQ(7)
  , PGCH(7), CLP(10), RLIM, MORL, NSPPG, ICASE, NCEC(7), T(200)
  , COMMON/ONE/NDIM, IHLF, RCRY, EPSC, MGORLI, CPG(20), POG(20), YPSAV(200,4), MO
  , COMMON/TWO/YSAVE(200,4), XSAVE(200), J, PSIO(10), PSIO2(10), TWOP, PSI12, MO
  , COMMON/THR/OXFULE(20), NCHAI, NCHAZ, PSIO1(10), POG(20), UNIVR, WIFU(20),
  , COMMON/FOUR/RHOIFU(20), RHOIX(20), TIFU(20), WJX(20), AIOX(20),
  , COMMON/FIVE/AIFU(20), RHOFU(20), TIOX(20), AIPCTF(20), ZCH, PI(20), DIACH,
  , COMMON/SIX/RG(20), AG(20), WG(20), RHOG(20), RAD(20), MDTI(20), PRO(20), PRF(20),
  , COMMON/SEVEN/PCIMO(20), MDTIFU(20), MDTIOX(20), MWG(20), AC, NADRW, MTOTMX
  , CDINJ(20)
  , NINCH=NCHAI+1+NCHAZ
  , IF(LOOP.EQ.1) CALL EQU LIB(NINCH)
  , IF(LOOP.EQ.1) GOTO 1
  , IF(MTOTMX.GT.0.AND.LOOP.GT.1) CALL EQU LIB(NINCH)
  , GOTO 3
1  ASTAR=TWOPI*RT*RT/2.
  UNIVR=SQRT(UNIVR*32.174)
  SUM=0.
  DO 2 I=1,NINCH
    FOGAM=SQRT(GAMG(I))*(2./(GAMG(I)+1.))*((GAMG(I)+1.)/(2.*GAMG(I)
    -2.))
  2  SUM=SUM+PCIMO(I)/FOGAM*SQRT(TOG(I)/MWG(I))
  MO=PG*ASTAR/UNIV/SUM
  DO 4 I=1,NINCH
    MDTI(I)=MO*PCIMO(I)
    MDTIFU(I)=MDTI(I)/(1.+OXFULE(I))
    MDTIOX(I)=MDTI(I)-MDTIFU(I)
  4  RETURN
END

```

```

PGFI 10
PGFI 20
PGFI 30
PGFI 40
PGFI 50
PGFI 60
PGFI 70
PGFI 80
PGFI 90
PGFI 100
PGFI 110
PGFI 120
PGFI 130
PGFI 131
PGFI 140
PGFI 150
PGFI 160
PGFI 170
PGFI 180
PGFI 190
PGFI 200
PGFI 210
PGFI 220
PGFI 230
PGFI 240
PGFI 250
PGFI 260
PGFI 270
PGFI 280
PGFI 290
PGFI 300
PGFI 310
PGFI 320

```

```

SUBROUTINE PRSPFD(NOAI,NINCH,PIAVG)
INJECTOR DISCHARGE COEFFS. = .7 ARE USED UNLESS READ BY NUM.
THIS OPTION MAY NOT BE USED IF INJECTOR VELOCITIES ARE
SPECIFIED AND IS NOT STRICTLY VALID FOR GAS INJECTION.

REAL MDTI,MDTIFU,MDTIOX,MWG
COMMON/ONE/NDIM,IHLF,RCRT,EPSC,MGORLI,NSPPG,ICASE,NCEC71,T(200)
COMMON/THR/OXFULE(20),PG,TOG(20),RGAS(20),UNIVR,WIFU(20),
1 AIFU(20),RHOIFU(20),RIFU(20),TIOX(20),WIOX(20),AIOX(20),
2 RHOIOX(20),RIOX(20),TIOX(20),AIPCTF(20),ZCH,PI(20),DIACH,
3 TG(20),AG(20),WG(20),RHOG(20),RAD(20),MDTI(20),PRO(20),PRF(20),
4 PCTMO(20),MDTIFU(20),MDTIOX(20),MWG(20),AC,NAORW,MTOTMX
5 ,CDINJ(20)
IF(NOAI.GT.1) GOTO 1
PIAVG=1.010*PG
1 DO 2 I=1,NINCH
  IF(MGORLI.EQ.2) MDTIFU(I)=CDINJ(I)*AIFU(I)*SQRT(2.*RHOIFU(I)
  1 *(PRF(I)-PIAVG))
  IF(MGORLI.EQ.2) GOTO 2
  MDTIFU(I)=CDINJ(I)*AIFU(I)*SQRT((2.*PIAVG*PRF(I)-2.*PIAVG**2)
  1 /RIFU(I)/TIFU(I))
2 CONTINUE
DO 3 I=1,NINCH
  MDTI(I)=MDTIFU(I)*(1.+OXFULE(I))
  MDTIOX(I)=MDTI(I)-MDTIFU(I)
  IF(OXFULE(I).EQ.0.) AIOX(I)=0.
  IF(OXFULE(I).EQ.0.) GOTO 3
  IF(MGORLI.EQ.2) AIOX(I)=MDTIOX(I)/CDINJ(I)/SQRT(RHOIOX(I)*2.*
  1 (PRO(I)-PIAVG))
  IF(MGORLI.EQ.1) AIOX(I)=MDTIOX(I)/CDINJ(I)/SQRT(PIAVG/TIOX(I)/
  1 RIOX(I)*2.*(PRO(I)-PIAVG))
3 CONTINUE
RETURN
END

```

```

PRSP 10
PRSP 20
PRSP 30
PRSP 40
PRSP 50
PRSP 60
PRSP 70
PRSP 80
PRSP 90
PRSP 100
PRSP 110
PRSP 120
PRSP 130
PRSP 131
PRSP 140
PRSP 150
PRSP 160
PRSP 170
PRSP 180
PRSP 190
PRSP 200
PRSP 210
PRSP 220
PRSP 230
PRSP 240
PRSP 250
PRSP 260
PRSP 270
PRSP 280
PRSP 290
PRSP 300
PRSP 310
PRSP 320
PRSP 330
PRSP 340

```

CC  
CC  
CC  
CC



```

TIFU(1)=TG(1)
WIFU(1)=WG(1)
RIFU(1)=RGAS(1)
RHOIFU(1)=RHOG(1)
AIFU(1)=MTIFU(1)/RHOIFU(1)/WIFU(1)
IF( OXFULE(1).EQ.0.) RETURN
TIOX(1)=TG(1)
WIOX(1)=WG(1)
RIOX(1)=RGAS(1)
RHOIOX(1)=RHOG(1)
AIOX(1)=MTIOX(1)/RHOIOX(1)/WIOX(1)
RETURN
END

```

```

SPPG 500
SPPG 510
SPPG 520
SPPG 530
SPPG 540
SPPG 550
SPPG 560
SPPG 570
SPPG 580
SPPG 590
SPPG 600
SPPG 610
SPPG 620

```

```

SUBROUTINE EQU LIB(NINCH)
REAL MO, MOCH, MDTI, MDTIFU, MDTIOX, MWG
COMMON
1 PRMT(6), DERY(4), AUX(16,4), Y(4), RM(10)
2 POCL(7), ERWT(4), RMIN(7), MODECH, RMINSQ(7), URMNSQ(7)
COMMON/ONE/NDIM, IHLF, RCRT, EPSC, MGORLI, NSPPG, ICASE, NCEC71, T(200)
COMMON/TWO/YSAVE(200,4), XSAVE(200), J, CPG(20), POG(20), YPSAV(200,4), MO
1 RT, RCWALL, GAMG(20), NCHAL, NCHAZ, PSI0(10), PSI02(10), TWOP, PSI12, MO
COMMON/THR/OXFULE(20), PG, TOG(20), RGAS(20), UNIVR, WIFU(20),
1 AIFU(20), RHOIFU(20), RIFU(20), TIFU(20), WIOX(20), AIOX(20),
2 RHOIOX(20), RIOX(20), TIOX(20), AIPCTF(20), ZCH, PI(20), DIACH,
3 TG(20), AG(20), WG(20), RHOG(20), RAD(20), MDTI(20), PRO(20), PRF(20),
4 PCTMO(20), MDTIFU(20), MDTIOX(20), MWG(20), AC, NAORW, MTOTMX
5 CDINJ(20)
COMMON/ZONE/KZONE, PGPSIA, OXFUL(20), LETOUT
DIMENSION SAVTOG(20), SAVGAM(20), SAVMWG(20)
NAMELIST /EQU/ TOG, GAMG, MWG, NCHANG
DO 3 I=1,20
3 OXFUL(I)=OXFULE(I)
NCHANG=0
IF(MODECH.NE.3.AND.NCEC71.GT.1.AND.LOOP.GT.1) RETURN
IF(MODECH.NE.3.AND.NCEC71.GT.1.AND.LETOUT.EQ.71) RETURN
IF(MODECH.NE.3.AND.NCEC71.EQ.1.AND.MTOTMX.EQ.1.AND.LETOUT.EQ.71)
1 GOTO 4
1 IF(MODECH.NE.3.AND.NCEC71.EQ.1.AND.LOOP.GT.1.AND.MTOTMX.EQ.1)
1 GOTO 4
IF(MODECH.NE.3.AND.NCEC71.NE.0.AND.LOOP.GT.1) RETURN
IF(MODECH.NE.3.AND.NCEC71.NE.0) CALL DRIVE(NINCH,PG)
IF(MODECH.NE.3.AND.NCEC71.EQ.1.AND.LOOP.EQ.1.AND.MTOTMX.EQ.1)
1 GOTO 7
1 IF(MODECH.NE.3.AND.NCEC71.NE.0) GOTO 2
IF(LOOP.GT.1.AND.MTOTMX.GT.0) GOTO 4
6 CONTINUE
IF(LOOP.GT.1) RETURN
IF(MODECH.EQ.3.AND.NCEC71.NE.0) CALL DRIVE(NINCH,PG)
IF(MODECH.EQ.3.AND.NCEC71.EQ.1.AND.LOOP.EQ.1.AND.MTOTMX.EQ.1.AND.
1 LETOUT.EQ.71) GOTO 4
1 IF(MODECH.EQ.3.AND.NCEC71.EQ.1.AND.LOOP.EQ.1.AND.MTOTMX.EQ.1)
1 GOTO 7
1 IF(MODECH.EQ.3.AND.NCEC71.NE.0) GOTO 2
C
IF(LOOP.GT.1.AND.MTOTMX.GT.0) GOTO 4
6 CONTINUE
IF(LOOP.GT.1) RETURN
IF(MODECH.EQ.3.AND.NCEC71.NE.0) CALL DRIVE(NINCH,PG)
IF(MODECH.EQ.3.AND.NCEC71.EQ.1.AND.LOOP.EQ.1.AND.MTOTMX.EQ.1.AND.
1 LETOUT.EQ.71) GOTO 4
1 IF(MODECH.EQ.3.AND.NCEC71.EQ.1.AND.LOOP.EQ.1.AND.MTOTMX.EQ.1)
1 GOTO 7
1 IF(MODECH.EQ.3.AND.NCEC71.NE.0) GOTO 2
C
READ(5,EQU)
IF(LOOP.EQ.1.AND.NCHANG.GT.0) GOTO 7
IF(LOOP.EQ.1.AND.NCHANG.EQ.0) GOTO 4
9 CONTINUE
IF(NCHANG.EQ.0) RETURN
2 CONTINUE
IF(NCEC71.NE.0) RETURN
DO 1 I=1,NINCH

```

```

EQU 500
EQU 510
EQU 520
EQU 530
EQU 540
EQU 550
EQU 560
EQU 570
EQU 580
EQU 590
EQU 600
EQU 610
EQU 620
EQU 630
EQU 640
EQU 650
EQU 660

```

```

1  RGAS(I)=UNIVR*32.174/MWG(I)
2  CPG(I)=GAMG(I)*RGAS(I)/(GAMG(I)-1.)
3  RETURN
4  DO 5 I=1,NINCH
5   TOG(I)=SAVTOG(I)
6   GAMG(I)=SAVGAM(I)
7   MWG(I)=SAVMWG(I)
8   RGAS(I)=UNIVR*32.174/MWG(I)
9   CPG(I)=GAMG(I)*RGAS(I)/(GAMG(I)-1.)
10  IF(LOOP.EQ.1.AND.NCHANG.EQ.0) GOTO 9
11  GOTO 6
12  DO 8 I=1,NINCH
13   SAVTOG(I)=TOG(I)
14   SAVGAM(I)=GAMG(I)
15   SAVMWG(I)=MWG(I)
16  GOTO 9
17  END

```

```

SUBROUTINE LOAD1(NPT)
SEVERAL CONVERSION FACTORS ARE IN THIS SUBROUTINE TO CONVERT
DATA GENERATED BY MODIFIED PROGRAM CEC71 TO THE ENGLISH TECHNICAL
UNITS REQUIRED BY CHAMBER AND THROAT CALCULATIONS.
MODIFICATION OF THIS SUBROUTINE WOULD BE ESSENTIAL IN
A CONVERSION TO A DIFFERENT UNIT SYSTEM.
REAL MWG,MO,MDTI,MDTIFU,MDTIOX
DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS
LOGICAL EQL,FROZ,AREA
COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
1 ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)
2 ,VLM(13),TOTN(13)
COMMON/PERF/PCP(22),VMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13)
1 ,APP(13),AEAT(13),CSTR,EQL,FROZ,SSO,AREA,AWT
COMMON/ACSTAR/CSTAR(13)
COMMON/ZONE/KZONE,PGPSIA,OXFUL(20),LETOUT
COMMON/LOAD/CST(20),VAC1DI(20)
COMMON/LOTAB/APRES(13),ASON(20,13),AMAC(20,13),AVEL(20,13),
1 ARHO(20,13),GAMR(20,13),TEMPE(20,13),WMR(20,13),VACSPI(20,13)
COMMON/TWO/YSAVE(200,4),XSAVE(200,4),CPG(20),POG(20),YPSAV(200,4),
1 RT,RCWALL,GAMG(20),NCHAL,NCHAZ,PSI01(10),PSI02(10),TWOP1,PSI12,MO
COMMON/THR/OXFULE(20),PG,TOG(20),RGAS(20),UNIVR,WIFU(20),
1 AIFU(20),RHOIFU(20),RIFU(20),WIOX(20),AIOX(20),
2 RHOIOX(20),RIOX(20),TIOX(20),AIPCTF(20),ZCH,PI(20),DIACH,
3 TG(20),AG(20),WG(20),RAD(20),MDTI(20),PRO(20),PRF(20),
4 PCTMO(20),MDTIFU(20),MDTIOX(20),MWG(20),AC,NAORW,MTOTMX
5 ,CDINJ(20)
DO 1 I=1,NPT
APRES(I)=PG/APP(I)
ASON(KZONE,I)=SONVEL(I)*3.281
AMAC(KZONE,I)=VMOC(I)
AVEL(KZONE,I)=ASON(KZONE,I)*VMOC(I)
ARHO(KZONE,I)=1./VLM(I)*1.94179
GAMR(KZONE,I)=GAMMAS(I)
TEMPE(KZONE,I)=(TTT(I)+.5)*1.8
1 WMR(KZONE,I)=WM(I)
TOG(KZONE,I)=(TTT(I)+.5)*1.8
RGAS(KZONE)=UNIVR*32.174/WM(1)
GAMG(KZONE)=GAMMAS(1)
CPG(KZONE)=GAMG(KZONE)*RGAS(KZONE)/(GAMG(KZONE)-1.)
MWG(KZONE)=WM(1)
RHOG(KZONE)=ARHO(KZONE,1)
RETURN
ENTRY LOAD2(NPT)
DO 2 I=2,NPT
2 VACSPI(KZONE,I)=VACI(I)
VAC1DI(KZONE)=VACI(2)
CST(KZONE)=CSTAR(2)
RETURN
END

```

LOAD 10  
LOAD 20  
LOAD 30  
LOAD 40  
LOAD 50  
LOAD 60  
LOAD 70  
LOAD 80  
LOAD 90  
LOAD 100  
LOAD 110  
LOAD 120  
LOAD 130  
LOAD 140  
LOAD 150  
LOAD 160  
LOAD 170  
LOAD 180  
LOAD 190  
LOAD 200  
LOAD 210  
LOAD 220  
LOAD 230  
LOAD 240  
LOAD 250  
LOAD 260  
LOAD 261  
LOAD 270  
LOAD 280  
LOAD 290  
LOAD 300  
LOAD 310  
LOAD 320  
LOAD 330  
LOAD 340  
LOAD 350  
LOAD 360  
LOAD 370  
LOAD 380  
LOAD 390  
LOAD 400  
LOAD 410  
LOAD 420  
LOAD 430  
LOAD 440  
LOAD 450  
LOAD 460  
LOAD 470  
LOAD 480  
LOAD 490

C  
C  
C  
C  
C

```

SUBROUTINE HPCG(PRMT,Y,DERY,NDIM,IHLF,FCT,OUTP,AUX)
DIMENSION PRMT(6),Y(NDIM),DERY(NDIM),AUX(16,NDIM)
N=1
IHLF=0
X=PRMT(1)
H=PRMT(3)
PRMT(5)=0,NDIM
DO 1 I=1,NDIM
  AUX(16,I)=0,DERY(I)
  AUX(15,I)=Y(I)
  AUX(1,I)=PRMT(2)-X)3,2,4
1 IF(H*(PRMT(2)-X)3,2,4
2 IHLF=12
3 GOTO 4
4 IHLF=13
5 CALL FCT(X,Y,DERY)
6 CALL OUTP(X,Y,DERY,IHLF,NDIM,PRMT)
7 IF(PRMT(5)16,5,6
8 IF(IHLF)7,7,6
9 RETURN
10 DO 8 I=1,NDIM
11 AUX(8,I)=DERY(I)
12 ISW=1
13 GOTO 100
14 X=X+H
15 DO 10 I=1,NDIM
16 AUX(2,I)=Y(I)
17 IHLF=IHLF+1
18 X=X-H
19 DO 12 I=1,NDIM
20 AUX(4,I)=AUX(2,I)
21 H=.5#H
22 N=1
23 ISW=2
24 GOTO 100
25 X=X+H
26 CALL FCT(X,Y,DERY)
27 IF(Y(1).LE.0.) RETURN
28 N=2
29 DO 14 I=1,NDIM
30 AUX(2,I)=Y(I)
31 AUX(9,I)=DERY(I)
32 ISW=3
33 GOTO 100
34 DELT=0
35 DO 16 I=1,NDIM
36 DELT=DELT+AUX(15,I)*ABS(Y(I)-AUX(4,I))
37 DELT=.06666667#DELT
38 IF(DELT-PRMT(4))19,19,17
39 IF(IHLF-10)11,18,18

```

```

HPCG11080
HPCG11110
HPCG11120
HPCG11130
HPCG11140
HPCG11150
HPCG11160
HPCG11170
HPCG11180
HPCG11190
HPCG11200
HPCG11210
HPCG11240
HPCG11250
HPCG11260
HPCG11290
HPCG11320
HPCG11330
HPCG11340
HPCG11350
HPCG11360
HPCG11370
HPCG11400
HPCG11410
HPCG11430
HPCG11440
HPCG11450
HPCG11480
HPCG11490
HPCG11500
HPCG11510
HPCG11520
HPCG11530
HPCG11540
HPCG11550
HPCG11570
HPCG11580
HPCG1158A
HPCG11590
HPCG11600
HPCG11610
HPCG11620
HPCG11630
HPCG11640
HPCG11670
HPCG11680
HPCG11690
HPCG11700
HPCG11710
HPCG11720

```



```

18 IHLF=11
   X=X+H
   GOTO 4
19 X=X+H
   CALL FCT(X,Y,DERY)
   IF(Y(1).LE.0.) RETURN
   DO 20 I=1,NDIM
     AUX(3,I)=Y(I)
20   AUX(10,I)=DERY(I)
   N=3
   ISW=4
   GOTO 100
21 N=1
   X=X+H
   CALL FCT(X,Y,DERY)
   IF(Y(1).LE.0.) RETURN
   X=PRMT(1)
   DO 22 I=1,NDIM
     AUX(11,I)=DERY(I)
22   Y(1)=AUX(1,I)+H*(.375*AUX(8,I)+.7916667*AUX(9,I)
1- .2083333*AUX(10,I)+.0416667*DERY(I))
23 X=X+H
   N=N+1
   CALL FCT(X,Y,DERY)
   CALL OUTP(X,Y,DERY,IHLF,NDIM,PRMT)
   IF(PRMT(5))6,24,6
24   IF(N-4)25,200,200
25   DO 26 I=1,NDIM
     AUX(N,I)=Y(I)
26   AUX(N+7,I)=DERY(I)
27   IF(N-3)27,29,200
     DELT=AUX(9,I)+AUX(9,I)
     DELT=DELT+DELT
28   Y(1)=AUX(1,I)+.3333333*H*(AUX(8,I)+DELT+AUX(10,I))
   GOTO 23
29   DO 30 I=1,NDIM
     DELT=AUX(9,I)+AUX(10,I)
     DELT=DELT+DELT+DELT
30   Y(1)=AUX(1,I)+.375*H*(AUX(8,I)+DELT+AUX(11,I))
   GOTO 23
100 DO 101 I=1,NDIM
     Z=H*AUX(N+7,I)
     AUX(5,I)=Z
101   Y(1)=AUX(N,I)+.4*Z
     Z=X+.4*H
     CALL FCT(Z,Y,DERY)
     IF(Y(1).LE.0.) RETURN
     DO 102 I=1,NDIM
       Z=H*DERY(I)

```

HPCG1750  
 HPCG1760  
 HPCG1770  
 HPCG1800  
 HPCG1810  
 HPCG181A  
 HPCG1820  
 HPCG1830  
 HPCG1840  
 HPCG1850  
 HPCG1860  
 HPCG1870  
 HPCG1890  
 HPCG1900  
 HPCG1910  
 HPCG191A  
 HPCG1920  
 HPCG1930  
 HPCG1940  
 HPCG1950  
 HPCG1960  
 HPCG1970  
 HPCG1980  
 HPCG1990  
 HPCG2000  
 HPCG2010  
 HPCG2020  
 HPCG2030  
 HPCG2040  
 HPCG2050  
 HPCG2060  
 HPCG2080  
 HPCG2090  
 HPCG2100  
 HPCG2110  
 HPCG2120  
 HPCG2140  
 HPCG2150  
 HPCG2160  
 HPCG2170  
 HPCG2180  
 HPCG2230  
 HPCG2240  
 HPCG2250  
 HPCG2260  
 HPCG2290  
 HPCG2300  
 HPCG230A  
 HPCG2310  
 HPCG2320

HPCG22330  
 HPCG22340  
 HPCG22360  
 HPCG22370  
 HPCG2237A  
 HPCG22380  
 HPCG22390  
 HPCG22400  
 HPCG22410  
 HPCG22430  
 HPCG22440  
 HPCG2244A  
 HPCG22450  
 HPCG22460  
 HPCG22470  
 HPCG22480  
 HPCG22540  
 HPCG22550  
 HPCG22580  
 HPCG22590  
 HPCG22600  
 HPCG22610  
 HPCG22620  
 HPCG22650  
 HPCG22680  
 HPCG22690  
 HPCG22700  
 HPCG22710  
 HPCG22720  
 HPCG22730  
 HPCG22740  
 HPCG22750  
 HPCG22760  
 HPCG22770  
 HPCG22810  
 HPCG2281A  
 HPCG22840  
 HPCG22850  
 HPCG22860  
 HPCG22870  
 HPCG22880  
 HPCG22910  
 HPCG22920  
 HPCG22930  
 HPCG22940  
 HPCG22970  
 HPCG22980  
 HPCG22990  
 HPCG23000  
 HPCG23010

```

102 AUX(6,I)=Z
    Y(I)=AUX(N,I)+.2969776*AUX(5,I)+.1587596*Z
    Z=X+.4557372*H
    CALL FCT(Z,Y,DERY)
    IF(Y(1).LE.O.) RETURN
    DO 103 I=1,NDIM
      Z=H*DERY(I)
    AUX(7,I)=Z
103 Z=X+H
    Y(I)=AUX(N,I)+.2181004*AUX(5,I)-3.050965*AUX(6,I)+3.832865*Z
    CALL FCT(Z,Y,DERY)
    IF(Y(1).LE.O.) RETURN
    DO 104 I=1,NDIM
      Z=X+H
104 OY(I)=AUX(N,I)+.1747603*AUX(5,I)-.5514807*AUX(6,I)
      I+.1.205536*AUX(7,I)+.1711848*H*DERY(I)
      GOTO(9,13,15,21),ISW
200 ISTEP=3
201 IF(N-8)204,202,204
202 DO 203 N=2,7
    DO 203 I=1,NDIM
      AUX(N-1,I)=AUX(N,I)
203 AUX(N+6,I)=AUX(N+7,I)
    N=7
204 N=N+1
    DO 205 I=1,NDIM
      AUX(N-1,I)=Y(I)
205 AUX(N+6,I)=DERY(I)
    X=X+H
206 ISTEP=ISTEP+1
    DO 207 I=1,NDIM
      ODEL T=AUX(N-4,I)+1.333333*H*(AUX(N+6,I)+AUX(N+5,I)+
      1AUX(N+4,I)+AUX(N+4,I))
      Y(I)=DEL T-.9256198*AUX(16,I)
207 AUX(16,I)=DEL T
      CALL FCT(X,Y,DERY)
      IF(Y(1).LE.O.) RETURN
    DO 208 I=1,NDIM
      ODEL T=.125*{9.*AUX(N-1,I)-AUX(N-3,I)+3.*H*(DERY(I)+AUX(N+6,I)+
      1AUX(N+6,I)-AUX(N+5,I))}
      AUX(16,I)=AUX(16,I)-DEL T
208 Y(I)=DEL T+.07438017*AUX(16,I)
      DEL T=O.
    DO 209 I=1,NDIM
      DEL T=DEL T+AUX(15,I)*ABS(AUX(16,I))
209 IF(DEL T-PRMT(4))210,222,222
210 CALL FCT(X,Y,DERY)
      CALL OUTP(X,Y,DERY,IHLF,NDIM,PRMT)
211 IF(PRMT(5))212,211,212
212 IF(IHLF-1)213,212,212
      RETURN
  
```

```

213 IF(H*(X-PRMT(2))214,212,212
214 IF(ABS(X-PRMT(2))-1*ABS(H)212,215,215
215 IF(DELTA-.02*PRMT(4))216,216,201
216 IF(IHLF)201,201,217
217 IF(N-7)201,218,218
218 IF(ISTEP-4)201,219,219
219 IMOD=ISTEP/2
220 IF(ISTEP-IMOD-IMOD)201,220,201
220 H=H+H
220 IHLF=IHLF-1
220 ISTEP=0
220 DO 221 I=1,NDIM
220 AUX(N-1,I)=AUX(N-2,I)
220 AUX(N-2,I)=AUX(N-4,I)
220 AUX(N-3,I)=AUX(N-6,I)
220 AUX(N+6,I)=AUX(N+5,I)
220 AUX(N+5,I)=AUX(N+3,I)
220 AUX(N+4,I)=AUX(N+1,I)
220 DELT=AUX(N+6,I)+AUX(N+5,I)
220 DELT=DELT+DELT
2210AUX(16,I)=8.962963*(Y(I)-AUX(N-3,I))-3.361111*H*(DERY(I)+DELT
2211+AUX(N+4,I))
221 GOTO 201
222 IHLF=IHLF+1
223 IF(IHLF-10)223,223,210
223 H=.5*H
223 ISTEP=0
224 DO 224 I=1,NDIM
224 OY(I)=.00390625*(80.*AUX(N-1,I)+135.*AUX(N-2,I)+40.*AUX(N-3,I)+
2241AUX(N-4,I))-1171875*(AUX(N+6,I)-6.*AUX(N+5,I)-AUX(N+4,I))*H
22410AUX(N-4,I)=.00390625*(12.*AUX(N-1,I)+135.*AUX(N-2,I)+
2241108.*AUX(N-3,I)+AUX(N-4,I))-0.0234375*(AUX(N+6,I)+18.*AUX(N+5,I)-
224129.*AUX(N+4,I))*H
22413AUX(N-3,I)=AUX(N-2,I)
22414AUX(N-4,I)=AUX(N+5,I)
224 X=X-H
224 DELT=X-(H+H)
224 CALL FCT(DELTA,Y,DERY)
224 IF(Y(1).LE.0.)RETURN
224 DO 225 I=1,NDIM
224 AUX(N-2,I)=Y(I)
224 AUX(N+5,I)=DERY(I)
224 Y(I)=AUX(N-4,I)
224 DELT=DELTA-(H+H)
224 CALL FCT(DELTA,Y,DERY)
224 IF(Y(1).LE.0.)RETURN
224 DO 226 I=1,NDIM
224 DELT=AUX(N+5,I)+AUX(N+4,I)
224 DELT=DELT+DELT
2240AUX(16,I)=8.962963*(AUX(N-1,I)-Y(I))-3.361111*H*(AUX(N+6,I)+DELT

```

HPCG3020  
HPCG3030  
HPCG3040  
HPCG3090  
HPCG3100  
HPCG3110  
HPCG3120  
HPCG3130  
HPCG3140  
HPCG3150  
HPCG3160  
HPCG3170  
HPCG3180  
HPCG3190  
HPCG3200  
HPCG3210  
HPCG3220  
HPCG3230  
HPCG3240  
HPCG3250  
HPCG3260  
HPCG3270  
HPCG3280  
HPCG3320  
HPCG3330  
HPCG3340  
HPCG3350  
HPCG3360  
HPCG3370  
HPCG3380  
HPCG3390  
HPCG3400  
HPCG3410  
HPCG3420  
HPCG3430  
HPCG3440  
HPCG3450  
HPCG3460  
HPCG346A  
HPCG3470  
HPCG3480  
HPCG3490  
HPCG3500  
HPCG3510  
HPCG3520  
HPCG352A  
HPCG3530  
HPCG3540  
HPCG3550  
HPCG3560

```
1+DERY(I))  
226 AUX(N+3,I)=DERY(I)  
GO TO 206  
END
```

```
HPCG3570  
HPCG3580  
HPCG3590  
HPCG3600
```

```

SUBROUTINE FCT(R,Y,DERY)
REAL MO,MOCH,MDTI,MDTIFU,MDTIOX,NEXPSI,MWG
COMMON/ONE/NDIM,IHLF,RCRT,EPSC,MGORLI,NSPPG
COMMON/TWO/YSAVE(200,4),XSAVE(200,4),POG(20),YPSAV(200,4),
1 RT,RCWALL,GAMG(20),NCHAL,NCHAP,PSI01(10),PSI02(10),TWDPI,PSI12,MO
COMMON/THR/OXFULE(20),PG,TOG(20),RGAS(20),UNIVR,WIFU(20),
1 AIFU(20),RHOIFU(20),RIFU(20),TIFU(20),WIOX(20),AIOX(20),
2 RHOIOX(20),RIOX(20),TIOX(20),AIPCTF(20),ZCH,PI(20),DIACH,
3 TG(20),AG(20),WG(20),RHOG(20),RAD(20),MDTI(20),PRO(20),PRF(20),
4 PCTMO(20),MDTI(20),MDTIOX(20),MWG(20),AC,NAORW,MTOTMX
5 CDINJ(20)
COMMON/CALC/HO,C,GAM,GAMSAV(200),K
DIMENSION Y(NDIM),DERY(NDIM)
NCHALP=NCHAL+1
NCHAP=NCHAP+1
NCHAP=NCHAP+1
IF(MTOTMX.GT.0)NCHAP=2
IF(J.GE.2)GOTO 3
IF(J.GE.1)GOTO 2
DO I=1,NDIM
1 DERY(I)=0.
K=1
GAM=GAMG(K)
IF(NCEC71.LT.2) GOTO 12
YI=Y(I)
IF(NCEC71.GT.1) CALL TAB(Y1,DENS,VELO,TEMP,EMACH)
T(1)=TEMP
YPSAV(1,4)=EMACH
YSAVE(1,3)=VELO
12 CONTINUE
RETURN
2 K=1
3 GOTO 7
JMI=J-1
NEXPSI=YSAVE(J,2)+(R-XSAVE(J))*(YSAVE(J,2)-YSAVE(JMI,2))/
1 (XSAVE(J)-XSAVE(JMI))
K=1
DO 4 I=2,NCHAP
IF(NEXPSI.LE.PSI01(I))GOTO 7
K=K+1
4 CONTINUE
K=K-1
IF(NCHAP.EQ.0)GOTO 7
IF(PSI12.GE.1.)GOTO 7
K=K+1
DO 6 I=2,NCHAP2P
IF(NEXPSI.LE.PSI02(I))GOTO 7
K=K+1
6 CONTINUE
K=K-1
7 CONTINUE
IF(NCEC71.LT.2) GOTO 14

```

10 FCT  
 20 FCT  
 30 FCT  
 40 FCT  
 50 FCT  
 60 FCT  
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 100 FCT  
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 130 FCT  
 140 FCT  
 150 FCT  
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 200 FCT  
 210 FCT  
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FCT  
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 FCT  
 FCT

```

Y1=Y(1)
IF(NCEC71.GT.1) CALL TAB(Y1,DENS,VELO,TEMP,EMACH)
JPI=J+1
T(JPI)=TEMP
YPSAV(JPI,4)=EMACH
YSAVE(JPI,3)=VELO
IF(NCEC71.GT.1) GOTO 8
14 HO=CPG(K)*TOG(K)
C=POG(K)/(POG(K)/RGAS(K)/TOG(K))**GAMG(K)
GAM=GAMG(K)
G2=1./GAM
G3=(GAM-1.)/GAM
8 G1=RCWALL*((RT*(1.+RCWALL/R)-R)/RCWALL)**1.5
IF(Y(1).LE.0.) WRITE(6,9) R,YSAVE(1,1)
9 FORMAT(26H PRESSURE IS LE ZERO AT R=,E15.6,10X,4HPCL=,E15.6)
IF(Y(1).LE.0.) DERY(1)=0.
IF(Y(1).LE.0.) DERY(2)=0.
IF(Y(1).LE.0.) RETURN
IF(NCEC71.LT.2) GOTO 10
DERY(1)=-DENS*VELO*VELO/G1
DERY(2)=TWOPI*R*DENS*VELO/M0
GOTO 11
10 DERY(1)=-Y(1)/C**G2*(2.*(HO-Y(1))*G3*C**G2/G3))/G1
DERY(2)=(Y(1)/C)**G2*TWOPI*R*SQRT(2.*(HO-Y(1))*G3*C**G2/G3))/M0
11 CONTINUE
END
  
```

```

SUBROUTINE OUTP(X,Y,DERY,IHL,NDI,PRMT)
  YSAVE(J,1) IS PRESSURE.
  YSAVE(J,2) IS PSI.
  YSAVE(J,3) IS VELOCITY.
  YPSAV(J,4) IS THE LOCAL MACH NUMBER.
  REAL MDTI,MDTIFU,MDTIOX,MO,MWG
  DIMENSION PRMT(6),Y(NDI),DERY(NDI)
  COMMON/ONE/NDIM,IHL,RCRT,DEPSC,MGORLI,NSPPG,ICASE,NCEC71,T(200)
  COMMON/TWO/YSAVE(200,4),XSAVE(200),J,CPG(20),POG(20),YPSAV(200,4),
1 RT,RCWALL,GAMG(20),NCHAI,NCHAZ2,PSIO1(10),PSIO2(10),TMDPI,PSI12,MO
  COMMON/THR/OXFULE(20),PG,TOG(20),RGAS(20),UNIVR,WIFU(20),
1 AIFU(20),RHOIFU(20),RIFU(20),TIFU(20),WIOX(20),AIOX(20),
2 RHOIOX(20),RIOX(20),TIOX(20),AIPCTF(20),ZCH,PI(20),DIACH,
3 TG(20),AG(20),WG(20),RHOG(20),RAD(20),MDTI(20),PRF(20),
4 PCTMO(20),MDTIFU(20),MDTIOX(20),MWG(20),AC,NAORW,MTOTMX
5 CDINJ(20)
  COMMON/CALC/HO,C,GAM,GAMSAV(200),K
  IHLF=IHL
  NDIM=NDI
  IF(Y(1).LE.0.) PRMT(5)=1.
  IF(Y(1).LE.0.) RETURN
  J=J+1
1 XSAVE(J)=X
  DO 2 I=1,NDIM
    YSAVE(J,I)=Y(I)
2 YPSAV(J,1)=DERY(I)
    T(J)=TOG(K)/YPSAV(J,3)
    YPSAV(J,3)=1./((YSAVE(J,1)/POG(K))* (1.-1./GAM)
    A=SQRT(TOG(K)*GAM*RGAS(K)/YPSAV(J,3))
    YPSAV(J,4)=SQRT(2.*((YPSAV(J,3)-1.)/(GAM-1.))
4 YSAVE(J,3)=A*YPSAV(J,4)
    IF(YSAVE(J,2).GE.PRMT(6)) PRMT(5)=1.0
  GAMSAV(J)=GAM
  RETURN
END

```

```

10 OUTP
20 OUTP
30 OUTP
40 OUTP
50 OUTP
60 OUTP
70 OUTP
80 OUTP
90 OUTP
100 OUTP
110 OUTP
120 OUTP
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140 OUTP
150 OUTP
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200 OUTP
210 OUTP
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250 OUTP
260 OUTP
270 OUTP
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300 OUTP
310 OUTP
320 OUTP
330 OUTP
340 OUTP
350 OUTP

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CCC

TAB 10  
TAB 20  
TAB 30  
TAB 40  
TAB 50  
TAB 60  
TAB 70  
TAB 80  
TAB 90  
TAB 100  
TAB 110  
TAB 120  
TAB 130  
TAB 140  
TAB 150  
TAB 160  
TAB 170  
TAB 180  
TAB 190  
TAB 200  
TAB 210  
TAB 220  
TAB 230  
TAB 240  
TAB 250

```

SUBROUTINE TAB(Y1,DENS,VELO,TEMP,EMACH)
COMMON/LOTAB/APRES(13),ASON(20,13),AMAC(20,13),AVEL(20,13),
1 ARHO(20,13),GAMR(20,13),TEMPE(20,13),WMR(20,13),VACSPI(20,13)
COMMON/CALC/HO,C,GAM,GAMSAV(200),K
IF(Y1.GE.APRES(3)) GOTO 1
IF(Y1.LE.APRES(12)) GOTO 2
DO 4 I=4,12
M1=I
M2=I-1
IF(Y1.GE.APRES(I)) GOTO 3
CONTINUE
SLO=(Y1-APRES(M1))/(APRES(M2)-APRES(M1))
DENS=ARHO(K,M1)+SLO*(ARHO(K,M2)-ARHO(K,M1))
VELO=AVEL(K,M1)+SLO*(AVEL(K,M2)-AVEL(K,M1))
TEMP=TEMPE(K,M1)+SLO*(TEMPE(K,M2)-TEMPE(K,M1))
EMACH=AMAC(K,M1)+SLO*(AMAC(K,M2)-AMAC(K,M1))
GAM=GAMR(K,M1)+SLO*(GAMR(K,M2)-GAMR(K,M1))
RETURN
1 M1=3
M2=4
GOTO 3
2 M1=12
M2=11
GOTO 3
END

```



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```

SUBROUTINE AITKEN(X,Y,N,K,XB,YB)
DIMENSION X(N),Y(N),XX(11),YY(11)
K1=K+1
IF(X(N)-X(1))10,1,1
IF(XB-X(1))2,2,3
1  LL=0
2  GOTO 19
3  IF(X(N)-XB)4,4,5
4  LL=N-K1
5  GOTO 19
6  LL=1
7  LU=N
8  LPL=LL+1
9  IF(LU-LPL)17,17,7
10 LI=(LL+LU)/2
11 IF(X(LI)-XB)8,8,9
12 LL=LI
13 GOTO 6
14 LU=LI
15 GOTO 6
16 LL=LI
17 GOTO 13
18 LL=LL-(K1+1)/2
19 IF(LL)2,19,18
20 IF(LL+K1-N)19,19,4
21 DO 20 I=1,K1
    II=LL+I
    XX(II)=X(II)-XB
    YY(II)=Y(II)
    DO 21 I=1,K
      JJ=II+K
      YY(JJ)=(1./(XX(JJ)-XX(II)))*(YY(II)*XX(JJ+1)-YY(J+1))*XX(II)
    YB=YY(K1)
  RETURN
END
  
```

```

SUBROUTINE UORD(RW,CLP,NCLP,MORDER)
DIMENSION RW(NCLP),CLP(NCLP)
DO 12 KP=1,NCLP
  RCHK=RW(KP)
  PCHK=CLP(KP)
  DO 11 LP=KP,NCLP
    IF(MORDER)8,9,8
    8 IF(RW(LP)-RCHK)10,11,11
    9 IF(CL(LP)-PCHK)10,11,11
    10 STOP=RCHK
    RCHK=RW(LP)
    PCHK=CL(LP)
    RW(LP)=STOP
    CL(LP)=STOP
    11 CONTINUE
    CL(KP)=PCHK
    12 RW(KP)=RCHK
  RETURN
END

```

```

UPOR 10
UPOR 20
UPOR 30
UPOR 40
UPOR 50
UPOR 60
UPOR 70
UPOR 80
UPOR 90
UPOR 100
UPOR 110
UPOR 120
UPOR 130
UPOR 140
UPOR 150
UPOR 160
UPOR 170
UPOR 180
UPOR 190
UPOR 200

```

```

SUBROUTINE PLYCF (X,Y,NEP,A,NORD,NSTOPD)
DOUBLE PRECISION XC,P,V,DP,B(10,11),BS(10,10),A(11)
DIMENSION X(NEP),Y(NEP)
JA=6
INORM=1
NSTOPD=1
NGORD=0
IF(NORD-NGORD)2,2,1
1 NGORD=NORD
2 NGRD1=NGORD+1
3 N=NORD
N1=N+1
N2=N+2
IF(NEP-GE.N1)GOTO 6
WRITE(JA,5)
5 FORMAT(/43H NOT SUFFICIENT DATA POINTS - CASE OMITTED. )
NSTOPD=2
GOTO 34
6 DO 7 I=1,N2
7 B(I,N2)=0.
8 DO 9 J=1,NGRD1
9 BS(J,I)=0.
DO 13 K=1,NEP
XC=1.
DO 13 J=1,NGRD1
IF(J.EQ.1)GOTO 11
BS(J,NGRD1)=BS(J,NGRD1)+XC
10 XC=XC*X(K)
GOTO 13
11 DO 12 I=1,NGRD1
BS(1,I)=BS(1,I)+XC
12 XC=XC*X(K)
CONTINUE
13 DO 15 J=2,NGRD1
DO 15 I=1,NGORD
BS(J,I)=BS(J-1,I+1)
15 DO 16 I=1,NEP
XC=1.
DO 16 J=1,N1
B(J,N2)=B(J,N2)+XC*Y(I)
XC=XC*X(I)
17 DO 18 I=1,N1
DO 18 J=1,N1
B(I,J)=BS(I,J)
18 DO 27 I=1,N1
IF(B(I,I).NE.0.)GOTO 22
19 NSTOPD=2
20 WRITE(JA,21)
21 FORMAT(/,25H MATRIX SINGULAR NO SOLN.)

```

```

NSTOPD=2
GOTO 34
22 P=1./B(I,I)
23 DO 23 J=1,N2
23 B(I,J)=P*B(I,J)
24 DO 26 K=1,N1
24 NUT=I-K
24 IF(NUT.EQ.0)GOTO 26
24 Q=B(K,I)
25 DO 25 J=1,N2
25 B(K,J)=B(K,J)-Q*B(I,J)
26 CONTINUE
27 CONTINUE
28 DO 29 I=1,N1
29 A(I)=B(I,N2)
30 DEVMAX=0.
30 RMS=0.
30 DO 33 I=1,NEP
30 V=0.
30 DO 31 J=1,N1
30 K1=N1-J+1
31 V=V*X(I)+A(K1)
31 DEV=V-Y(I)
32 IF(ABS(DEV).LT.ABS(DEVMAX))GOTO 33
32 IMAX=I
32 DEVMAX=DEV
33 RMS=RMS+DEV*DEV
33 H=NEP
34 RMS=SQRT(RMS/H)
34 CONTINUE
34 RETURN
END

```

```

PLYC 510
PLYC 520
PLYC 530
PLYC 540
PLYC 550
PLYC 560
PLYC 570
PLYC 580
PLYC 590
PLYC 600
PLYC 610
PLYC 620
PLYC 630
PLYC 640
PLYC 650
PLYC 660
PLYC 670
PLYC 680
PLYC 690
PLYC 700
PLYC 710
PLYC 720
PLYC 730
PLYC 740
PLYC 750
PLYC 760
PLYC 770
PLYC 780
PLYC 790
PLYC 800
PLYC 810
PLYC 820

```

```

SUBROUTINE DRIVE(NINCH,PG)
MAIN PROGRAM
COMMON BLK. MISC IN MAIN,SAVE,&EQLBRM CONTAIN SIZE--OTHERS DO NOT
DOUBLE PRECISION G,X
THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR
IBM 360 MACHINES ONLY
DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS
DOUBLE PRECISION COEF,S,EN,ENLN,H0,DELN
REAL MIX(15)
INTEGER DATA, OMIT, ENSERT, REAC, BLANK, THRM, END, SUB
LOGICAL SHOCK,MMHG,UV,IC,DETN,SIUNIT,EUNITS,NSQM,CALCH
LOGICAL HP,SP,TP,NEWRR,IONS,MOLES,FROZ,EQL,PSIA,RKT,VOL,TV,SV
LOGICAL FA,OF,ERATIO,FPCT,OTTO
DIMENSION OMIT(3,3),NCD(4),ENSERT(3,3),RHO(26),LVP(2),VM(2),VL(26)
1,DATA(22)
COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
1,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)
2,VL(13),TOTN(13)
COMMON/SPECES/COEF(2,7,150),EN(150,13),ENLN(150),HO(150)
1,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2),SLN(150)
COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),BO(15),BOP(15,2)
1,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AC(2),AM(2)
2,HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
3,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4,RHOP,RMW(15),TLN,CR,OXF(15),ENNL,ENSAVE,ENLSAV,TRACE,SIZE
COMMON/DOUBLE/G(20,21),X(20)
COMMON/INDEX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM
1,NS,KMAT,IMAT,IQI,NOF,NOMIT,IP,NEWRR,NSUB,NSUP,ITM,CPCVFR,CPCVEQ
2,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JSI,VOL,SHOCK,IT,NFZ,CALCH
3,IQSAVE,LSAVE,ISUP,ISUB,ITNUM
COMMON/PERF/PCP(22),VMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13)
1,APP(13),AEAT(13),CSTR,EQL,FROZ,SSO,AREA,AWT
COMMON/ZONE/KZONE,PGPSIA,OXFUL(20),LETOUT
EQUIVALENCE (OMIT,ENLN), (ENSERT,DELN), (OXF,MIX)
1,(OF,OXFL),(RHO,P,VL),(SO,SO),(OTTO,CPCVFR),(DATA,DAT)
DATA MIT/4HOMIT/,BLANK/1H/,PSIA/4HPSIA/,REAC/4HREAC/,I2/2HOO/
1,NMLT/4HNAME/,IE/1HE/,INSERT/4HINSE/,THRM/4HITHER/,END/3HEND/
2,GAS/1HG/,LAST/4HLAST/
NAMELIST/INPT2/KASE,T,P,PSIA,MMHG,NSQM,V,RHO,ERATIO,OF,FPCT,FA,
1MIX,TP,HP,SP,TV,UV,SV,RKT,SHOCK,DETN,OTTO,CR,SO,SO,IONS,IDEBUG,
2TRACE,SIUNIT,EUNITS
PGPSIA=PG/144.

```

```

C      IF(LETOUT.EQ.71) RETURN
C      NEWR = .FALSE.
C
C      NPT=0
C      KZONE=0
C      1   KZONE=KZONE+1
C      IF(KZONE.GT.NINCH)RETURN
C      1   WRITE(6,400)
C      400 FORMAT(IH1)
C      RR = 8314.3
C      R = RR/4184.
C      203 READ (5,204) (DATA(I),I=1,15)
C      204 FORMAT(5(3A4,3X))
C      WRITE (6,2045)(DATA(I),I=1,15)
C      2045 FORMAT(1X,5(3A4,3X)) GO TO 90
C      IF(DATA(1).EQ.THRM) GO TO 11
C      IF(DATA(1).EQ.REAC) GO TO 11
C      IF (DATA(1).EQ.MIT) GO TO 205
C      IF (DATA(1).EQ.INSERT) GO TO 180
C      IF(DATA(1).EQ.NMLT) GO TO 210
C      IF(DATA(1).EQ.BLANK) GO TO 203
C      1023 WRITE(6,1024)
C      1024 FORMAT(40HOERROR IN ABOVE CARD. CONTENTS IGNORED.)
C      GO TO 203
C      11 NSERT = 0
C      MOLES = .FALSE.
C      CALL REACT
C      IF(NLM.EQ.O) WRITE(6,52)
C      52 FORMAT(24HOERROR IN REACTANT CARDS)
C      CALCH = .FALSE.
C      DO 755 N=1,NREAC
C      IF(NAME(N,5).EQ.IZ) CALCH=.TRUE.
C      755 CONTINUE
C      GO TO 203
C
C      READ THERMO DATA FROM CARDS AND STORE ON TAPE 4
C
C      NEWR = .TRUE.
C      90 REWIND 4
C      READ(5,5) TLOW,TMID,THIGH
C      5   FORMAT (3F10.3)
C      WRITE (4,5) TLOW,TMID,THIGH
C      97 READ (5,10)(DAT(I),I=1,16),NCD(1)
C      10   FORMAT(3A4,6X,2A3,4(A2,F3.0),A1,2F10.3,I15)
C      IF(DATA(1).EQ.BLANK) DATA(1)=END
C      WRITE (4,10)(DAT(I),I=1,16)
C      IF(DATA(1).NE.END) LAST
C      WRITE(4,10) LAST
C      GO TO 203

```

```

18 READ(5,20)(DAT(I),I=1,5),NCD(2),(DAT(J),J=6,10),NCD(3),(DAT(K),
1K=1,14),NCD(4)
20 FORMAT(5E15.8,I5/5E15.8,I5/4E15.8,I20)
21 WRITE(4,21)(DAT(I),I=1,14)
21 FORMAT(5E15.8/5E15.8/4E15.8)
DO 25 I=1,4
IF(NCD(I).EQ.1) GO TO 25
WRITE(6,22) (DATA(J),J=1,3)
22 FORMAT(28HOERROR IN ORDER OF CARDS FOR ,3A4)
25 CONTINUE
GO TO 97

C
C
C CHECK INSERT CARDS
180 DO 185 I=4,15,3
IF (DATA(I).EQ.BLANK) GO TO 185
INSERT = INSERT+1
INSERT(1,INSERT) = DATA(I)
INSERT(2,INSERT) = DATA(I+1)
INSERT(3,INSERT) = DATA(I+2)
185 CONTINUE
GO TO 203

C
C
C CHECK CMIT CARDS
205 DO 208 I=4,15,3
IF(DATA(I).EQ.BLANK) GO TO 208
NCMIT = NCMIT+1
CMIT(1,NCMIT) = DATA(I)
CMIT(2,NCMIT) = DATA(I+1)
CMIT(3,NCMIT) = DATA(I+2)
208 CONTINUE
NEWIR=.TRUE.
REWIND 4
GO TO 203

C
C
C BEGIN NAMELIST INPT2
210 DO 300 I=1,26
P(I)=0.
T(I)=0.
V(I)=0.
300 CONTINUE
TRACE=0.
SO=0.
V1=0.
V2=0.
CR=0.
RHOP=0.
KASE=0

```

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MAIN 93
MAIN 94
MAIN 95
MAIN 96
MAIN 97
MAIN 98
MAIN 99
MAIN 100
MAIN 101
MAIN 102
MAIN 103
MAIN 104
MAIN 105
MAIN 106
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MAIN 109
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MAIN 129
MAIN 130
MAIN 131
MAIN 132
MAIN 133
MAIN 134
MAIN 135
MAIN 136
MAIN 137
MAIN 138
MAIN 139
MAIN 140
MAIN 141

```

```

142  TP = .FALSE.
143  HP=.FALSE.
144  SP=.FALSE.
145  TV = .FALSE.
146  UV = .FALSE.
147  SV = .FALSE.
148  OTTO = .FALSE.
149  RKKT = .TRUE.
150  SHOCK = .FALSE.
151  DETN = .FALSE.
152  VOL = .FALSE.
153  MMHG = .FALSE.
154  PSIA = .TRUE.
155  NSQM = .FALSE.
156  SIUNIT = .FALSE.
157  EUNITS = .FALSE.
158  IONS = .FALSE.
159  IDEBUG = 0
160  FA = .FALSE.
161  OF = .TRUE.
162  ERATIO = .FALSE.
163  FPCT = .FALSE.
164  DO 303 I=1,15
165  MIX(I) = 0.
166  CONTINUE
167  NT = 1
168  EQL = .TRUE.
169  READ(5,INPT2)
170  P(1)=PGPSIA
171  MIX(1)=OXFUL(KZONE)
172  WRITE(6,INPT2)
173  IF(.NOT.DETN.AND..NOT.SHOCK) GO TO 1303
174  DO 1300 N=1,NREAC
175  IF(FAZ(N).NE.GAS) GO TO 1301
176  CONTINUE
177  GO TO 1303
178  WRITE(6,1302)
179  FORMAT(60HOCONDENSED REACTANTS NOT PERMITTED IN DETN OR SHOCK PROB
180  1LEMS)
181  GO TO 1
182  IF(.NOT.TV.AND..NOT.UV.AND..NOT.SV) GO TO 304
183  VOL = .TRUE.
184  DC 1304 I=1,26
185  IF(RHO(I).NE.0.) VL(I) = 1./RHO(I)
186  IF(V(I).NE.0.) VL(I)=V(I)
187  IF(VL(I).EQ.0.) GO TO 1305
188  NP = I
189  CONTINUE
190  TP = TV
191  HP = UV
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304 SP = SV
GO TO 322
DO 305 I=1,26
IF(P(I).EQ.0.) GO TO 322
NP = I
IF (MMHG) P(NP) = P(NP)/760.
IF(PSIA) P(NP)=P(NP)/14.696006
IF(NSQM) P(NP)=P(NP)/101325.
CONTINUE
305 DO 307 IT = 1,26
322 IF (T(IT).EQ.0.) GO TO 722
NT = IT
CONTINUE
307 DO 625 IST=1,15
722 IF(WP(1).EQ.0.) OXF(IST)=0.
IF(MIX(IST).NE.0.) GO TO 323
IF(IST.NE.1) GO TO 745
WRITE(6,724)
724 FORMAT(48HONO INPT2 VALUE GIVEN FOR OF, EQAT, FA, OR FPCT )
IF (WP(2).NE.0.) OXFL = WP(1)/WP(2)
GO TO 333
323 OXFL = MIX(IST)
IF(FA) OXFL=1./MIX(IST)
IF(FPCT) OXFL=(100.-MIX(IST))/MIX(IST)
IF(.NOT.ERATIO) GO TO 333
EQAT = MIX(IST)
IF(EQAT.EQ.1.) EQAT = 1.000005
OXFL = (-EQAT*VMIN(2)-VPLS(2))/(VPLS(1)+EQAT*VMIN(1))
333 OXF(IST) = OXFL
NOF = IST
CONTINUE
625 IF (.NOT.IONS) GO TO 746
745 IF(LLMT(NLM).EQ.IE) GO TO 748
NLM = NLM+1
IF(LLMT(NLM).EQ.IE) GO TO 748
LLMT(NLM) = IE
BOP(NLM,1) = 0.
BOP(NLM,2) = 0.
GO TO 747
746 IF(LLMT(NLM).EQ.IE) NLM=NLM-1
NLM1 = NLM+1
IF(LLMT(NLM1).NE.IE) GO TO 748
LLMT(NLM1) = 0
NLMR = .TRUE.
747 REWIND 4
748 IF(NEWNR) CALL SEARCH
IF(NS.EQ.0) GO TO 1
C INITIAL ESTIMATES
C
C

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SO = SO/R
ENN = .1
ENNL = -2.3025851
SUMN = ENN
XI = NS - NC
XLN = ENN/XI
DO 432 J=1,NS
  IF(IUSE(J).GT.0) IUSE(J)=-IUSE(J)
  ENL(J) = 0.
  IF (IUSE(J).NE.0) GO TO 432
  ENL(J) = XI
  ENLN(J) = XLN
CONTINUE
432 IQI = NL+1
  IF (NC.EQ.0.OR.NSERT.EQ.0) GO TO 790
  DO 302 I=1,NSERT
    INC = 0
    DO 301 J=1,NS
      IF(IUSE(J).EQ.0) GO TO 301
      INC = INC+1
      IF(SUB(J,1).NE.INSERT(1,I)) GO TO 301
      IF(SUB(J,2).NE.INSERT(2,I)) GO TO 301
      IF(SUB(J,3).NE.INSERT(3,I)) GO TO 301
      IF(T(I).EQ.0.) GO TO 295
      IF(T(I).LT.TEMP(INC,1).OR.T(I).GT.TEMP(INC,2)) GO TO 301
      IQI = IQI+1
      IUSE(J) = -IUSE(J)
    GO TO 302
  CONTINUE
301 CONTINUE
302 CONTINUE
790 IF(.NOT.TP.AND..NOT.HP.AND..NOT.SP) GO TO 791
  CALL THERMP
  GO TO 800
791 CONTINUE
  IF(DETN) CALL DETON
  IF(RKKT) CALL ROCKET
  IF(SHOCK) CALL SHCK
  NSERT = 0
  GO TO 1
END
  
```

```

C
C
C
SUBROUTINE REACT
LOGICAL HP,SP,TP,      CONVG,NEWR,IONS,MOLES,EQL,FROZ,VOL
DIMENSION ANAME(15,5),V(15),LLMTS(15),SBOP(15,2)
COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),BO(15),BOP(15,2)
1  ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AC(2),AM(2)
2  ,HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
3  ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4  ,RHOP,RMW(15),TLN,CR,OXF(15),ENNL,ENSAVE,ENLSAV,TRACE
C COMMON/INOX/  IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM
1  ,NS,KMAT,IMAT,IQ1,NOF,NOMIT,IP,NEWR,NSUB,NSUP,ITM,CPCVFR,CPCVEQ
2  ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JSI,VOL,SHOCK,IT,NFZ,CALCH
3  ,IQSAVE,LSAVE,ISUP,ISUB,ITNUM
EQUIVALENCE (NAME,ANAME),(NLM,L),(BLANK,LANK)
DATA MOL/IHM/,CX/IHO/,LANK/IH /,IZERO/2HOO/,NLS/O/,ZERO/IHO/
DO 10 K=1,2
WP(K)=0.
HPP(K)=0.
RH(K)=0.
VPLS(K)=0.
VMIN(K)=0.
AM(K)=0.
DO 8 J=1,15
LLMT(J)=0
BOP(J,K)=0.
10 CONTINUE
8 NFUEL = 0
N=1
L=1
C
C
C
READ AND WRITE REACTANT CARDS
20 READ(5,21)(NAME(N,I),ANUM(N,I),I=1,5),PECWT(N),MOLE,ENTH(N),FAZ(N)
1  ,RTEMP(N),FOX(N),DENS(N)
21 FORMAT(5(A2,F7.5),F7.5,A1,F9.5,A1,F8.5,A1,F8.5)
IF(NAME(N,1).EQ.LANK) GO TO 200
IF(L.EQ.0)GO TO 20
WRITE (6,31)(NAME(N,I),ANUM(N,I),I=1,5),PECWT(N),MOLE,ENTH(N),FAZ
1  (N),RTEMP(N),FOX(N),DENS(N)
31 FORMAT(1X,5(A2,1X,F7.4,2X),F10.6,2X,A1,F11.2,2X,A1,2X,F8.3,2X,
1A1,3X,F8.5)
35 IF(MOLE.EQ.MOL) MOLES=.TRUE.
C
C
C
IF OXIDANT, K=1

```

```
C
C
IF FUEL, K=2
IF(FOX(N).EQ.ZERO) FOX(N)=OX
K=1
IF(FOX(N).EQ.OX) GO TO 37
K=2
NFUEL = NFUEL+1
DO 38 J=1,15
DATA(J) = 0.
CONTINUE
RM=O.

STORE ATOMIC SYMBOLS IN LLMT ARRAY.
CALCULATE MOLECULAR WEIGHT.
TEMPORARILY STORE ATOMIC VALENCE IN V.

DO 100 JJ=1,5
IF(ANUM(N,JJ).EQ.O.)GO TO 101
IF(ANAME(N,JJ).EQ.ZERO) ANAME(N,JJ)=OX
DO 41 J=1,15
NJ = J
IF(LLMT(J).EQ.O) GO TO 45
IF(ANAME(N,JJ).EQ.LLMT(J))GO TO 46
CONTINUE
L = NJ
LLMT(J)=NAME(N,JJ)
DO 48 KK=1,101
IF(ATOM(1,KK).EQ.ANAME(N,JJ))GO TO 50
CONTINUE
L=L+1
GO TO 20
RM=RM+ANUM(N,JJ)*ATOM(2,KK)
V(J)=ATOM(3,KK)
DATA(J)=ANUM(N,JJ)
CONTINUE

ADD CONTRIBUTIONS TO WP(K), HPP(K), AM(K), BOP(I,K) AND RH(K)

PCWT=PECWT(N)
IF(MOLES) PCWT=PCWT*RM
WP(K)=WP(K) + PCWT
EM = ENTH(N)
IF(ANAME(N,5).NE.IZERO)HPP(K)=HPP(K)+EM
AM(K)=AM(K)+PCWT/RM
DO 110 J=1,L
BOP(J,K)=DATA(J)*PCWT/RM+BOP(J,K)
CONTINUE
IF(DENS(N).NE.O.)GO TO 115
GO TO 117
RH(K)=RH(K)+PCWT/DENS(N)
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117 RMW(N) = RM
    N = N+1
    IF(N.NE.16) GO TO 20
200 NREAC=N-1
    IF(NFUEL.GT.0) GO TO 210
C
C
C    100 PERCENT OXIDANT, CALL REACTANTS FUEL
C
C    DO 205 N=1,NREAC
C      FOX(N) = BLANK
C      CONTINUE
C    205 RH(2) = RH(1)
C      RH(1) = O
C      WP(2) = WP(1)
C      WP(1) = O
C      HPP(2) = HPP(1)
C      AM(2) = AM(1)
C      AM(1) = O
C    208 J=1,L
C      BOP(J,2) = BOP(J,1)
C      CONTINUE
C    210 IF(L.EQ.0) GO TO 1000
C
C      NORMALIZE HPP(K),AM(K),BOP(I,K), AND PECWT(N).
C      CALCULATE RH(K), V+(K), AND V-(K)
C
C      DO 220 K=1,2
C      IF(WP(K).EQ.0.)GO TO 220
C      HPP(K)=HPP(K)/WP(K)
C      AM(K) = WP(K)/AM(K)
C      IF(RH(K).NE.0.)RH(K)=WP(K)/RH(K)
C      DO 215 J=1,L
C      BOP(J,K)=BOP(J,K)/WP(K)
C      IF(V(J).LT.0.)VMIN(K)=VMIN(K)+BOP(J,K)*V(J)
C      IF(V(J).GT.0.)VPLS(K)=VPLS(K)+BOP(J,K)*V(J)
C      CONTINUE
C      IF(MOLES) GO TO 220
C      DO 218 N=1,NREAC
C      IF(FOX(N).EQ.OX.AND.K.EQ.2) GO TO 218
C      IF(FOX(N).NE.OX.AND.K.EQ.1) GO TO 218
C      PECWT(N) = PECWT(N)/WP(K)
C      CONTINUE
C    218 CONTINUE
C    220 NEWR=.TRUE.
C
C    ARE ELEMENTS SAME AS FOR LAST SET OF REACTANTS, IF SO, NEWR=.FALSE.
C
C      IF(NLM.NE.NLS) GO TO 226
C      IF(NOMIT.NE.O) GO TO 226
C      DO 224 I=1,NLS

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DO 222 J=1,NLM
IF(LLMT(J).NE.LLMTS(I)) GO TO 222
SBOP(I,1) = SBOP(J,1)
SBOP(I,2) = SBOP(J,2)
GO TO 224
222 CONTINUE
GO TO 226
224 CONTINUE
NEW = .FALSE.
DO 225 I=1,NLM
LLMT(I) = LLMTS(I)
SBOP(I,1) = SBOP(I,1)
SBOP(I,2) = SBOP(I,2)
225 CONTINUE
GO TO 229

C
226 NLS = NLM
NOMIT = 0
REWIND 4
DO 228 I=1,NLM
LLMTS(I) = LLMT(I)
CONTINUE
228 DO 230 N=1,NREAC
229 IF (DENS(N).NE.O.) GO TO 230
RH(2) = 0.
RH(1) = 0.
GO TO 1000
230 CONTINUE
1000 RETURN
END

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SUBROUTINE SEARCH
SEARCH TAPE FOR THERMO DATA FOR SPECIES TO BE CONSIDERED
THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR
IRM 360 MACHINES ONLY

DOUBLE PRECISION COEF,S,EN,ENLN,H0,DELN
INTEGER SUB,CMIT,END,TOOBIG
LOGICAL NEWR,OTTO
DIMENSION DATE(2,3),MT(4),B(4),OMIT(3,3),NAM(3),TOOBIG(3,50)
COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)
1,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2),SLN(150)
COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),BO(15),BOP(15,2)
1,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCY,R,RR,HSUBO,AC(2),AM(2)
2,HPP(2),RH(2),VMIN(2),VPLS(2),WPI(2),DATA(22),NAME(15,5)
3,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4,RHOP,RMW(15),TLN,CR,OXF(15),ENNL,ENSAVE,ENLSAV,TRACE
COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NLM
1,NS,KMAT,IMAT,IQI,NOF,NOMIT,IP,NEWR,NSUB,NSUP,ITM,CPCVFR,CPCVEQ
2,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JSI,VOL,SHOCK,IT,NFZ,CALCH
3,IQSAVE,LSAVE,ISUP,ISUB,ITNUM

EQUIVALENCE (DATE,EN),(OMIT,ENLN),(ENDD,END),(TOOBIG,ENLN)

DATA GAS/IHG/,END/3HEND/
I2B = 0
NC = 0
IX = 0

CHECK DIMENSION FOR NUMBER OF SPECIES, CLEAR A(I,J)

SUB(1,1) = END
DO 3 I=1,1000
IF(A(1,I).EQ.ENDD) GO TO 4
DO 3 J=1,NLM
A(J,I) = 0.
3 CONTINUE
4 MAXNS = I-1

READ TEMPERATURE RANGES FOR COEFFICIENTS OF GASEOUS SPECIES.
READ(4,5) TLOW,TMID,THIGH
5 FORMAT (3F10.3)
NS = 1

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C
C
C BEGIN LOOP FOR READING SPECIES DATA FROM TAPE.
      7 READ      (4,10)(NAM(I),I=1,3), DATE(1,NS),DATE(2,NS), (MT(J),B(J),
1      J=1,4), PHAZ,I1,T2
10  FORMAT(3A4,6X,2A3,4(A2,F3.0),A1,2F10.3)
    IF(NAM(I).EQ.END) GO TO 171
    READ      (4,20) ((COEF(I,J,NS),J=1,7),I=1,2)
20  FORMAT(5E15.8)
    IF(NOMIT.EQ.0) GO TO 810
    DO 805 I=1,NCMIT
    DO 804 J=1,3
    IF(OMIT(J,I).NE.NAM(J)) GO TO 805
804  CONTINUE
    GO TO 7
805  CONTINUE
810  DO 820 K=1,4
    IF(B(K).EQ.0.) GO TO 825
    DO 168 I=1,NLM
    IF(LLMT(I).EQ.MT(K)) GO TO 820
168  CONTINUE
    IF(NS.GT.MAXNS) GO TO 7
    DO 819 J=1,NLM
    A(J,NS) = 0.
819  GO TO 7
820  IF(NS.LE.MAXNS) A(I,NS) = B(K)
825  IF(NS.LE.MAXNS) GO TO 828
    I2B = I2B+1
    DO 826 I=1,3
    TOOBIG(I,I2B) = NAM(I)
    GO TO 7
828  DO 829 I=1,3
829  SUB(NS,I) = NAM(I)
    IUSE(NS) = 0
    IF(PHAZ.EQ.GAS) GO TO 170
C
C
C CONDENSED SPECIES
NC= NC+1
TEMP(NC,1)= T1
TEMP(NC,2)= T2
IX= IX+1
IF(NS.EQ.1.OR.IUSE(NS-1).EQ.0) GO TO 145
DO 830 I=1,NLM
IF(A(I,NS).NE.A(I,NS-1)) GO TO 145
830  CONTINUE
IX= IX-1
145  IUSE(NS)= -IX
170  NS= NS+1
    GO TO

```

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SRCH 100

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SRCH 101  
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SRCH 104  
SRCH 105  
SRCH/106  
SRCH 107  
SRCH 108  
SRCH 109  
SRCH 110  
SRCH/111  
SRCH/112  
SRCHA 112  
SRCH 113  
SRCH 114  
SRCH 115  
SRCH 116  
SRCH 117  
SRCH 118  
SRCH 119  
SRCH 120  
SRCH 121  
SRCH 122

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C      END CARD HAS BEEN READ.
C
C      171  NS= NS-1
C      NEWR= .FALSE.
C      WRITE(6,172)
C      172  FORMAT(42H0SPECIES BEING CONSIDERED IN THIS SYSTEM )
C      DO 174 I=1,NS,5
C      I5= I+4
C      174  WRITE (6,176)(DATE(1,J),SUB(J,1),SUB(J,2),SUB(J,3),J=1,
C      1  I5)
C      174  CONTINUE
C      176  FORMAT(5(5X,2A3,2X,3A4))
C      IF(I28.GT.0) GO TO 870
C      RETURN
C      870  WRITE(6,871) I2B
C      871  FORMAT(35H0INSUFFICIENT STORAGE FOR FOLLOWING,I3,8H SPECIES)
C      880  WRITE(6,880)(TOOBIG(1,J),TOOBIG(2,J),TOOBIG(3,J),J=1,I2B)
C      FORMAT(8(3X,3A4))
C      NS = 0
C      RETURN
C      END

```

```

C      SUBROUTINE HCALC
C      CALCULATE PROPERTIES FOR TOTAL REACTANT USING THERMO DATA FOR
C      ONE OR MORE REACTANTS.
C
C      THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR
C      IBM 360 MACHINES ONLY
C
C      DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS
C      DOUBLE PRECISION COEF,S,EN,ENLN,HO,DELN
C
C      LOGICAL MOLES,VOL,SHOCK,CALCH
C      CALCULATE ENTHALPY FOR PROPELLANT USING COEFFICIENTS
C      DIMENSION NUM(15,5)
C
C      COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
C      1 ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),YTT(13)
C      2 ,VLM(13),TOTN(13)
C      COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),HO(150)
C      1 ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2),SLN(150)
C      COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),BO(15),BOP(15,2)
C      1 ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCF,R,RR,HSUBO,AC(2),AM(2)
C      2 ,HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
C      3 ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
C      4 ,RHOP,RMW(15),TLN,CR,OXF(15),ENNL,ENSAVE,ENLSAV,TRACE
C      COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM
C      1 ,NS,KMAT,IMAT,IQI,NOF,NOMIT,IP,NEW,NSUB,NSUP,ITM,CPCVFR,CPCVEQ
C      2 ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JSI,VOL,SHOCK,IT,NFZ,CALCH
C      3 ,IQSAVE,LSAVE,ISUP,ISUB,ITNUM
C
C      EQUIVALENCE (ANUM,NUM),(L,NLM),(J,JSI)
C      EQUIVALENCE (AM1,DATA(20)),(CPRI,DATA(21))
C      DATA AG/1HG/,IZERO/2H00/,OX/1H0/,BLK/1H/
C
C      TSAVE = TT
C
C      CALCULATE MOLECULAR WEIGHT OF TOTAL REACTANT, AM1.
C
C      IF (AM(1).NE.0.0 .AND. AM(2).NE.0.0) GO TO4
C      AM1= AM(2)
C      IF (AM(2).EQ.0.0) AM1= AM(1)
C      GO TO 9
C      4 AM1=(OF+1.)*AM(1)*AM(2)/(AM(1)+OF*AM(2))
C      9 TM = 0.
C      IF (PP.GT.0.) TM = ALOG(PPP*AM1)
C      SSUM(NPT) = 0.
C      HPP(1) = 0.
C      HPP(2) = 0.
C      HSUBO = 0.

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98 HCAL
99 HCAL
100 HCAL

CPR1 = 0.
ANN = (1.+OF)

LOOP ON REACTANTS.
IF OXIDANT, K=1
IF FUEL, K=2

DO 900 N=1,NREAC
K=2
IF(FOX(N).EQ.OX)K=1
IF(NAME(N,5).NE.IZERO) GO TO 90
IF(.NOT.CALCH.AND.TT.NE.O.) GO TO 15
TT = RTEMP(N)

IS TT IN RANGE

15 IF(SHOCK) GO TO 16
IF(TT.LT.(TLOW/1.2).OR.TT.GT.(THIGH*1.2)) GO TO 75
16 J = NUM(N,5)
IF (J.NE.O) GO TO 90
DO 10 J=1,L
DATA(J)=0.
10 CONTINUE

TEMPORARILY STORE STOICHIOMETRIC COEFFICIENTS IN DATA ARRAY.

DO 40 I=1,4
IF(ANUM(N,I).EQ.O.)GO TO 50
DO 20 J=1,L
IF(LLMT(J).EQ.NAME(N,I)) GO TO 30
20 CONTINUE
30 DATA(J)=ANUM(N,I)
40 CONTINUE
50 IS=0

SEARCH FOR REACTANT IN THERMO SPECIES. STORE INDEX IN NUM(N,5).

DO 70 J=1,NS
IF(IUSE(J).EQ.O)GO TO 55
IS = IS+1
IF(FAZ(N).EQ.AG)GO TO 70
IF(TT.GT.TEMP(IS,2).AND.TEMP(IS,2).NE.THIGH) GO TO 70
IF(TT.LT.TEMP(IS,1).AND.TEMP(IS,1).NE.TLOW) GO TO 70
GO TO 56
IF(FAZ(N).NE.AG.AND.FAZ(N).NE.BLK) GO TO 70
55 DO 60 I=1,L
IF(A(I,J).NE.DATA(I)) GO TO 70
60 CONTINUE
NUM(N,5) = J
GO TO 90

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```

70 CONTINUE
GO TO 80

C
C
C
CALCULATE EN FOR REACTANT AND CALL CPHS TO CALCULATE PROPERTIES.

90 IF (MOLES) ENJ = PECWT(N)/WP(K)
IF (.NOT.MOLES) ENJ = PECWT(N)/RMW(N)
ENJ = ENJ/ANN
IF(K.EQ.1) ENJ = ENJ*OF
IF(NAME(N,5).NE.IZERO)GO TO 500
NSS = NS
NS = J
TLN = ALOG(TT)
IF(.NOT.CALCH) EN(J,NPT) = ENJ
CALL CPHS
NS = NSS
IF (HO(J).GT.-.01 .AND. HO(J).LT..01) HO(J) = 0.
RTMP(N) = TT
IF(VOL) HO(J)=HO(J)-1.
ENTH(N) = HO(J)*R*TT

ADD CONTRIBUTION TO CP, H, AND S OF TOTAL REACTANT.

CPRI = CPRI + CPSUM
SSUM(NPT) = SSUM(NPT) + ENJ * (S(J)-ALOG(ENJ)-TM)
ER = ENTH(N)*ENJ/R
HSUBO = HSUBO+ER
HPP(K) = HPP(K)+ER
CONTINUE
IF(TSAVE.NE.0.) TT=TSAVE
GO TO 1000
75 WRITE(6,76)
76 FORMAT(50HOREACTANT TEMPERATURE OUT OF RANGE OF THERMO DATA )
TT = 0.
GO TO 1000
80 WRITE(6,85) N
85 FORMAT(9HOREACTANT,I2,22H IS NOT IN THERMO DATA )
TT = 0.
1000 RETURN
END

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IF(.NOT.CALCH) GO TO 750
CALL HCALC
IF(IT.EQ.0.) RETURN
CALCH = .FALSE.
IF(OF.NE.0.) HPP(1)=SUM#HPP(1)/OF
HPP(2) = SUM#HPP(2)
GO TO 760
750 HSUBO= (OF#HPP(1) + HPP(2))/SUM
760 IC = 0
TEM = SMALB/BIGB
SIZE = 18.420681
IF(TEM.LT.1.E-5) SIZE=ALOG(1000./TEM)
JSOL = 0
JLIQ = 0
WRITE(6,770)
FORMAT(1H,25X,14HEFFECTIVE FUEL,10X,17HEFFECTIVE OXIDANT,12X,7HMI
1XTURE)
IF(VOL) WRITE(6,772)
IF(.NOT.VOL) WRITE(6,774)
FORMAT(16H INTERNAL ENERGY,14X,6HHPP(2),19X,6HHPP(1),19X,5HHSUBO )
772 FORMAT(9H ENTHALPY,21X,6HHPP(2),19X,6HHPP(1),19X,5HHSUBO )
774 WRITE(6,776)HPP(2),HPP(1),HSUBO
776 FORMAT(19H (KG-MOL)(DEG K)/KG,E21.8,2E25.8 )
778 WRITE(6,778)
778 FORMAT(12HOKG-ATOMS/KG,17X,8HBOP(1,2),17X,8HBOP(1,1),18X,5HBO(1))
780 FORMAT(8X,A2,5X,3E25.8)
WRITE(6,780)(LLMT(I),
8OP(1,2),BOP(1,1),BO(1),I=1,NLM)
RETURN
END
SAVE0106
SAVE0107
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SAVE0112
SAVE0113
SAVE0114
SAVE0115
SAVE0116
SAVE/117
SAVE0118
SAVE0119
SAVE0120
SAVE/121
SAVE0122
SAVE0123
SAVE/124
SAVE0125
SAVE/126
SAVE0127
SAVE0128
SAVE/129
SAVE0130
SAVE0131

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SUBROUTINE EQLBRM
ROUTINE TO CALCULATE EQUILIBRIUM COMPOSITION AND PROPERTIES
C
C
C DOUBLE PRECISION X,G,SUM,SUM2,E,BOD
C
C THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR
C IBM 360 MACHINES ONLY
C
C DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS
C DOUBLE PRECISION COEF,S,EN,ENLN,HO,DELN
C DOUBLE PRECISION ENL,PROW,DLNT,AA
C
C LOGICAL HP,SP,TP,CONVG,IONS,SINGC,LOGV,ISING,I35,VOL,SHOCK,RITE
C
C
C COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
1 ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WH(13),SONVEL(13),TTT(13)
2 ,VLM(13),TOTN(13)
C COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),HO(150)
1 ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2),SLN(150)
C COMMON/MISC/ENN,SUMN,IT,SO,ATOM(3,101),BO(15),BOP(15,2)
1 ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AC(2),AM(2)
2 ,HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
3 ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4 ,RHOP,RMW(15),TLN,CR,OXF(15),ENNL,ENSAVE,ENLSAV,TRACE,SIZE
C COMMON/DOUBLE/G(20,21),X(20)
C COMMON/INDEX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM
1 ,NS,KMAT,IMAT,IQI,NOF,NOMIT,IP,NEWB,NSUB,NSUP,ITM,CPCVFR,CPCVEQ
2 ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JSI,VOL,SHOCK,IT,NFZ,CALCH
3 ,IQSAVE,LSAVE,ISUP,ISUB,ITNUM
C
C EQUIVALENCE (NLM,L),(LOGV,CPCVEQ)
C
C DATA IE/1HE/,SMALNO/1.E-6/,SMNOL/-13.815511/,ITN/35/
C
C SINGC = .FALSE.
C PIE = 0.
C I35 = .FALSE.
C E = 2.718281828459
C ENL = ENNL
C RITE = .FALSE.
C IF(IDEBUG.GT.0.AND.NPT.GE.IDEBUG) RITE=.TRUE.
C ISING = .FALSE.
C LOGV = .FALSE.
C IF(.NOT.VOL) GO TO 6
C RV = RV/101.325
C PP = RV*ENN#TT/VLM(NPT)
C TLN = ALOG(TT)
C CONVG = .FALSE.
C ITNUMB = ITN
6

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49 JS1 = 1
50 CALL CPHS
51 TM = ALOG(PP/ENN)
52
53 IF (.NOT. IGNS.OR. IE.EQ. LLMT(L)) GO TO 33
54 L = L+1
55 IQ1 = IQ1+1
56 DO 499 J = 1, NS
57 IF (A(L,J) .EQ. 0.) GO TO 499
58 EN(J,NPT) = 1.E-8
59 ENLN(J) = -SIZE
60 CONTINUE
61 IF(NPT.EQ.1.AND..NOT.SHOCK) WRITE(6,244)(LLMT(I), I=1,L)
62 IF(NPT.EQ.1) CONTINUE
63 FCFORMAT (4HOPT, 14(5X,A4))
64
65 BEGIN ITERATION
66
67 IF (.NOT. CONVG) GO TO 62
68 SUMN = ENN
69 IF(J SOL.EQ. 0) GO TO 62
70 ENSOL = EN(J SOL, NPT)
71 EN(J SOL, NPT) = EN(J SOL, NPT) + EN(J LIQ, NPT)
72 IUSE(J LIQ) = -IUSE(J LIQ)
73 IQ1 = IQ1-1
74 DLVTP(NPT) = 0.
75 CPR(NPT) = 0.
76 GAMMAS(NPT) = 0.
77 LOGV = .TRUE.
78 CALL MATRIX
79 NUMB = ITN-ITNUMB+1
80 IQ2 = IQ1 + 1
81 IF(.CONVG) IMAT=IMAT-1
82 IF(.NOT.RITE) GO TO 72
83 IF(.NOT. CONVG) GO TO 88
84 IF(.NOT. LOGV) WRITE(6,81)
85 FCFORMAT(15HOT DERIV MATRIX)
86 IF(.LOGV) WRITE(6,82)
87 FCFORMAT(15HOP DERIV MATRIX)
88 GO TO 89
89 WRITE(6,772) NUMB
90 FCFORMAT(11HOITERATION, 13, 6X, 7HMATRIX //)
91 DO 911 I=1, IMAT
92 WRITE(6,73) (G(I,K), K=1, KMAT)
93 ITST = IMAT
94 CALL GAUSS
95 IF(ITST.NE. IMAT) GO TO 774
96 IF(.NOT. RITE) GO TO 773
97 WRITE(6,373)(LLMT(I), I=1,L)
98 FCFORMAT (7HOPI, 9(A4, 10X))

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73      WRITE (6,73)(X(I),I=1,IMAT)
773     FORMAT (9E14.6)
       IF(.NOT.CONVG) GO TO 85
       IF(.NOT.LOGV) GO TO 174
       GO TO 171
C
C
C     TEMPERATURE DERIVATIVES--CONVG=T, LOGV=F
174     DLVTP(NPT) = 1.-X(IQ1)
175     CPR(NPT) = G(IQ2,IQ2)
       DO 176 J=1,IQ1
176     CPR(NPT) = CPR(NPT)-G(IQ2,J)*X(J)
       CONTINUE
C
C
C     PRESSURE DERIVATIVE--CONVG=T, LOGV=T
       LOGV = .TRUE.
       GO TO 62
C
C
C     SINGULAR MATRIX
774     IF(.NOT.CONVG) GO TO 775
       WRITE(6,172)
172     FORMAT(28HDERIVATIVE MATRIX SINGULAR )
       GO TO 1171
775     IF(.NOT.HP.OR.NPT.NE.1.OR.NC.EQ.0.OR.TT.GT.100.) GO TO 871
       WRITE(6,874)
874     FORMAT(96HLOW TEMPERATURE IMPLIES CONDENSED SPECIES SHOULD HAVE
18EEN INCLUDED ON AN INSERT CARD, RESTART )
       GO TO 873
871     WRITE(6,774)
774     FORMAT(16HSINGULAR MATRIX)
       IF(SINGC) GO TO 873
       DO 970 JJ = 1, NS
       IF(IUSE(JJ).NE.O) GO TO 970
       IF(EN(JJ,NPT).NE.O.) GO TO 970
       ENLJ(NPT) = SMALNO
970     CONTINUE
       IF(ISING) GO TO 870
       ISING = .TRUE.
       WRITE (6,776)
776     FORMAT (8HORESTART)
       GO TO 62
C
C
C     TEST FOR SINGULARITY TO CONDENSED SPECIES.
870     NCOND = IQ1-NLM-2
       IF(TP.OR.VOL) NCOND=NCOND+1
       IF(NCOND.LT.2.OR.SIZEG.EQ.0.) GO TO 873

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DO 872 J=1,NS
IF(IUSE(J).LE.O.) GO TO 872
IF(J.EQ.JDELG) GO TO 872
DO 671 I=1,NLM
IF(A(I,J).EQ.A(I,JDELG)) GO TO 671
IF(A(I,J).EQ.O.OR.A(I,JDELG).EQ.O.) GO TO 872
671 CONTINUE
SINGC = .TRUE.
IQ1 = IQ1-1
EN(J,NPT) = 0.
IUSE(J) = -IUSE(J)
CONTINUE
872 IF(SINGC) GO TO 40
GO TO 873

C
C
C
OBTAIN CORRECTIONS TO THE ESTIMATES

85 ITNUMB= ITNUMB-1
KK = L + 1
IF(VOL) X(IQ2)=X(IQ1)
IF(TP) X(IQ2)=0.
DLNT= X(IQ2)
SUM = X(IQ1)
IF(.NOT.VOL) GO TO 97
X(IQ1) = 0.
SUM = -DLNT
97 DO 101 J=1,NS
IF(IUSE(J)) 101,98,100
DELN(J) = HO(J)*DLNT-HO(J)+S(J)-ENLN(J)-TM*SUM
DO 99 K=1,L
DELN(J)= DELN(J)+A(K,J)*X(K)
CONTINUE
99 IF(PIE.NE.O.) DELN(J)=DELN(J)+A(L+1,J)*PIE
GO TO 101
100 DELN(J) = X(KK)
KK = KK + 1
101 CONTINUE

C
C
C
CALCULATE CONTROL FACTOR, AMBDA
AMBDA= 1.
AMBDA1= 1.
SUM = X(IQ1)
IF(SUM.LT.O.) SUM=-SUM
IF(DLNT.GT.SUM) SUM=DLNT
IF(-DLNT.GT.SUM) SUM=-DLNT
DO 917 J=1,NS
IF(IUSE(J).NE.O.) GO TO 917
IF((EN(J,NPT).GT.O.).AND.DELN(J).LE.O.) SUM = DELN(J)
IF((EN(J,NPT).NE.O.) .OR. DELN(J).LE.O.) GO TO 917

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ENN = E*ENL
GO TO 1115
2115 ENN = SUMN
ENL = ALOG(ENN)
PP = RV*TT*ENN/VLM(NPT)
1115 TM = ALOG(PP/ENN)
IF (LLMT(L).NE.IE) GO TO 116
C
C CHECK ON REMOVING IONS
C
DO 1116 J = 1,NS
IF (A(L,J).EQ.0.) GO TO 1116
IF (EN(J,NPT).GT.0.) GO TO 116
1116 CONTINUE
PIE = X(L)
L = L-1
IQL = IQL-1
GO TO 43
C
C TEST FOR CONVERGENCE
C
116 IF (ITNUMB.EQ.0) GO TO 14
IF (AMBDA.LT.1.) GO TO 43
SUM = X(IQL)
IF (SUM.LT.0.) SUM = -SUM
IF (SUM.GT.0.5E-5) GO TO 43
DO 130 J=1,NS
IF (IUSE(J).LT.0) GO TO 130
AA = DELN(J)/SUMN
IF (AA.LT.0.) AA = -AA
IF (IUSE(J).EQ.0) AA = AA*EN(J,NPT)
IF (AA.GT.0.5E-5) GO TO 43
130 CONTINUE
LE = L
IF (TRACE.EQ.0.) GO TO 275
IF (ITN.GT.35) GO TO 222
ITN = ITN+15
ITNUMB = ITNUMB+15
222 DO 225 I=1,NLM
IF (BO(I).EQ.0.) GO TO 227
SUM = 0.
DO 223 J=1,NS
223 SUM = SUM+EN(J,NPT)*A(I,J)
BO = DBLE(BO(I))
IF (DABS(BO -SUM)/BOD .GT..0001) GO TO 43
225 CONTINUE
227 IF (.NOT.IONS) GO TO 275
C
C CHECK ON ELECTRON BALANCE
C

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229 IF(PIE.NE.0.) LE=L+1
    IF(PIE.EQ.0.) PIE=X(L)
    ITER = 1
    SUM2 = 0.
    SUM = 0.
    DO 230 J=1,NS
        IF(IUSE(J).LT.0.OR.A(LE,J).EQ.0.) GO TO 230
        IF(ENLN(J).GT.-87.) EN(J,NPT)=E*ENLN(J)
        AN = A(LE,J)*EN(J,NPT)
        IF(EN(J,NPT)/ENN.GT.1.E-7) GO TO 275
        SUM = SUM+AN
        SUM2 = SUM2+AN*A(LE,J)
    CONTINUE
230 IF(SUM2.EQ.0.) GO TO 275
    DPIE = -SUM/SUM2
    DO 250 J=1,NS
        IF(A(LE,J).EQ.0.) GO TO 250
        ENLN(J) = ENLN(J)+A(LE,J)*DPIE
    CONTINUE
250 IF(ABS(DPIE).LE..0001) GO TO 275
    PIE = PIE+DPIE
    ITER = ITER+1
    IF(ITER.LE.1TN) GO TO 229
    WRITE(6,260)
260 FORMAT(37H0DID NOT CONVERGE ON ELECTRON BALANCE)
    GO TO 873
275 CONTINUE

C
C
C    CALCULATE ENTROPY, CHECK ON DELTA S FOR SP PROBLEMS
    TOTN(NPT) = 0.
    SSUM(NPT) = 0.
    DO 183 J=1,NS
        IF(IUSE(J).LT.0) GO TO 183
        TOTN(NPT) = TOTN(NPT) + EN(J,NPT)
        SS = S(J)
        IF(IUSE(J).EQ.0) SS=SS-ENLN(J)-TM
        SSUM(NPT) = SSUM(NPT)+SS*EN(J,NPT)
    CONTINUE
183 IF(.NOT.SP) GO TO 13
    SS = SSUM(NPT) - SO
    IF(SS.LT.(-0.00005).OR.SS.GT.0.00005) GO TO 43
    IF(RITE) WRITE(6,1183) SS
1183 FORMAT(12H0DELTA S/R =,E15.8)
C
13 CONVG= .TRUE.
    GO TO 160
14 WRITE(6,973) ITN,NPT
973 FORMAT(14H12,69H ITERATIONS DID NOT SATISFY CONVERGENCE REQUIREME
    INTS FOR THE PCINT
15)
EQLM 283
EQLM 284
EQLM 285
EQLM 286
EQLM 287
EQLM 288
EQLM 289
EQLM 290
EQLM 291
EQLM 292
EQLM 293
EQLM 294
EQLM 296
EQLM 297
EQLM 298
EQLM 299
EQLM 300
EQLM 301
EQLM 302
EQLM 303
EQLM 304
EQLM 305

```

```

IF(NC.EQ.0.OR.I35) GO TO 873
I35 = .TRUE.
IF (.NOT.HP.OR.NPT.NE.1.OR.IT.GT.100.) GO TO 261
WRITE(6,874)
GO TO 873
261 NCOND = IQ1-NLM-2
    IF(TP.OR.VOL) NCOND=NCOND+1
    IF(NCOND.NE.1.OR.ENN.GT.1.E-4) GO TO 873
C HIGH TEMPERATURE, INCLUDED CONDENSED CONDITION
WRITE(6,265)
265 FORMAT(31HTRY REMOVING CONDENSED SPECIES)
ENN = .1
ENL = -2.3025851
SUMN = ENN
XI = NS - NC
XI = ENN/XI
XLN = ALOG(XI)
DO 432 J=1,NS
    IF(IUSE(J).GT.0) IUSE(J)=-IUSE(J)
    ENL(N(J)) = 0.
    IF (IUSE(J).NE.0) GO TO 432
    EN(J,NPT) = XI
    ENL(N(J)) = XLN
432 CONTINUE
    IQ1 = NLM+1
    GO TO 40
C
C CONVERGENCE TESTS ARE SATISFIED, TEST CONDENSED SPECIES.
C
160 IF(NC.EQ.0) GO TO 143
    DO 146 J=1,NS
        IF(EN(J,NPT).GE.0.) GO TO 146
        IF (J.NE.JSOL .AND. J.NE.JLIQ) GO TO 147
        JSOL = 0
        JLIQ = 0
147 IQ1 = IQ1 - 1
        EN(J,NPT) = 0.
        GO TO 166
146 CONTINUE
        SIZEG = 0.
        INC = 0
        DO 170 J = 1,NS
            IF(IUSE(J).EQ.0) GO TO 170
            INC = INC + 1
            IF(RITE) WRITE(6,144)(SUB(J,I),I=1,3),TEMP(INC,1),TEMP(INC,2),IUSE
1E(J),EN(J,NPT)
144 FORMAT(1H0,3A4,2F10.3,3X,5HIUSE=,I4,E15.7)
            IF(EN(J,NPT).GT.0.) GO TO 169
            KG = 1

```

EQLM 306  
EQLM 307  
EQLM 308

EQLM 309  
EQLM 310  
EQLM 311  
EQLM 312  
EQLM 313  
EQLM 314  
EQLM 315  
EQLM 316  
EQLM 317  
EQLM 318  
EQLM 319  
EQLM 320  
EQLM 321  
EQLM 322  
EQLM 323  
EQLM 324  
EQLM 325  
EQLM 326  
EQLM 327  
EQLM 328  
EQLM 329  
EQLM 330  
EQLM 331

```

154 IF(IUSE(J).EQ.-IUSE(J+1)) GO TO 154
   IF(J.EQ.1.OR.IUSE(J).NE.-IUSE(J-1)) GO TO 153
   KG = -1
   JKG = J + KG
   TMELT = TEMP(INC,1)
   IMP = INC + KG
   IF(TMELT.EQ.TEMP(IMP,2)) GO TO 158
   TMELT = TEMP(IMP,2)
   IF(TMELT.EQ.TEMP(IMP,1)) GO TO 157
   WRITE(6,156)
156 FORMAT(50H03 PHASES OF A CONDENSED SPECIES ARE OUT OF ORDER )
   GO TO 873

C
C JTH SPECIES A SOLID (EN=0), (J+KG)TH SPECIES A LIQUID (EN IS +)
157 IF(TT.GT.TMELT) GO TO 169
   IF(TP.AND.TT.EQ.TMELT) GO TO 169
   IF(TP) GO TO 1165
   IF(TT.LE.TMELT-150.) GO TO 1165
   JSOL = J
   JLIQ = JKG
   GO TO 159

C
C JTH SPECIES A LIQUID(EN=0), (J+KG)TH SPECIES A SOLID (EN IS +)
158 IF(TT.LT.TMELT) GO TO 169
   IF(TP.AND.TT.EQ.TMELT) GO TO 169
   IF(TP) GO TO 1165
   IF(TT.GE.TMELT+150.) GO TO 1165
   JSOL = JKG
   JLIQ = J
159 TLN = ALOG(TMELT)
   TT = TMELT
   EN(JKG,NPT) = .5 * EN(JKG,NPT)
   EN(J,NPT) = EN(JKG,NPT)
   GO TO 165

C
C WRONG PHASE INCLUDED FOR T INTERVAL, SWITCH EN
1165 EN(J,NPT) = EN(JKG,NPT)
   IUSE(J) = -IUSE(J)
   IUSE(JKG) = -IUSE(JKG)
   EN(JKG,NPT) = 0.
   GO TO 40
153 IF(TT.LT.TEMP(INC,1).AND.TEMP(INC,1).NE.TLOW) GO TO 169
   IF(TT.GT.TEMP(INC,2)) GO TO 169

C
C SUM = 0.
DO 167 I = 1,L

```

EQLM 332  
 EQLM 333  
 EQLM 334  
 EQLM 335  
 EQLM 336  
 EQLM 337  
 EQLM 338  
 EQLM 339  
 EQLM 340  
 EQLM 341  
 EQLM 342  
 EQLM 343  
 EQLM 344  
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 EQLM 370  
 EQLM 371  
 EQLM 372  
 EQLM 373  
 EQLM 374  
 EQLM 375  
 EQLM 376  
 EQLM 377  
 EQLM 378  
 EQLM 379  
 EQLM 380  
 EQLM 381





```

DO 1200 J=1,NS
IF(IUSE(J).NE.0) GO TO 1200
IF(ENLN(J).GT.-87.) EN(J,NPT)=E*ENLN(J)
1200 CONTINUE
200 IF(.NOT.RITE) GO TO 863
WRITE(6,201) NPT, PP, TT, HSUM(NPT), SSUM(NPT), WM(NPT), CPR(NPE
1T), DLVPT(NPT), DLVTP(NPT), GAMMAS(NPT), VLM(NPT)
201 FORMAT(7HOPCINT=I3,3X,2HP=E13.6,3X,2HT=E13.6,3X,4HH/R=E13.6,3X,4HEQLM
1S/R=E13.6//3X,3HMM=E13.6,3X,5HCP/R=E13.6,3X,6HDLVPT=E13.6,3X,6HDLVEQLM
2TP=E13.6,3X,9HGAMMA(S)=E13.6,3X,2HV=E13.6)
863 IF(TT.GE.TLOW.AND.TT.LE.THIGH.OR.SHOCK) GO TO 1000
WRITE(6,306) TT,NPT
306 FORMAT(17H0THE TEMPERATURE=E12.4,26H IS OUT OF RANGE FOR POINT,15)
IF(TT.GE.TLOW/1.5.AND.TT.LE.THIGH*1.25) GO TO 1000
NPT = NPT+1
ERROR, SET TT=0
873 TT=0. NPT-1
RETURN
1000 END

```

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SUBROUTINE CPHS
CALCULATES THERMODYNAMIC PROPERTIES FOR INDIVIDUAL SPECIES

THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR
IBM 360 MACHINES ONLY

DOUBLE PRECISION COEF,S,EN,ENLN,H0,DELN

COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)
1 DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2),SLN(150)
2 COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),BO(15),BOP(15,2)
3 1,FM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,R,RR,HSUBO,AC(2),AM(2)
4 2,HPP(2),RH(2),VMIN(2),VPLS(2),DATA(22),NAME(15,5)
5 3,ANUM(15,5),PECWT(15),ENH(15),FAZ(15),RTEMP(15),DENS(15)
6 4,RHOP,RMW(15),TLN,CR,OXF(15),ENNL,ENSAVE,ENLSAV,TRACE
7 COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NPT,NLM
8 1,NS,KMAT,IMAT,IQI,NOF,NOMIT,IP,NEWNR,NSUB,NSUP,ITM,CPCVFR,CPCVEQ
9 2,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JSI,VOL,SHOCK,IT,NFZ,CALCH
10 3,IQSAVE,LSAVE,ISUP,ISUB,ITNUM

EQUIVALENCE (J,JSI)

K = 1
IF(TT.LE.TMID)K = 2
KK = 0
CPSUM=0.
90 IF(COEF(K,1,J).NE.0.)GO TO 97
IF (IUSE(J).LT.0) GO TO 100

IF COEFFICIENTS ARE ZERO, USE OTHER TEMPERATURE INTERVAL

KK = K
K = 1
IF (KK.EQ.1) K = 2
IF S(J) = (((COEF(K,5,J)/4.)*TT+ COEF(K,4,J)/3.)*TT+ COEF(K,3,J)/2.
1)*TT+COEF(K,2,J))*TT+ COEF(K,1,J))*TLN + COEF(K,7,J)
H0(J) = (((COEF(K,5,J)/5.)*TT+ COEF(K,4,J)/4.)*TT+ COEF(K,3,J)/3.
1)*TT+ COEF(K,2,J)/2.)*TT+ COEF(K,1,J) + COEF(K,6,J))/TT
CPSUM= CPSUM+(((COEF(K,5,J))*TT+ COEF(K,4,J))*TT+ COEF(K,3,J))*TT
1 + COEF(K,2,J))*TT+ COEF(K,1,J))*EN(J,NPT)
IF (KK.EQ.0) GO TO 100
KK = KK
KK = 0
100 IF(J.EQ.NS) GO TO 200
J=J+1
GO TO 90
200 RETURN
END

```





```

65  CONTINUE
   SSS = SSS + G(IQ2,IQ1)
   HSUM(NPT) = HSUM(NPT) + G(IQ1,IQ2)
   G(IQ1,IQ1) = SUMN - ENN
C
C
C   REFLECT SYMMETRIC PORTIONS OF THE MATRIX
C
   ISYM = IQ1
   IF (HP.OR.CONVG) ISYM=IQ2
   DO 102 I=1,ISYM
   DO 102 J=I,ISYM
   G(J,I)=G(I,J)
102 CONTINUE
C
C   COMPLETE THE RIGHT HAND SIDE
C
   IF(.NOT.CONVG) GO TO 140
   IF(.NOT.LOGV) GO TO 175
C
C   LOGV = .TRUE.-- SET UP MATRIX TO SOLVE FOR DLVPT
C
   G(IQ1,IQ2) = ENN
   IQ = IQ1 - 1
   DO 135 I = 1,IQ
   G(I,IQ2) = G(I,IQ1)
135 CONTINUE
   GO TO 175
140 DO 145 I=1,L
   X(I)=BO(I)-G(I,IQ1)
   G(I,KMAT) = G(I,KMAT)+X(I)
145 CONTINUE
   G(IQ1,KMAT) = G(IQ1,KMAT)+ENN-SUMN
C
C   COMPLETE ENERGY ROW AND TEMPERATURE COLUMN
C
   IF (KMAT.EQ. IQ2) GO TO 185
   IF (SP)ENERGY = SO+ENN-SUMN - SSS
   IF (HP)ENERGY=HSUBO/TT - HSUM(NPT)
   G(IQ2,IQ3)=G(IQ2,IQ3)+ ENERGY
175 G(IQ2,IQ2)= G(IQ2,IQ2)+CPSUM
185 IF(.NOT.VOL.CR.CONVG) GO TO 1000
C
C   CONSTANT VOLUME MATRIX
C
   IQ = IQ1-1
   IF (KMAT.EQ.IQ2) GO TO 230
   DO 220 I=1,IQ
   G(IQ1,I) = G(IQ2,I)-G(IQ1,I)
   G(I,IQ1) = G(I,IQ2)-G(I,IQ3)
   G(I,IQ2) = G(I,IQ3)

```

```

MATX 100
MATX 101
MATX 102
MATX 103
MATX 104
MATX 105
MATX 106
MATX 107
MATX 108
MATX 109
MATX 110
MATX 111
MATX 112
MATX 113
MATX 114
MATX 115
MATX 116
MATX 117
MATX 118
MATX 119
MATX 120
MATX 121
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MATX 131
MATX 132
MATX 133
MATX 134
MATX 135
MATX 136
MATX 137
MATX 138
MATX 139
MATX 140
MATX 141
MATX 142
MATX 143
MATX 144
MATX 145
MATX 146
MATX 147
MATX 148
MATX 149

```

```

220 CONTINUE
   G(IQ1,IQ1) = G(IQ2,IQ2)-G(IQ1,IQ2)-G(IQ2,IQ1)
   G(IQ1,IQ2) = G(IQ2,IQ3)-G(IQ1,IQ3)
   IF (UV) G(IQ1,IQ2) = G(IQ1,IQ2) + ENN
   GO TO 260
230 DO 240 I=1,IQ
   G(I,IQ1) = G(I,IQ2)
240 CONTINUE
260 KMAT = IMAT
   IMAT = IMAT-1
1000 RETURN
      END

```

```

MATX 150
MATX 151
MATX 152
MATX 153
MATX 154
MATX 155
MATX 156
MATX 157
MATX 158
MATX 159
MATX 160
MATX 161

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```

SUBROUTINE GAUSS
  SOLVE ANY LINEAR SET OF UP TO 20 EQUATIONS
  NUMBER OF EQUATIONS = IMAT
  DOUBLE PRECISION G,X,COEFX(20),SUM,Z
  COMMON/DOUBLE/G(20,21),X(20)
  COMMON/INDEX/ IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM
  1 ,NS,KMAT,IMAT,IQI,NQF,NOMIT,IP,NEWNR,NSUB,NSUP,ITM,CPCVFR,CPCVEQ
  2 ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JSI,VOL,SHOCK,IT,NFZ,CALCH
  3 ,IQSAVE,LSAVE,ISUP,ISUB,ITNUM
  DATA BIGNO/1.E+38/
  BEGIN ELIMINATION OF NTH VARIABLE
  IUSE1 = IMAT+1
  6 DO 45 NN=1,IMAT
    IF(NN-IMAT) 8,83,8
    83 IF(G(NN,NN)) 31,23,31
  SEARCH FOR MAXIMUM COEFFICIENT IN EACH ROW
  DO 18 I=NN,IMAT
    COEFX(I) = BIGNO
    IF(G(I,NN).EQ.0.) GO TO 18
    COEFX(I) = 0.
    DO 10 J=NN,IUSE1
      SUM = G(I,J)
      IF(SUM.LT.0.) SUM=-SUM
      IF(J.NE.NN) GO TO 9
      Z = SUM
      GO TO 10
    9 IF(SUM.GT.COEFX(I)) COEFX(I)=SUM
    10 CONTINUE
    COEFX(I) = COEFX(I)/Z
    18 CONTINUE
  LOCATE ROW WITH SMALLEST MAXIMUM COEFFICIENT
  TEMP = BIGNO
  I=0
  DO 20 J=NN,IMAT
    IF (COEFX(J)-TEMP) 87,22,22
    87 TEMP=COEFX(J)
    I=J
  22 CONTINUE
  IF(I) 28,23,28

```







```

1 10X,16HCHEMICAL FORMULA,51X,21H(SEE NOTE)    CAL/MOL,10X,5HDEG K,OUTP 51
2 4X,4HG/CC,OUTP 52
  IF(MOLES) WRITE(6,6) OUTP 53
6 FORMAT(79X,5HMOLES,7X, 33H ENERGY STATE TEMP DENSITY/ OUTP 54
1 10X,16HCHEMICAL FORMULA,66X,7HCAL/MOL,10X,13HDEG K G/CC ) OUTP 55
  DO 15 N=1,NREAC OUTP 56
  IF(FOX(N).NE.CX)GO TO 10 OUTP 57
  HD1 = OXID OUTP 58
  HD2 = ANT OUTP 59
  GO TO 11 OUTP 60
10 HD1 = FUEL OUTP 61
11 HD2 = FB OUTP 62
12 DO 13 J=1,5 OUTP 63
13 IF(NAME(N,J).EQ.IZ.OR.NAME(N,J).EQ.IB) GO TO 14 OUTP 64
  CONTINUE OUTP 65
  J=6 OUTP 66
14 J=J-1 OUTP 67
  HEAD(3)=YN(J) OUTP 68
  HEAD(7)=YX(J) OUTP 69
  HEAD(9)=F75 OUTP 70
  IF(PECWT(N).GE.10.) HEAD(9)=F73 OUTP 71
  WRITE(6,HEAD)HD1,HD2,(NAME(N,JJ),ANUM(N,JJ),JJ=1,J),PECWT(N),ENTH( OUTP 72
  IN),FAZ(N),RTEMP(N),DENS(N) OUTP 73
15 CONTINUE OUTP 74
  FPC = 100./(1.+OF) OUTP 75
  WRITE(6,20) OF ,FPC,EQRAT,RHOP OUTP 76
20 FORMAT(1H0,15X, 4H0/F=, F8.4,4X,13HPERCENT FUEL=F8.4,4X, OUTP 77
  1 19HEQUIVALENCE RATIO= ,F7.4,4X,17HREACTANT DENSITY=,F8.4//) OUTP 78
  AGV = 9.80665 OUTP 79
  RETURN OUTP 80
  ENTRY OUT2 OUTP 81
  FMT(4) = FMT(6) OUTP 82
  OUTP 83
  OUTP 84
  OUTP 85
  OUTP 86
  OUTP 87
  OUTP 88
  OUTP 89
  OUTP 90
  OUTP 91
  OUTP 92
  OUTP 93
  OUTP 94
  OUTP 95
  OUTP 96
  OUTP 97
  OUTP 98
  OUTP 99
  OUTP 100

```

```

C C C C C
WRITE (6,FMT)(FT(I),I=1,4),(NV(J),J=1,NPT)
C C C C C
DENSITY
DO 70 I=1,NPT
IF(VLM(I).NE.O.) V(I)=1./VLM(I)
70 CONTINUE
CALL EFMT(NPT,FRHO,V)
C C C C C
ENTHALPY
DO 75 I=1,NPT
V(I)=HSUM(I)*R
75 CONTINUE
FMT(5)=FB
IF(R.LT.10.) GO TO 76
CALL EFMT(NPT,FH,V)
FMT(7)=F1
GO TO 77
76 FMT(7)=F1
WRITE (6,FMT)(FH(I),I=1,4),(V(J),J=1,NPT)
C C C C C
ENTROPY
FMT(7)=F4
77 DO 78 I=1,NPT
V(I)=SSUM(I)*R
78 CONTINUE
WRITE (6,FMT)(FS(I),I=1,4),(V(J),J=1,NPT)
WRITE (6,80)
80 FORMAT ( ' 1H ' )
C C C C C
MOLECULAR WEIGHT
FMT(7)=F3
WRITE (6,FMT)(FM(I),I=1,4),(WM(J),J=1,NPT)
(DLV/DLPT)
C C C C C
FMT(7)=F5
IF(EQL) WRITE(6,FMT)(FV(I),I=1,4),(DLVPT(J),J=1,NPT)
(DLV/DLTP)
C C C C C
FMT(7)=F4
IF(EQL) WRITE(6,FMT)(FD(I),I=1,4),(DLVTP(J),J=1,NPT)
HEAT CAPACITY
IF(R.GT.10.) FMT(7)=F1
C C C C C

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```

DO 85 I=1,NPT
  V(I) = CPR(I) * R
85 CONTINUE
  WRITE(6,FMT)(FC(I),I=1,4),(V(J),J=1,NPT)
C
C
C GAMMA(S)
C
  FMT(7) = F4
  WRITE(6,FMT)(FG(I),I=1,4),(GAMMAS(J),J=1,NPT)
C
C SONIC VELOCITY
C
  FMT(7) = F1
  DO 95 I = 1,NPT
    SONVEL(I) = (RR*GAMMAS(I)*TTT(I)/WM(I))**.5
95 CONTINUE
  WRITE(6,FMT)(FL(I),I=1,4),(SONVEL(J),J=1,NPT)
  RETURN
C
C ENTRY OUT3
C
  TRA = 5.E-6
  IF(TRACE.NE.0.) TRA= TRACE
  IF(.NOT.EQL) GO TO 331
C
C MOLE FRACTIONS - EQUILIBRIUM
C
  WRITE(6,80)
  FMT(7) = F5
  WRITE(6,310)
310 FORMAT(15HMOLE FRACTIONS //)
  DO 330 K=1,NS
  DO 315 I=1,NPT
    V(I) = EN(K,I)/TOTN(I)
315 CONTINUE
  DO 316 I=1,NPT
    IF(TRACE.EQ.0.) GO TO 317
    IF(V(I).GE.TRACE) GO TO 325
317 IF(V(I).GE.(5.E-6)) GO TO 320
316 CONTINUE
  GO TO 330
C 320 WRITE(6,FMT) SUB(K,1),SUB(K,2),SUB(K,3),FB,(V(I),I=1,NPT)
320 CONTINUE
  GO TO 330
325 FSB(1) = SUB(K,1)
  FSB(2) = SUB(K,2)
  FSB(3) = SUB(K,3)
  CALL EFM(T,NPT,FSB,V)
330 CONTINUE
C 331 WRITE(6,335) TRA

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```

OUTP 151
OUTP 152
OUTP 153
OUTP/154
OUTP 155
OUTP 156
OUTP 157
OUTP 158
OUTP/159
OUTP 160
OUTP 161
OUTP 162
OUTP 163
OUTP 164
OUTP 165
OUTP 166
OUTP/167
OUTP 168
OUTP 169
OUTP 170
OUTP 171
OUTP 172
OUTP 173
OUTP 174
OUTP 175
OUTP 176
OUTP 177
OUTP/178
OUTP 179
OUTP/180
OUTP 181
OUTP 182
OUTP 183
OUTP 184
OUTP 185
OUTP 186
OUTP 187
OUTP 188
OUTP 189
OUTP 190
OUTP 191
OUTP/192
OUTP/192
OUTP 193
OUTP 194
OUTP 195
OUTP 196
OUTP 197
OUTP/198
OUTP 199

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331 CONTINUE
335 FORMAT(83H0ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOL
2/ )
1E FRACTIONS WERE LESS THAN ,E12.5,28H FOR ALL ASSIGNED CONDITIONS/
LINE= 0
NN = 1
IF(EQL) NN=NPT
DO 350 K=1,NS
DO 340 I=1,NN
IF((EN(K,I)/TOTN(I)).GE.TRA) GO TO 343
340 CONTINUE
LINE= LINE+1
Z(LINE,1)= SUB(K,1)
Z(LINE,2)= SUB(K,2)
Z(LINE,3)= SUB(K,3)
343 IF ((LINE.NE.10) .AND. K.NE.NS) GO TO 350
IF (LINE.EQ.0) GO TO 1000
WRITE(6,345) (Z(LN,1),Z(LN,2),Z(LN,3),LN=1,LINE)
C 345 FORMAT (10(1X,3A4))
LINE= 0
350 CONTINUE
C IF(.NOT. MOLES) WRITE(6,360)
360 FORMAT(78HNOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXI
1000 2DANT IN TOTAL OXIDANTS
RETURN
END

```

```

OUTPA199
OUTP 200
OUTP 201
OUTP 202
OUTP 203
OUTP 204
OUTP 205
OUTP 206
OUTP 207
OUTP 208
OUTP 209
OUTP 210
OUTP 211
OUTP 212
OUTP 213
OUTP 214
OUTP 215
OUTP 216
OUTP 217
OUTP 218
OUTP 219
OUTP 220
OUTP 221
OUTP 222
OUTP 223
OUTP 224

```

```

C
C
C
SUBROUTINE VARFMT(V,NPT)
  DIMENSION V(13)
  COMMON/OUPT/FMT(30),FP(4),FI(4),FH(4),FS(4),FM(4),FV(4),FD(4)
  1 ,FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMT19,FA1,FA2
  2 ,FR1,FC1,FN(4),FR(4),FA(4),FI(4),FI(4),FMT9X,F0
C
  DO 45 I=1,NPT
    K=2*I+3
    FMT(K)=F4
    IF (V(I).GE.10.) FMT(K)=F3
    IF (V(I).GE.100.) FMT(K)=F2
    IF (V(I).GE.1000.) FMT(K)=F1
    IF (V(I).GE.100000.) FMT(K)=F0
  45 CONTINUE
  RETURN
END

```

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VRFT
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VRFT

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C	1	SUBROUTINE EFMT(NPT,AA,V)	EFMT
C	2	DIMENSION AA(3), V(13), W(13), NE(13), FRMT(7)	EFMT
C	3	COMMON/OUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4)	EFMT
C	4	1,FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMT19,FA1,FA2	EFMT
C	5	2,FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,FO	EFMT
C	6	DATA FRMT/3H(1H,4H,3A4,4H,11X,4H,13(,4HF7.4,4H,I2),1H)/,F63/4HF6.3	EFMT
C	7	1/,FI3/4H,I3)/,F74/4HF7.4/,FI2/4H,I2)/,F11X/4H,11X/,F2X/3H,2X/	EFMT
	8	FRMT(5) = F74	EFMT
	9	FRMT(6) = FI2	EFMT
	10	J1 = 1	EFMT
	11	FRMT(3) = F2X	EFMT
	12	IF(FMT(4).NE.FMT9X) GO TO 130	EFMT
	13	J1 = 2	EFMT
	14	FRMT(3) = F11X	EFMT
	15	DO 145 I=J1,NPT	EFMT
	16	IF(V(I).NE.O.) GO TO 140	EFMT
	17	W(I) = 0.	EFMT
	18	NE(I) = 0.	EFMT
	19	GO TO 145	EFMT
	20	EE = ALOG10(ABS(V(I)))	EFMT
	21	NE(I) = EE	EFMT
	22	FE = NE(I)	EFMT
	23	IF(EE.LE.O..AND.FE.NE.EE) NE(I)=NE(I)-1	EFMT
	24	IF(IABS(NE(I)).LT.10) GO TO 144	EFMT
	25	FRMT(5) = F63	EFMT
	26	FRMT(6) = FI3	EFMT
	27	W(I) = V(I)/10.**NE(I)	EFMT
	28	144 CONTINUE	EFMT
	29	145 WRITE(6,FRMT) (AA(I),I=1,3),(W(J), NE(J),J=J1,NPT)	EFMT
C	30	RETURN	EFMT
	31	1000 END	EFMT



```

SUBROUTINE THERMP
C THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR
C IBM 360 MACHINES ONLY
C
C DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS
C DOUBLE PRECISION COEF,S,EN,ENLN,H0,DELN
C
C LOGICAL HP,SP,TP,UV,SV,NEW, IONS,MOLES,FROZ,EQL,PSIA,RKT,VOL,TV
C 1,CALCH
C
C DIMENSION VL(26)
C
C COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
C 1,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)
C 2,VLM(13),TOTN(13)
C COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),HO(150)
C 1,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2),SLN(150)
C COMMON/MISC/ENN,SUMN,IT,SO,ATOM(3,101),LLMT(15),BO(15),BOP(15,2)
C 1,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPC,T,R,RR,HSUBO,AC(2),AM(2)
C 2,HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
C 3,ANUM(15,5),PECHT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
C 4,RHOP,RMW(15),TLN,CR,OXF(15),ENNL,ENSAVE,ENLSAV,TRACE
C COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM
C 1,IONS,KMAT,IMAT,IQI,NOF,NOMIT,IP,NEW,NSUB,NSUP,ITM,CPCVFR,CPCVEQ
C 2,ISAVE,LSAVE,ISUP,ISUB,ITNUM
C 3,IQSAVE,LSQ,JSOL,JLIQ,KASE,NREAC,IC,JSI,VOL,SHOCK,IT,NFZ,CALCH
C COMMON/OUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4)
C 1,FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMTI9,FA1,FA2
C 2,FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,FO
C
C EQUIVALENCE (K,ISV),(VL,P),(UV,HP),(TP,TV),(SP,SV)
C
C DATA FUU/4HU,C/
C
C IF(T(1).EQ.0.) T(1) = 3800.
C
C ICF = 0
C ICF = ICF+1
C OF = OXF(ICF)
C CALL NEWOF
C IF(TT.EQ.0..AND.CALCH) RETURN
C
C SET ASSIGNED P OR VOLUME
C
C DO 903 IP=1,NP
C PP = P(IP)
C VLM(NPT) = VL(IP)
C
C SET ASSIGNED T

```



```

      IF (NT.EQ.1.AND.NP.EQ.1) GO TO 95
      IF (IP.EQ.1.AND.IT.EQ.1) ISV=-ISV
      IF (NT.EQ.1) GO TO 871
      IF (IT.EQ.NT.OR.IT.EQ.0.) ISV=0
      CALL SAVE
      871 CONTINUE
      902 CONTINUE
      903 CONTINUE
      1000 GC TO 95
      RETURN
      END

```

```

THRP 101
THRP 102
THRP 103
THRP 104
THRP 105
THRP 106
THRP 107
THRP 108
THRP 109
THRP 110

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```

      PP = P(IP)
      IPP = 1
      LOOP FOR PRESSURE RATIOS
331  IF(EQL) GO TO 332
      CALL FROZEN
      GO TO 1332
332  CALL EQLBRM
      TT = 0 IF NO CONVERGENCE
1332 IF(TT.NE.0.) GO TO 333
      IF(NPT.LT.1) GO TO 1000
      GO TO 900
333  IF(IPP.GT.1) GO TO 195
      COMBUSTION CHAMBER
      EQL = SEQL
      TP = .FALSE.
      HP = .FALSE.
      SP = .TRUE.
      SO = SSUM(1)
      CPRF = CPSUM
      TMELT = 0.
      ITROT = 3
      THI = .FALSE.
      APP(2) = ((GAMMAS(1)+1.)/2.)*(GAMMAS(1)/(GAMMAS(1)-1.))
      PP = PPP(1)/APP(2)
      TT = 2.*TT/(GAMMAS(1)+1.)
      ISV = 1
      GO TO 870
195  USQ = 2.*(HSUM(1)-HSUM(NPT)) * RR
      IF (IPP.GT.2) GO TO 900
      THROAT
190  IF(.NOT.TH1) GO TO 191
      GAMMAS(2) = 0.
      GO TO 899
191  ASQ = GAMMAS(2)*TT*ENN*RR
      IF(EQL) WRITE(6,194) APP(2),TT
194  FORMAT (7H PC/PT= F9.6, 6H T = F9.2)
      IF(IDEBUG.EQ.1.OR.1DEBUG.EQ.2) WRITE(6,923)USQ,ASQ
923  FORMAT(5H USQ=,E15.8,5X,4HASQ=,E15.8)
      DH = (USQ-ASQ)/ASQ
      IF(DH.LT.0.) DH=-DH
      IF(DH.LE.0.4E-4.OR.ITROT.EQ.0) GO TO 899
      IF(JSOL.NE.0) GO TO 925

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ROCK 81
ROCK 82
ROCK 83
ROCK 84
ROCK 85
ROCK 86
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ROCK 121
ROCK 122
ROCK 123
ROCK 124
ROCK 125
ROCK 126
ROCK 127
ROCK 128
ROCK 129
ROCK 130

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      IF (TMELT.EQ.0.) GO TO 192
      DLT = ALOG(TMELT/TT)
      DO = DLT*CPR(2)/(ENN*DLVTP(2))
      PP = PP*EXP(DO)
      APP(2) = P(IP)/PP
      TH1 = .TRUE.
      GO TO 331
925  TMELT = TT
192  APP(2) = APP(2)/(1.+(USQ-ASQ)/(ENN*TT*RR*(GAMMAS(2)+1.)))
193  PP = P(IP)/APP(2)
      ITROT = ITROT-1
      GO TO 331
899  AWT = ENN*TT/(PP*USQ**.5)
      PCPLT = ALOG(APP(2))

C
C
900  ISV = 0
      AEAT(NPT) = ENN*TTT(NPT)/(PP*USQ**.5*AWT)
      IF (TT.EQ.0.) GO TO 860
      IF (AREA) GO TO 800
      IF (IPP.LT.NPP) GO TO 859
      IF (NSUB.EQ.0.AND.NSUP.EQ.0) GO TO 860
      AREA = .TRUE.

      PCP ESTIMATES FOR AREA RATIOS

C
C
      IF (ITNUM.NE.0) GO TO 810
      DLNP = 1.
      ITNUM = 1.
      ARATIO = SUBAR(ISUB)
      IF (NSUB.LE.0) ARATIO = SUPAR(ISUP)
      ELN = ALOG(ARATIO)
      IF (NSUB.LE.0) GO TO 799
      APPL = PCPLT/(SUBAR(ISUB)+(10.587*ELN**2+9.454)*ELN)
      IF (ARATIO.LT.1.09) APPL = .9*APPL
      IF (ARATIO.GT.10.) APPL = APPL/ARATIO
      GO TO 859
799  IF (SUPAR(ISUP).LT.2.) GO TO 805
      IF (ISUP.GT.1.AND.SUPAR(ISUP-1).GE.2.) GO TO 802
      APPL = GAMMAS(2)+ELN*1.4
      GO TO 859
805  APPL = SQRT(ELN*(1.535+3.294*ELN))+PCPLT
      GO TO 859

C
C
      TEST FOR CONVERGENCE ON AREA RATIO.

C
C
810  CHECK = .00004
      IF (IDEBUG.LE.0.OR.NPT.LT.IDEBUG) GO TO 809
      WRITE(6,181) ITNUM,ARATIO,AEAT(NPT),APP(NPT),DLNP
1811  FORMAT(6HO1TER=,I2,5X,15HASSIGNED AE/AT=,F15.8,5X,6HAE/AT=,F15.8,ROCK 131
      ROCK 132
      ROCK 133
      ROCK 134
      ROCK 135
      ROCK 136
      ROCK 137
      ROCK 138
      ROCK 139
      ROCK 140
      ROCK 141
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      ROCK 176
      ROCK 177
      ROCK 178

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15X,5HPC/P=F15.8,5X,13HDELTA LN PCP=,F15.8)
809 IF(ABS(AEAT(NPT))-ARATIO)/ARATIO .LE.CHECK) GO TO 830
DELTAE = (AEAT(NPT)-ARATIO)/ARATIO
IF(ABS(DLNP).LT.00004) GO TO 830
AEATL= ALOG(AEAT(NPT))
ITNUM = ITNUM+1
IF(ITNUM.GT.10) GO TO 840
C
C IMPROVED PCP ESTIMATES.
C
ASQ = GAMMAS(NPT)*ENN*RR*TT
DLNPE = GAMMAS(NPT)*USQ/(USQ-ASQ)
DLNP = DLNPE*ELN-DLNPE*AEATL
APPL = APPL+DLNP
IF(ITNUM.EQ.1) GO TO 859
IF (APPL.LT.0.) APPL = .000001
PP = P(IP)/APP(NPT)
GO TO 331
C
830 ITNUM = 0
AEAT(NPT) = ARATIO
IF(NSUB.LE.0) GO TO 834
ISUB = ISUB+1
IF(ISUB.LE.NSUB) GO TO 800
ISUB = 1
NSUB = -NSUB
IF(ISUP.LE.NSUP) GO TO 800
GO TO 835
834 ISUP = ISUP+1
IF(ISUP.LE.NSUP) GO TO 800
ISUP = 1
AREA = .FALSE.
GO TO 860
840 WRITE(6,841) ARATIO
841 FORMAT(34HODID NOT CONVERGE FOR AREA RATIO =,F10.5)
GO TO 830
C
C TEST FOR OUTPUT -- END OF PCP,SUBAR,AND SUPAR SCHEDULES OR NPT=13.
C
ISV = NPT
859 IF(NPT.NE.13) GO TO 870
860 IF(EQL) GO TO 861
CPR(1) = CPRF
GAMMAS(1) = CPRF/(CPRF-1./WM(1))
CALL RKTOUT
861 IF(IT.EQ.0.) AREA=.FALSE.
IF(.NOT.EQL.AND.TT.EQ.0.) WRITE(6,862)
862 FORMAT(105HOCALCULATIONS WERE STOPPED BECAUSE NEXT POINT IS MORE THAN 50 DEG BELOW TEMP RANGE OF A CONDENSED SPECIES)

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ROCK 179  
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 ROCK 226  
 ROCK 227



IF (ISV.EQ.0) GO TO 990	ROCK 228
IDEBUG = IDEBUG-13	ROCK 229
IF(EQL) WRITE(6,865)	ROCK/230
FORMAT(1H1)	ROCK 231
NPT = 2	ROCK 232
SET INDICES AND ESTIMATES FOR NEXT POINT.	ROCK 233
	ROCK 234
870 NPT = NPT + 1	ROCK 235
IF(.NOT.EQL.AND.(ISV.NE.1.OR.SEQL)) GO TO 880	ROCK 236
IF(ISV.EQ.1) ISV = -1	ROCK 237
CALL SAVE	ROCK 238
880 IPP = IPP+1	ROCK 239
IF(NPT.EQ.2) GO TO 331	ROCK 240
IF(.NOT.AREA) APP(NPT)=PCP(IPP-2)	ROCK 241
IF(AREA) APP(NPT)=EXP(APPL)	ROCK 242
PP = P(IPP)/APP(NPT)	ROCK 243
GO TO 331	ROCK 244
END OF PCP, SUBAR, AND SUPAR SCHEDULES.	ROCK 245
	ROCK 246
990 IF(IDEBUG.LT.0) IDEBUG=IDEBUG+13	ROCK 247
IF(NSUB.LT.0) NSUB=-NSUB	ROCK 248
IF (.NOT.FROZ.OR..NOT.EQL) GO TO 997	ROCK 249
SET UP FOR FROZEN.	ROCK 250
	ROCK 251
TT = TTT(1)	ROCK 252
IPP = 1	ROCK 253
NPT = 1	ROCK 254
ITROT = 3	ROCK 255
CALL SAVE	ROCK 256
EQL = .FALSE.	ROCK 257
ENN = 1./WM(1)	ROCK 258
ITNUM = 0	ROCK 259
ISUB = 1	ROCK 260
ISUP = 1	ROCK 261
GO TO 334	
997 NPT = 1	ROCK 262
ARE THERE MORE ASSIGNED,	ROCK 263
1) CHAMBER PRESSURES(IP = NP)	ROCK 264
2) CHAMBER TEMPERATURES(IT = NT)	ROCK 265
3) O/F VALUES(IOF = NOF)	ROCK 266
IF(IP.EQ.NP.AND.IT.EQ.NT.AND.IOF.EQ.NOF) GO TO 1000	ROCK 267
WRITE(6,865)	ROCK 268
CALL SAVE	ROCK 269
TT = TTT(1)	ROCK/270
998 CONTINUE	ROCK 271
	ROCK 272
	ROCK 273
	ROCK 274

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IF(IT.GE.NT) GO TO 999
IT = IT+1
TT = T(IT)
GO TO 322
999 IF (IOF.GE.NOF) GO TO 1000
GO TO 321
RETURN
1000 END

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ROCK 275
ROCK 276
ROCK 277
ROCK 278
ROCK 279
ROCK 280
ROCK 281
ROCK 282

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C SUBROUTINE RKTOU
C
C ROCKET PERFORMANCE PARAMETERS
C
C THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR
C IBM 360 MACHINES ONLY
C
C DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS
C DOUBLE PRECISION COEF,S,EN,ENLN,HO,DELN
C
C LOGICAL EQL,FROZ ,TP,HP,SP,SHOCK,AREA
C
C DIMENSION NV(13),Z(10,4)
C
C COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
1 GAMMAS(13),P(26),T(26),V(13),PPP(13),SONVEL(13),TTT(13)
2 VLM(13),TOTN(13)
C COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),HO(150)
1 DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2),SLN(150)
C COMMON/MISC/ENNSUMN,TT,SO,ATOM(13,101),LLMT(15),BO(15),BOP(15,2)
1 TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EORAT,FPCT,R,RR,HSUBO,AC(2),AM(2)
2 HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
3 ANUM(15,5),PECHT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4 RHOP,RMW(15),TLN,CR,OXF(15),ENNL,ENSAVE,ENLSAV,TRACE
C COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM
1 TONS,KMAT,IMAT,IQI,NOF,NOMIT,IP,NEWNR,NSUB,NSUP,ITM,CPCVFR,CPCVEQ
2 IQSAVE,LSAVE,PCP(22),JMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13)
3 APP(13),AEAT(13),CSTR,EQL,FROZ,SSO,AREA,AMT
C COMMON/OUPT/FPMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4)
1 FC(4),FG(4),FB,FM13,F1,F2,F3,F4,F5,FL(4),FMT19,FA1,FA2
2 FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,FO
C COMMON/ZONE/KZONE,PGPSIA,OXFUL(20),LETOU
C COMMON/ACSTAR/CSTAR(13)
C
C EQUIVALENCE (V,NV),(Z,HO)
C
C DATA EXIT/4HEXIT/
C
C IF(.NOT.EQL) GO TO 636
C WRITE(6,37)
37 FORMAT(1H1/24X,84HTHEORETICAL ROCKET PERFORMANCE ASSUMING EQUILIBR
1 IUM COMPOSITION DURING EXPANSION
GO TO 39
C
636 WRITE(6,38)
636 CONTINUE
38 FORMAT(1H1,26X,78HTHEORETICAL ROCKET PERFORMANCE ASSUMING FROZEN CROU
1 COMPOSITION DURING EXPANSION
IF(NFZ.GT.1) WRITE(6,637)NFZ

```

Line	Code	Statement	Column
637		FORMAT(58X,11HAFTER POINT,12)	48
39		IF(TTT(1).EQ.I(IT)) WRITE(6,737)	49
737		FORMAT(52X,28HAT AN ASSIGNED TEMPERATURE )	50
		TEM = PPP(1)*14.696006	51
		WRITE(6,40) TEM	52
40		FORMAT(5SHOPC = ,F8.1,5H PSIA)	53
		CALL OUT1	54
		NEX = NPT - 2	55
862		DO 862 I = 1,NEX	56
		V(I) = EXIT	57
48		WRITE(6,48) (V(I),I=1,NEX)	58
		FORMAT(1H0,16X,16HCHAMBER THROAT ,11(5X,A4))	59
		PRESSURE RATIOS	60
		FMT(4) = FMT(6)	61
		CALL VARFMT (APP,NPT)	62
		WRITE(6,FMT) FRI,FB,FB,(APP(J),J=1,NPT)	63
		CALL OUT2	64
		AGV = 9.80665	65
		DO 202 K=2,NPT	66
		SPIM(K) = (2.*RR*(HSUM(1)-HSUM(K))**.5/AGV	67
		AW (A/W) IN UNITS OF SEC/ATM	68
		AW = RR*TTT(K)/(PPP(K)*	69
		IF(K.NE.2)GO TO 200	70
		CSTR = 32.174*PPP(1)*AW	71
		AEAT(2) = 1.	72
200		VACI(K)=SPIM(K)+PPP(K)*AW	73
		IF (SONVEL(K).NE.O.) VMOC(K)=SPIM(K)*AGV/SONVEL(K)	74
202		NV(K)= CSTR + .5	75
		CONTINUE	76
		MACH NUMBER	77
		VMOC(1)=0.	78
		IF(GAMMAS(2).EQ.O.) VMOC(2)=0.	79
		FMT(7) = F3	80
		WRITE(6,FMT)(FN(I),I=1,4),(VMOC(J),J=1,NPT)	81
		WRITE(6,208)	82
208		FORMAT (1H )	83
		CALL LOAD1(NPT)	84
		AREA RATIO	85
		FMT(4) = FMT9X	86
		CALL VARFMT (AEAT,NPT)	87
		FMT(5) = FB	88

```

C      WRITE(6,FMT)FA1,FA2,FB,FB,(AEAT(J),J=2,NPT)
C
C*
C      FMT(5) = FMT13
C      FMT(6) = FMT19
C      FMT(7) = FB
C      WRITE(6,FMT)(FR(I),I=1,4),(NV(J),J=2,NPT)
C      DO 1 I=2,NPT
C      1 CSTAR(I)=NV(I)
C
C      CF - THRUST COEFFICIENT
C
C      FMT(6) = FMT(8)
C      FMT(7) = F3
C      DO 212 I=2,NPT
C      212 V(I)=32.174*SPIM(I)/CSTR
C      WRITE(6,FMT)FC1,FB,FB,(V(J),J=2,NPT)
C
C      VACUUM IMPULSE
C
C      FMT(5) = FMT13
C      FMT(7) = F1
C      WRITE(6,FMT)(FA(I),I=1,4),(VACI(J),J=2,NPT)
C
C      SPECIFIC IMPULSE
C
C      WRITE(6,FMT)(FI(I),I=1,4),(SPIM(J),J=2,NPT)
C      CALL LCAD2(NPT)
C      WRITE(6,208)
C      FMT(4) = FB
C      FMT(5) = FMT13
C      FMT(7) = F5
C      IF(EQL) GO TO 312
C      WRITE(6,310)
C      310 FORMAT(15HMOLE FRACTIONS //)
C
C      MOLE FRACTIONS - FROZEN
C
C      TRA = 5.E-6
C      IF(TRACE.NE.0.) TRA=TRACE
C      LINE = 0
C      DO 430 K = 1,NS
C      V(LINE+1) = EN(K,NFZ)/TOTN(NFZ)
C      IF(V(LINE+1).LT.1RA) GO TO 424
C      LINE = LINE+1
C      Z(LINE,1) = SUB(K,1)
C      Z(LINE,2) = SUB(K,2)
C      Z(LINE,3) = SUB(K,3)
C      Z(LINE,4) = V(LINE)

```

```

ROUT/ 97
ROUT 98
ROUT 99
ROUT 100
ROUT 101
ROUT 102
ROUT 103
ROUT/104
ROUTA104
ROUTB104
ROUT 105
ROUT 106
ROUT 107
ROUT 108
ROUT 109
ROUT 110
ROUT 111
ROUT/112
ROUT 113
ROUT 114
ROUT 115
ROUT 116
ROUT 117
ROUT/118
ROUT 119
ROUT 120
ROUT 121
ROUT/122
ROUTA122
ROUT/123
ROUT 124
ROUT 125
ROUT 126
ROUT 127
ROUT/128
ROUT 129
ROUT 130
ROUT 131
ROUT 132
ROUT 133
ROUT 134
ROUT 135
ROUT 136
ROUT 137
ROUT 138
ROUT 139
ROUT 140
ROUT 141
ROUT 142
ROUT 143

```

```

ROUT 144
ROUT 145
ROUT/146
ROUT 147
ROUT 148
ROUT 149
ROUT 150
ROUT 151
ROUT 152

```

```

424 IF (LINE.NE.4.AND.K.NE.NS) GO TO 430
    IF (LINE.EQ.0) GO TO 312
    WRITE(6,426) (Z(LN,1),Z(LN,2),Z(LN,3),Z(LN,4),LN=1,LINE)
    FORMAT(1H,4(3A4,F9.5,7X))
    LINE = 0
430 CONTINUE
312 CALL OUT3
1000 RETURN
END

```

C

```

SUBROUTINE FROZEN
  (FROZEN COMPOSITION EXPANSION ONLY)
  THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR
  IBM 360 MACHINES ONLY
  DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS
  DOUBLE PRECISION COEF,S,EN,ENLN,H0,DELN
  DOUBLE PRECISION SUMS,SUMH,SS
  LOGICAL EQL,FROZ,CONVG,SP,HP,VOL
  COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
  1 ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)
  2 ,VLM(13),TOTN(13)
  1 COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)
  1 DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2),SLN(150)
  1 COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),BO(15),BOP(15,2)
  1 TM,TLOW,TMID,HIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AC(2),AM(2)
  2 ,HPP(2),RHO(2),VMIN(2),VPLS(2),WPI(2),DATA(22),NAME(15,5)
  3 ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
  4 COMMON/INDX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NPT,NLM
  1 ,NS,KMAT,IMAT,IQI,NOF,NOMIT,IP,NEWIR,NSUB,NSUP,ITM,CPCVFR,CPCVEQ
  2 ,IQSAVE,LSAVE,ISUP,ISUB,ITNUM
  3 COMMON/PERF/PCP(22),VMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13)
  1 ,APP(13),AEAT(13),CSTR,EQL,FROZ,SS0,AREA,AWT
  1 COMMON/OUPT/FMT(30),FP(4),FH(4),FS(4),FM(4),FV(4),FD(4)
  1 ,FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMT19,FA1,FA2
  2 ,FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,F0
  CONVG = .FALSE.
  TLN = ALOG(TT)
  DO 51 ITER=1,8
  SUMS = 0.
  SUMH = 0.
  JSI = ITM
  NPT = NPT
  CALL CPHS
  CC = CPSUM
  55 NPT = NNN
  DO 60 J=ITM,NS
  IF (EN(J,NFZ).EQ.0.) GO TO 60
  SS = S(J)
  PMN = PP*WM(NFZ)*EN(J,NFZ)
  IF(IUSE(J).EQ.0) SS=SS-ALOG(PMN)
  SUMS = SUMS+SS*EN(J,NFZ)
  IF (CONVG)
    SUMH=SUMH+H0(J)*EN(J,NFZ)

```

```

60 CONTINUE
   IF (CONVG) GO TO 81
   DLNT=(SUMS-SO)/CC
   TLN=TLN-DLNT
   IF(DLNT.LT.0.) DLNT=-DLNT
   IF(DLNT.LT.0.5E-4) CONVG=.TRUE.
   IT = EXP(TLN)
51 CONTINUE
   WRITE(6,70)
70 FORMAT(40HOFROZEN DID NOT CONVERGE IN 8 ITERATIONS)
   GO TO 903
81 TT(NPT)=TT
   SSUM(NPT)=SUMS
   HSUM(NPT)=TT*SUMH
   GAMMAS(NPT)= CPSUM/(CPSUM-1./WM(NFZ))
   VLM(NPT) = RR*TT/(WM(NFZ)*101.325*PP)
   WM(NPT) = WM(NFZ)
   DLVPT(NPT) = -1.
   DLVTP(NPT) = 1.
   TOTN(NPT) = TOTN(NFZ)
   PPP(NPT) = PP
   CPR(NPT) = CPSUM
   IF (TT.LT.(TLOW-150.))GO TO 903
   IF(NC.EQ.0) GO TO 1000
   INC =0
   DO 901 I=1,M,NS
   IF(IUSE(I).EQ.0.OR.IUSE(I).EQ.-10000) GO TO 901
   INC = INC+1
   IF (INC(I,NFZ).EQ.0.) GO TO 901
   IF(TT.LT.(TEMP(1)-50.)).OR.TT.GT.(TEMP(1)+50.))GO TO 903
901 CONTINUE
   GO TO 1000
903 TT=0.
   NPT=NPT-1
1000 RETURN
      END

```



1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32	33	34	35	36	37	38	39	40	41	42	43	44	45	46	47	48	49	50			
BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK	BLOCK
BLOCK DATA DIMENSION ATEM(3,50) COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),BO(15),BCP(15,2) 1 ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,R,RR,HSUBO,AC(2),AM(2) 2 ,HPP(2),RH(2),VMIN(2),VPLS(2),MPI(2),DATA(22),NAME(15,5) 3 ,ANUM(15,5),PE,CWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15) 4 ,RHOP,RMW(15),TLN,CR,OXF(15),ENNL,ENSAVE,ENLSAV,TRACE CCMOP/OUPT/FMT(30),FP(4),FI(4),FJ(4),FK(4),FL(4),FM(4),FN(4),FO 1 ,FC(4),FG(4),FH(4),FI(4),FJ(4),FK(4),FL(4),FM(4),FN(4),FO 2 ,FR1,FC1,FN(4),FR(4),FA(4),FI(4),FJ(4),FK(4),FL(4),FM(4),FN(4),FO EQUIVALENCE (ATOM(1,52),ATEM) ATOMIC SYMBOLS, WEIGHTS, AND VALENCES DATA ATOM/ A 2MH, 1.00797, 1., B 2HBE, 9.0122, 2., C 2HNE, 14.0067, 0., D 2HNE, 20.183, 0., E 2HAL, 26.9815, 3., F 2HS, 32.064, 4., G 2HK, 39.102, 1., H 2HTI, 47.900, 4., I 2HMN, 54.9380, 2., J 2HNI, 58.710, 3., K 2HGA, 69.720, 4., L 2HSE, 78.960, 1., M 2HRB, 85.47, 7., N 2HTR, 91.220, 2., O 2HPC, 99.000, 3., P 2HPD, 106.400, 4., Q 2HIN, 114.820, 5., DATA ATEM/ R 2HTE, 127.600, 4., S 2HCS, 132.905, 1., T 2HCE, 140.120, 3., U 2HPM, 145.000, 3., V 2HGD, 157.250, 3., W 2HHD, 164.930, 3., X 2HYB, 173.040, 5., Y 2HTA, 180.948, 4., Z 2HOS, 190.200, 3., A 2HAU, 196.967, 2., B 2HPB, 207.190, 0., C 2HAT, 210.000, 5., D 2HRA, 226.000, 5., E 2HPA, 231.000, 5., 2HHE, 4.0026, 0., 2HH, 10.811, 3., 2HNA, 15.9994, -2., 2HNA, 22.9898, 1., 2HSI, 28.086, 4., 2HCL, 35.453, -1., 2HCA, 40.080, 2., 2HV, 50.942, 5., 2HFE, 55.847, 3., 2HCU, 63.540, 2., 2HGE, 72.590, -1., 2HBR, 79.909, 2., 2HSR, 87.620, 2., 2HNB, 92.906, 5., 2HRU, 101.070, 3., 2HAG, 107.870, 1., 2HSN, 118.690, 4., 2HI, 126.904, -1., 2HBA, 137.340, 2., 2HPR, 140.907, 3., 2HSM, 150.350, 3., 2HTB, 158.924, 3., 2HER, 167.260, 3., 2HLU, 174.997, 3., 2HW, 183.850, 6., 2HIR, 192.200, 4., 2HIG, 200.590, 2., 2HBI, 208.980, 3., 2HRN, 222.000, 0., 2HAC, 227.000, 6., 2HU, 238.030, 5., 2HLI, 6.939, 1., 2HCF, 12.0115, 4., 2HMG, 18.9984, -1., 2HHP, 24.312, 5., 2HAR, 30.9738, 0., 2HSC, 39.948, 3., 2HCR, 44.956, 3., 2HCO, 51.996, 2., 2HZN, 58.9332, 2., 2HAR, 65.370, 3., 2HKS, 74.9216, 0., 2HMY, 83.800, 3., 2HMD, 88.905, 6., 2HRM, 95.94, 3., 2HCD, 102.905, 2., 2HSB, 112.400, 3., 2HXB, 121.750, 3., 2HXA, 131.300, 0., 2HND, 138.910, 3., 2HEU, 144.240, 3., 2HDY, 151.960, 3., 2HTM, 162.500, 3., 2HFE, 168.934, 4., 2HRE, 178.490, 7., 2HPT, 185.200, 4., 2HTL, 195.090, 1., 2HPD, 204.370, 2., 2HPO, 210.000, 1., 2HFR, 223.000, 4., 2HTH, 232.038, 5., 2HNP, 237.000, 5., 																																																				

F	2HPU,242.000	, 4.00	2HAM,243.000	, 3.00	2HCM,247.000	, 3.00	BLOK	51
G	2HBK,249.000	, 3.00	2HCF,251.000	, 3.00	2HES,254.000	, 0.00	BLOK	52
H	2HFM,253.000	, 0.00	2HD,2.014102	, 1.00			BLOK	53
							BLOK	54
							BLOK	55

C C C  
 INFORMATION USED IN VARIABLE OUTPUT FORMAT  
 DATA FMT/3H(1H,4H,3A4,4H,A2,,3HF9,,2H0,,3HF9,,2H0,,3HF9,,2H0,,3HF98L0K0056  
 1.,2H0,,3HF9,,2H0,,3HF9,,2H0,,3HF9,,2H0,,3HF9,,2H0,,3HF98L0K0057  
 2.,2H0,,3HF9,,2H0,,3HF9,,2H0,,3HF9,,2H0,,3HF9,,2H0,,3HF98L0K0058  
 31H,,2H0,,2H1,,2H2,,2H3,,2H4,,2H5,,/FMT13/2H13/,FMT13/3H9X/,FMT198L0K0059  
 4/3H19,/  
 DATA  
 1,FT/4HT, D,4HEG K,4H,3A4,4H,3A4,4H,A2,,3HF9,,2H0,,3HF9,,2H0,,3HF9,,2H0,,3HF98L0K0060  
 2,FS/4HS, C,4HAL/(,4HG)(K,2H),2H,/,FM/4HM, M,4HAL/G,2H,2H,/,1H,/,1H,/  
 3,FV/4H(DLV,4H/DLP,4H)T,2H,/,FD/4H(DLV,4H/DLT,2H)P,1H,/,1H,/  
 4,FC/4HCP, 4H(CAL/,4H(G)(,2HK)/,FG/4HGMM,4HA (S,2H),1H,/  
 5,FL/4HSON, 4HVEL,,4HM/SE,2HC/  
 C C C  
 INFORMATION USED IN PERFORMANCE OUTPUT  
 DATA FR1/4HPC/P/, FC1/2HCF/, FN/4HMACH,4H NUM,4HBER,1H,/  
 1,FR/4HCSTA,4HR, F,4HT/SE,2HC,/,FI/4HISP,,4H LB-,4HSEC/,2HLB/  
 2,FA/4HIVAC,4H,LB-,4HSEC/,2HLB,/,FA1/4HAE/A/,FA2/IHT/  
 .END  
 BLOK 61  
 BLOK 62  
 BLOK 63  
 BLOK 64  
 BLOK 65  
 BLOK 66  
 BLOK 67  
 BLOK 68  
 BLOK 69  
 BLOK 70  
 BLOK 71  
 BLOK 72  
 BLOK 73

# APPENDIX F SAMPLE CASES AND SAMPLE INPUTS

## SAMPLE INPUTS:

```

RESERVOIR PRESS. FIXED--1 ZONE--FROZEN--N2H4/N2O4--PRF=30KPSFA,PRO=30KPSFA
LIQUID INJECTION--RC/RT=1.0--CORE O/F=1.5--NCEC71=0
1
&NUM PRMT=0.,1.,.002,.001,0.,1., RT=.1, RCRT=1., EPSC=6., ESPG=.50,
OXFULE=1.5,19*0., PRF=30000.,19*0., PRO=30000.,19*0., AITAC=.0005,
AIPCT=1.,19*0., RHOIFU=1.9488,19*0., TIFU=537.,19*0.,
RHOIOX=2.7787,19*0., TIOX=537.,19*0., CDINJ=.7,19*0.,
MTOTMX=0,MODECH=2,NAORW=1,MGORLI=2,NCHA1=1,NCHA2=0,NCEC71=0, &END
&EQU NCHANG=1, TOG=5400.,19*0.,MWG=21.1,19*0.,GAMG=1.23,19*0., &END
ZONE MASS FLOWS FIXED--2 ZONE--FROZ,FROZ--MDTI(1)=.1,MDTI(2)=.025
GAS INJECTION--RC/RT=.5--STRIATED FLOW--INJ VELOCITIES FIXED--80/20 STRIATION
2
&NUM PRMT=0.,1.,.004,.001,0.,1., RT=.1, RCRT=.5, MDTI=.1,.025,18*0.,
OXFULE=6.,.5,18*0., RIFU=2*24665.,18*0., TIFU=2*537.,18*0.,
WIFU=170.,600.,18*0., RIOX=2*1554.,18*0., TIOX=2*537.,18*0., EPSC=4.,
WIOX=170.,600.,18*0., AGAMGU=1.2092,1.3792,18*0., ATOGU=6089.,1460.,18*0.,
AMWGU=12.969,3.024,18*0., MODECH=1,MGORLI=1,NCHA1=1,NCHA2=1,
MTOTMX=0, NAORW=2, NCEC71=0, &END
&EQU NCHANG=1, TOG=6089.,1460.,18*0., MWG=12.969,3.024,18*0.,
GAMG=1.2092,1.3792,18*0., &END
CHAMBER STATIC PRESS. FIXED--2 ZONE--EQUILIBRIUM--H2/O2 AT 50 PSIA
GAS INJECTION--RC/RT=.5--CORE O/F=6., SHEATH O/F=.5--80/20 STRIATION
2
&NUM PRMT=0.,1.,.008,.001,0.,1.,RT=.2,RCRT=.5,EPSC=4.,PG=7200.,
TIFU=2*537.,18*0.,RIFU=2*24665.,18*0.,TIOX=2*537.,18*0.,
RIOX=2*1554.,18*0.,WIFU=150.,600.,18*0.,WIOX=150.,600.,18*0.,
PCTMO=.8,.2,18*0.,MTOTMX=0,MODECH=3,NAORW=2,MGORLI=1,NCHA1=1,NCHA2=1,
NCEC71=2,OXFULE=6.,.5,18*0., &END
REACTANTS
O 2. 00 100.0 0.0 G298.15 0
H 2. 00 100. 0. G298.15 F
NAMELISTS
REACTANTS
O 2. 00 100.0 0.0 G298.15 0
H 2. 00 100. 0. G298.15 F
NAMELISTS
CHAMBER STATIC PRESS. FIXED--2 ZONE--EQUILIBRIUM--H2/O2 AT 50 PSIA
GAS INJECTION--RC/RT=.5--CORE O/F=6., SHEATH O/F=.5--60/40 STRIATION
71
&NUM PCTMO=.6,.4,18*0., &END

```

## PARAMETERS IN NAMELIST NUM VARIABLES

GNU:

[illegible]

END

CASE 1

RESERVOIR PRESS. FIXED--1 ZONE--FROZEN--N2H4/N2O4--PRF=30KPSFA,PRO=30KPSFA  
LIQUID INJECTION--RC/RT=1.0--CORE O/F=1.5--NCECT1=0

LOOP= 6 RC/RT= 0.100000E 01 MODECH= 2 MGORLI= 2 NAORH= 1 NCECT1= 0  
NSPPG= 0 MTCMA= 0 LETOUT= 1 NINCH= 1

RT= 0.100000E 00 RTCALC= 0.100002E 00 PG= 0.833603E 04 EPSC= 0.600000E 01 CLP= 0.546936E 04

INJECTOR PARAMETERS

ZONE PSI LIMITS =0.0 0.1000E 01

ZONE	PI	TIFU	TIOX	AIFU	AIOX	WIFU	WIOX	RHOIFU	RHOIOX	RIFU	RIOX	MOTIFU	MOTIOX	PRF	PRO
1	0.841055E 04	0.537000E 03	0.942476E-04	0.104196E 03	0.194880E 01	0.0	0.0	0.194880E 01	0.0	0.0	0.0	0.191376E-01	0.300000E 05	0.300000E 05	0.300000E 05
1		0.537000E 03	0.118393E-03	0.872596E 02	0.277870E 01	0.0	0.0	0.277870E 01	0.0	0.0	0.0	0.287064E-01	0.300000E 05	0.300000E 05	0.300000E 05

BURNED GAS PARAMETERS

PG	TOG	CPC	GANG	TG	AG	WG	RHOG	MDTI
0.838534E 04	0.540000E 04	0.126023E 05	0.123000E 01	0.539405E 04	0.188337E 00	0.387364E 03	0.655802E-03	0.478440E-01

THROAT PLANE

R	P	PSI	T	W	M	GAM
0.0	0.546930E 04	0.0	0.498530E 04	0.323300E 04	0.850496E 00	0.123000E 01
0.100000E-02	0.546934E 04	0.988361E-04	0.498530E 04	0.323302E 04	0.850500E 00	0.123000E 01
0.200000E-02	0.546925E 04	0.395343E-03	0.498528E 04	0.323309E 04	0.850520E 00	0.123000E 01
0.300000E-02	0.546905E 04	0.889528E-03	0.498525E 04	0.323321E 04	0.850554E 00	0.123000E 01
0.400000E-02	0.546876E 04	0.148139E-02	0.498520E 04	0.323341E 04	0.850613E 00	0.123000E 01
0.500000E-02	0.546832E 04	0.247095E-02	0.498512E 04	0.323370E 04	0.850695E 00	0.123000E 01
0.599999E-02	0.546773E 04	0.355822E-02	0.498502E 04	0.323400E 04	0.850803E 00	0.123000E 01
0.799999E-02	0.546609E 04	0.632598E-02	0.498474E 04	0.323519E 04	0.851119E 00	0.123000E 01
0.999999E-02	0.546374E 04	0.968494E-02	0.498434E 04	0.323675E 04	0.851563E 00	0.123000E 01
0.120000E-01	0.546064E 04	0.142354E-01	0.498381E 04	0.323800E 04	0.852147E 00	0.123000E 01
0.140000E-01	0.545675E 04	0.193779E-01	0.498314E 04	0.324139E 04	0.852886E 00	0.123000E 01
0.160000E-01	0.545200E 04	0.253130E-01	0.498234E 04	0.324454E 04	0.853785E 00	0.123000E 01
0.180000E-01	0.544637E 04	0.320414E-01	0.498138E 04	0.324827E 04	0.854848E 00	0.123000E 01
0.200000E-01	0.543982E 04	0.395639E-01	0.498025E 04	0.325262E 04	0.856089E 00	0.123000E 01
0.220000E-01	0.543231E 04	0.478814E-01	0.497896E 04	0.325760E 04	0.857511E 00	0.123000E 01
0.240000E-01	0.542381E 04	0.569950E-01	0.497751E 04	0.326323E 04	0.859120E 00	0.123000E 01
0.260000E-01	0.541429E 04	0.669058E-01	0.497587E 04	0.326955E 04	0.860923E 00	0.123000E 01
0.280000E-01	0.540369E 04	0.776150E-01	0.497405E 04	0.327656E 04	0.862929E 00	0.123000E 01
0.300000E-01	0.539200E 04	0.891241E-01	0.497204E 04	0.328430E 04	0.865142E 00	0.123000E 01
0.319999E-01	0.537916E 04	0.101435E 00	0.496982E 04	0.329280E 04	0.867573E 00	0.123000E 01
0.339999E-01	0.536514E 04	0.114548E 00	0.496739E 04	0.330208E 04	0.870226E 00	0.123000E 01
0.359999E-01	0.534989E 04	0.128466E 00	0.496475E 04	0.331213E 04	0.873114E 00	0.123000E 01
0.379999E-01	0.533336E 04	0.143191E 00	0.496188E 04	0.332304E 04	0.876242E 00	0.123000E 01
0.399999E-01	0.531550E 04	0.158723E 00	0.495877E 04	0.333482E 04	0.879624E 00	0.123000E 01
0.419999E-01	0.529625E 04	0.175066E 00	0.495541E 04	0.334749E 04	0.883265E 00	0.123000E 01
0.439999E-01	0.527554E 04	0.192221E 00	0.495178E 04	0.336112E 04	0.887185E 00	0.123000E 01
0.459999E-01	0.525338E 04	0.210189E 00	0.494788E 04	0.337572E 04	0.891391E 00	0.123000E 01
0.479999E-01	0.522961E 04	0.228974E 00	0.494368E 04	0.339134E 04	0.895896E 00	0.123000E 01
0.499999E-01	0.520418E 04	0.248576E 00	0.493918E 04	0.340803E 04	0.900715E 00	0.123000E 01
0.519999E-01	0.517702E 04	0.268998E 00	0.493435E 04	0.342584E 04	0.905866E 00	0.123000E 01
0.539999E-01	0.514804E 04	0.290241E 00	0.492917E 04	0.344488E 04	0.911369E 00	0.123000E 01
0.559999E-01	0.511713E 04	0.312307E 00	0.492363E 04	0.346508E 04	0.917238E 00	0.123000E 01
0.579999E-01	0.508420E 04	0.335197E 00	0.491769E 04	0.348661E 04	0.923495E 00	0.123000E 01
0.599999E-01	0.504913E 04	0.358913E 00	0.491133E 04	0.350952E 04	0.930166E 00	0.123000E 01
0.619999E-01	0.501180E 04	0.383455E 00	0.490452E 04	0.353390E 04	0.937275E 00	0.123000E 01
0.639999E-01	0.497208E 04	0.408023E 00	0.489722E 04	0.355980E 04	0.944849E 00	0.123000E 01
0.659999E-01	0.492982E 04	0.435013E 00	0.488941E 04	0.358738E 04	0.952920E 00	0.123000E 01
0.679999E-01	0.488485E 04	0.462038E 00	0.488104E 04	0.361663E 04	0.961523E 00	0.123000E 01
0.699999E-01	0.483701E 04	0.489802E 00	0.487207E 04	0.364777E 04	0.970695E 00	0.123000E 01
0.719999E-01	0.478611E 04	0.518548E 00	0.486244E 04	0.368088E 04	0.980475E 00	0.123000E 01
0.739999E-01	0.473193E 04	0.548037E 00	0.485210E 04	0.371612E 04	0.990915E 00	0.123000E 01
0.759999E-01	0.467426E 04	0.578328E 00	0.484099E 04	0.375362E 04	0.100206E 01	0.123000E 01
0.779999E-01	0.461284E 04	0.609432E 00	0.482903E 04	0.379355E 04	0.101398E 01	0.123000E 01
0.799999E-01	0.454741E 04	0.641333E 00	0.481614E 04	0.383611E 04	0.102672E 01	0.123000E 01
0.819999E-01	0.447765E 04	0.674031E 00	0.480225E 04	0.388151E 04	0.104037E 01	0.123000E 01
0.839999E-01	0.440326E 04	0.707438E 00	0.478722E 04	0.392998E 04	0.105502E 01	0.123000E 01
0.859999E-01	0.432387E 04	0.741702E 00	0.477096E 04	0.398178E 04	0.107074E 01	0.123000E 01
0.879999E-01	0.423509E 04	0.776656E 00	0.475333E 04	0.403721E 04	0.108766E 01	0.123000E 01
0.899999E-01	0.414850E 04	0.812321E 00	0.473617E 04	0.409657E 04	0.110599E 01	0.123000E 01
0.919999E-01	0.405163E 04	0.848665E 00	0.471330E 04	0.416028E 04	0.112557E 01	0.123000E 01
0.939999E-01	0.394798E 04	0.885650E 00	0.469051E 04	0.422874E 04	0.114687E 01	0.123000E 01
0.959999E-01	0.383699E 04	0.923230E 00	0.466557E 04	0.430243E 04	0.116997E 01	0.123000E 01
0.979999E-01	0.371807E 04	0.961350E 00	0.463818E 04	0.438192E 04	0.119509E 01	0.123000E 01
0.999999E-01	0.359057E 04	0.999942E 00	0.460802E 04	0.446784E 04	0.122251E 01	0.123000E 01
0.101999E 00	0.345382E 04	0.103892E 01	0.457468E 04	0.456090E 04	0.125251E 01	0.123000E 01
THROAT WALL						
0.100002E 00	0.359037E 04	0.100000E 01	0.460796E 04	0.446796E 04	0.122255E 01	0.123000E 01

PERFORMANCE

THROAT ISPVAC,LBF-SEC/LBM CSTAR,FT/SEC  
0.212052E 03 0.550632E 04

THROAT ISPVID,LBF-SEC/LBM CSTID,FT/SEC  
0.211126E 03 0.545208E 04

MO,LBF-SEC/FT MOID,LBF-SEC/FT  
0.478440E-01 0.483202E-01

CD,DISCHARGE COEFFICIENT= 0.990145E 00

THROAT ISPVAC/ISPVID= 0.100438E 01

CSTAR/CSTID= 0.100995E 01

# CASE 2

CHAMBER STATIC PRESS. FIXED--2 ZONE--EQUILIBRIUM--H2/O2 AT 50 PSIA  
GAS INJECTION--RC/RT=.5--CORE O/F=6., SHEATH O/F=.5--80/20 STRIATION

LDOP= 3 RC/RT= 0.500000E 00 MODECH= 3 MGORLI= 1 NAORM= 2 NCECTI= 2  
NSPPC= 0 MTOTAX= 0 LETOUT= 2 MINCH= 2

RT= 0.200000E 00 RTCALC= 0.200000E 00 PG= 0.720000E 04 EPSC= 0.400000E 01 CLP= 0.510585E 04

## INJECTOR PARAMETERS

ZONE PSI LIMITS =0.0 0.8000E 00  
ZONE PSI LIMITS =0.8000 0.1000E 01

ZONE	P1	TIFU TIOX	AIFU AIOX	WIFU WIOX	RHOIFU RHOIX	RIFU RIOX	MDTIFU MDTIOX	PRF PRO
1	0.732444E 04	0.537000E 03	0.164505E 00	0.150000E 03	0.552992E-03	0.246650E 05	0.136455E-01	0.293374E 05
1		0.537000E 03	0.621870E-01	0.150000E 03	0.877706E-02	0.155400E 04	0.818728E-01	0.303067E 05
2	0.732444E 04	0.537000E 03	0.479806E-01	0.600000E 03	0.552992E-03	0.246650E 05	0.159197E-01	0.300841E 05
2		0.537000E 03	0.151149E-02	0.600000E 03	0.877706E-02	0.155400E 04	0.795986E-02	0.421579E 05

## BURNED GAS PARAMETERS.

POG	TOG	CPC	GAMG	TG	AG	WG	RHOG	MDTI
0.727946E 04	0.576760E 04	0.361197E 05	0.112110E 01	0.576076E 04	0.424293E 00	0.702770E 03	0.320337E-03	0.955183E-01
0.735471E 04	0.146013E 04	0.598062E 05	0.137920E 01	0.145162E 04	0.784664E-01	0.100890E 04	0.301643E-03	0.238796E-01



THROAT PLANE

R	P	PSI	T	M	M	GAM
0.0	0.510385E 04	0.0	0.561116E 04	0.388867E 04	0.789643E 00	0.111959E 01
0.400000E-02	0.510568E 04	0.385709E-03	0.561115E 04	0.388885E 04	0.789680E 00	0.111959E 01
0.799999E-02	0.510500E 04	0.154287E-02	0.561109E 04	0.388960E 04	0.789838E 00	0.111958E 01
0.120000E-01	0.510360E 04	0.347169E-02	0.561097E 04	0.389114E 04	0.790162E 00	0.111958E 01
0.160000E-01	0.510140E 04	0.617256E-02	0.561078E 04	0.389357E 04	0.790673E 00	0.111958E 01
0.200000E-01	0.509832E 04	0.964611E-02	0.561018E 04	0.389696E 04	0.791388E 00	0.111958E 01
0.240000E-01	0.509432E 04	0.138932E-01	0.561017E 04	0.390136E 04	0.792312E 00	0.111958E 01
0.320000E-01	0.508345E 04	0.247123E-01	0.560973E 04	0.391334E 04	0.794833E 00	0.111957E 01
0.400000E-01	0.506850E 04	0.386420E-01	0.560794E 04	0.392981E 04	0.798297E 00	0.111956E 01
0.480000E-01	0.504925E 04	0.556973E-01	0.560628E 04	0.395102E 04	0.802759E 00	0.111954E 01
0.560000E-01	0.502343E 04	0.758979E-01	0.560422E 04	0.397725E 04	0.808277E 00	0.111952E 01
0.640000E-01	0.499871E 04	0.992673E-01	0.560175E 04	0.400888E 04	0.814930E 00	0.111950E 01
0.719999E-01	0.496271E 04	0.125833E 00	0.559891E 04	0.404634E 04	0.822810E 00	0.111947E 01
0.799999E-01	0.492291E 04	0.155625E 00	0.559538E 04	0.409018E 04	0.832033E 00	0.111944E 01
0.879998E-01	0.487670E 04	0.188679E 00	0.559139E 04	0.414108E 04	0.842741E 00	0.111941E 01
0.959998E-01	0.482332E 04	0.225033E 00	0.558679E 04	0.419988E 04	0.855110E 00	0.111937E 01
0.104000E 00	0.476136E 04	0.284716E 00	0.558105E 04	0.426557E 04	0.869117E 00	0.111932E 01
0.112000E 00	0.469123E 04	0.307741E 00	0.557417E 04	0.433964E 04	0.885048E 00	0.111926E 01
0.120000E 00	0.461009E 04	0.354127E 00	0.556626E 04	0.442477E 04	0.903354E 00	0.111919E 01
0.128000E 00	0.451668E 04	0.403897E 00	0.555715E 04	0.452274E 04	0.924424E 00	0.111912E 01
0.136000E 00	0.440886E 04	0.457057E 00	0.554644E 04	0.463584E 04	0.948747E 00	0.111903E 01
0.144000E 00	0.428390E 04	0.513594E 00	0.553446E 04	0.476692E 04	0.976935E 00	0.111893E 01
0.151999E 00	0.413899E 04	0.573451E 00	0.551920E 04	0.491905E 04	0.101007E 01	0.111881E 01
0.159999E 00	0.396808E 04	0.636495E 00	0.550089E 04	0.509384E 04	0.104903E 01	0.111875E 01
0.167999E 00	0.376746E 04	0.702514E 00	0.547866E 04	0.530458E 04	0.109511E 01	0.111850E 01
0.175999E 00	0.352957E 04	0.771150E 00	0.545018E 04	0.555840E 04	0.115126E 01	0.111830E 01
0.179999E 00	0.346329E 04	0.788654E 00	0.544225E 04	0.562857E 04	0.116690E 01	0.111824E 01
0.179999E 00	0.339231E 04	0.805683E 00	0.541855E 04	0.571049E 04	0.109924E 01	0.111806E 01
0.180999E 00	0.335338E 04	0.816284E 00	0.538177E 04	0.574985E 04	0.110868E 01	0.111803E 01
0.181499E 00	0.333385E 04	0.821031E 00	0.536921E 04	0.576961E 04	0.111342E 01	0.111803E 01
0.181999E 00	0.331411E 04	0.825777E 00	0.535785E 04	0.578956E 04	0.111821E 01	0.111803E 01
0.182499E 00	0.329417E 04	0.830523E 00	0.534757E 04	0.580972E 04	0.112305E 01	0.111803E 01
0.182999E 00	0.327396E 04	0.835285E 00	0.533855E 04	0.583016E 04	0.112796E 01	0.111803E 01
0.183999E 00	0.322285E 04	0.844825E 00	0.532955E 04	0.587172E 04	0.113793E 01	0.111803E 01
0.184999E 00	0.319068E 04	0.854407E 00	0.532055E 04	0.591436E 04	0.114816E 01	0.111803E 01
0.185999E 00	0.314746E 04	0.864020E 00	0.531124E 04	0.595804E 04	0.115865E 01	0.111803E 01
0.186999E 00	0.310318E 04	0.873661E 00	0.530185E 04	0.600326E 04	0.116975E 01	0.111803E 01
0.187999E 00	0.305780E 04	0.883325E 00	0.529245E 04	0.604989E 04	0.118136E 01	0.111803E 01
0.188999E 00	0.301129E 04	0.893012E 00	0.528305E 04	0.609766E 04	0.119325E 01	0.111803E 01
0.190999E 00	0.291476E 04	0.912438E 00	0.527365E 04	0.614984E 04	0.121794E 01	0.111803E 01
0.192999E 00	0.281336E 04	0.931912E 00	0.526425E 04	0.620234E 04	0.124479E 01	0.111803E 01
0.194999E 00	0.270681E 04	0.951404E 00	0.525485E 04	0.626139E 04	0.127351E 01	0.111803E 01
0.195999E 00	0.259488E 04	0.970879E 00	0.524545E 04	0.632751E 04	0.130472E 01	0.111803E 01
0.200999E 00	0.235391E 04	0.100960E 01	0.523605E 04	0.639351E 04	0.133750E 01	0.111803E 01
0.200000E 00	0.241596E 04	0.100000E 01	0.522665E 04	0.646259E 04	0.137531E 01	0.111803E 01

THROAT WALL

PERFORMANCE

THROAT	ISPVAC,FT/SEC	CSTAR,FT/SEC
	0.927952E 04	0.767759E 04
THROAT	ISPV10,FT/SEC	CSTD,FT/SEC
	0.920196E 04	0.753465E 04
M0,LBF-SEC/FT	M010,LBF-SEC/FT	
0.119398E 00	0.121603E 00	
CO-DISCHARGE	COEFFICIENT=	0.981301E 00
THROAT	ISPVAC/ISPV10=	0.100843E 01
CSTAR/CSTD=	0.101897E 01	

# CASE 3

CHAMBER STATIC PRESS. FIXED--2 ZONE--EQUILIBRIUM--H2/O2 AT 50 PSIA  
GAS INJECTION--RC/RT=.5--CORE O/F=6., SHEATH O/F=.5--60/40 STRIATION

LOOP= 3 RC/RT= 0.500000E 00 MODECH= 3 MGORLI= 1 NAORV= 2 NCECTI= 2  
NSPPG= 0 MTOTMX= 0 LETOUT=71 MINCH= 2

RT= 0.200000E 00 RTCALC= 0.200074E 00 PG= 0.720000E 04 EPSC= 0.400000E 01 CLP= 0.498080E 04

ZONE PSI LIMITS =0.0 0.6000E 00  
ZONE PSI LIMITS =0.6000 0.1000E 01

## INJECTOR PARAMETERS

ZONE	PI	TIFU TIOX	AIFU AIOX	WIFU WIOX	RHOIFU RHOIOX	RIFU RIOX	MDTIFU MDTIOX	PRF PRO
1	0.731038E 04	0.537000E 03	0.124879E 00	0.150000E 03	0.551930E-03	0.246650E 05	0.103387E-01	0.293374E 05
1		0.537000E 03	0.472075E-01	0.150000E 03	0.876020E-02	0.155400E 04	0.620321E-01	0.303067E 05
2	0.731038E 04	0.537000E 03	0.971282E-01	0.600000E 03	0.551930E-03	0.246650E 05	0.321644E-01	0.300841E 05
2		0.537000E 03	0.305975E-02	0.600000E 03	0.876020E-02	0.155400E 04	0.160824E-01	0.421579E 05

## BURNED GAS PARAMETERS

POC	TOC	CPG	GANG	TG	AG	WG	RHOG	MDTI
0.727150E 04	0.576760E 04	0.361197E 05	0.112110E 01	0.576144E 04	0.338855E 00	0.666798E 03	0.320299E-03	0.723708E-01
0.734444E 04	0.146013E 04	0.598062E 05	0.137920E 01	0.145218E 04	0.164059E 00	0.975317E 03	0.301527E-03	0.482472E-01

THROAT PLANE

R	P	PSI	T	M	GAM
0.0	0.498080E 04	0.0	0.50038E 04	0.402641E 04	0.111949E 01
0.400000E-02	0.498083E 04	0.36688E-03	0.50036E 04	0.402660E 04	0.111949E 01
0.799999E-02	0.497991E 04	0.34630E-02	0.50030E 04	0.402739E 04	0.111949E 01
0.120000E-01	0.497844E 04	0.34051E-02	0.50017E 04	0.402901E 04	0.111949E 01
0.150000E-01	0.497613E 04	0.61891E-02	0.50000E 04	0.403155E 04	0.111948E 01
0.200000E-01	0.497250E 04	0.967040E-02	0.50000E 04	0.403511E 04	0.111948E 01
0.250000E-01	0.496871E 04	0.139279E-01	0.50000E 04	0.403912E 04	0.111948E 01
0.300000E-01	0.496473E 04	0.247731E-01	0.50000E 04	0.404328E 04	0.111947E 01
0.350000E-01	0.496059E 04	0.387344E-01	0.50000E 04	0.404759E 04	0.111946E 01
0.400000E-01	0.495625E 04	0.558259E-01	0.50000E 04	0.405228E 04	0.111946E 01
0.450000E-01	0.495175E 04	0.76052E-01	0.50000E 04	0.405717E 04	0.111944E 01
0.500000E-01	0.494713E 04	0.994735E-01	0.50000E 04	0.406228E 04	0.111944E 01
0.550000E-01	0.494238E 04	0.126075E 00	0.50000E 04	0.406759E 04	0.111942E 01
0.600000E-01	0.493753E 04	0.155955E 00	0.50000E 04	0.407303E 04	0.111942E 01
0.650000E-01	0.493258E 04	0.188952E 00	0.50000E 04	0.407854E 04	0.111933E 01
0.700000E-01	0.492753E 04	0.225256E 00	0.50000E 04	0.408413E 04	0.111930E 01
0.750000E-01	0.492238E 04	0.264838E 00	0.50000E 04	0.408980E 04	0.111926E 01
0.800000E-01	0.491713E 04	0.307713E 00	0.50000E 04	0.409554E 04	0.111920E 01
0.850000E-01	0.491178E 04	0.353897E 00	0.50000E 04	0.410133E 04	0.111914E 01
0.900000E-01	0.490633E 04	0.403395E 00	0.50000E 04	0.410717E 04	0.111907E 01
0.950000E-01	0.490078E 04	0.456195E 00	0.50000E 04	0.411306E 04	0.111900E 01
1.000000E-01	0.489513E 04	0.512250E 00	0.50000E 04	0.411891E 01	0.111891E 01
0.110000E 00	0.488938E 04	0.571453E 00	0.50000E 04	0.412475E 01	0.111880E 01
0.120000E 00	0.488353E 04	0.602705E 00	0.50000E 04	0.413058E 01	0.111867E 01
0.130000E 00	0.487768E 04	0.619297E 00	0.50000E 04	0.413641E 01	0.111867E 01
0.140000E 00	0.487183E 04	0.627588E 00	0.50000E 04	0.414224E 01	0.111867E 01
0.150000E 00	0.486598E 04	0.635921E 00	0.50000E 04	0.414807E 01	0.111867E 01
0.160000E 00	0.486013E 04	0.644296E 00	0.50000E 04	0.415390E 01	0.111867E 01
0.170000E 00	0.485428E 04	0.652729E 00	0.50000E 04	0.415973E 01	0.111867E 01
0.180000E 00	0.484843E 04	0.661205E 00	0.50000E 04	0.416556E 01	0.111867E 01
0.190000E 00	0.484258E 04	0.669734E 00	0.50000E 04	0.417139E 01	0.111867E 01
0.200000E 00	0.483673E 04	0.678263E 00	0.50000E 04	0.417722E 01	0.111867E 01
0.210000E 00	0.483088E 04	0.686792E 00	0.50000E 04	0.418305E 01	0.111867E 01
0.220000E 00	0.482503E 04	0.695321E 00	0.50000E 04	0.418888E 01	0.111867E 01
0.230000E 00	0.481918E 04	0.703850E 00	0.50000E 04	0.419471E 01	0.111867E 01
0.240000E 00	0.481333E 04	0.712379E 00	0.50000E 04	0.420054E 01	0.111867E 01
0.250000E 00	0.480748E 04	0.720908E 00	0.50000E 04	0.420637E 01	0.111867E 01
0.260000E 00	0.480163E 04	0.729437E 00	0.50000E 04	0.421220E 01	0.111867E 01
0.270000E 00	0.479578E 04	0.737966E 00	0.50000E 04	0.421803E 01	0.111867E 01
0.280000E 00	0.478993E 04	0.746495E 00	0.50000E 04	0.422386E 01	0.111867E 01
0.290000E 00	0.478408E 04	0.755024E 00	0.50000E 04	0.422969E 01	0.111867E 01
0.300000E 00	0.477823E 04	0.763553E 00	0.50000E 04	0.423552E 01	0.111867E 01
0.310000E 00	0.477238E 04	0.772082E 00	0.50000E 04	0.424135E 01	0.111867E 01
0.320000E 00	0.476653E 04	0.780611E 00	0.50000E 04	0.424718E 01	0.111867E 01
0.330000E 00	0.476068E 04	0.789140E 00	0.50000E 04	0.425301E 01	0.111867E 01
0.340000E 00	0.475483E 04	0.797669E 00	0.50000E 04	0.425884E 01	0.111867E 01
0.350000E 00	0.474898E 04	0.806198E 00	0.50000E 04	0.426467E 01	0.111867E 01
0.360000E 00	0.474313E 04	0.814727E 00	0.50000E 04	0.427050E 01	0.111867E 01
0.370000E 00	0.473728E 04	0.823256E 00	0.50000E 04	0.427633E 01	0.111867E 01
0.380000E 00	0.473143E 04	0.831785E 00	0.50000E 04	0.428216E 01	0.111867E 01
0.390000E 00	0.472558E 04	0.840314E 00	0.50000E 04	0.428799E 01	0.111867E 01
0.400000E 00	0.471973E 04	0.848843E 00	0.50000E 04	0.429382E 01	0.111867E 01
0.410000E 00	0.471388E 04	0.857372E 00	0.50000E 04	0.429965E 01	0.111867E 01
0.420000E 00	0.470803E 04	0.865901E 00	0.50000E 04	0.430548E 01	0.111867E 01
0.430000E 00	0.470218E 04	0.874430E 00	0.50000E 04	0.431131E 01	0.111867E 01
0.440000E 00	0.469633E 04	0.882959E 00	0.50000E 04	0.431714E 01	0.111867E 01
0.450000E 00	0.469048E 04	0.891488E 00	0.50000E 04	0.432297E 01	0.111867E 01
0.460000E 00	0.468463E 04	0.900017E 00	0.50000E 04	0.432880E 01	0.111867E 01
0.470000E 00	0.467878E 04	0.908546E 00	0.50000E 04	0.433463E 01	0.111867E 01
0.480000E 00	0.467293E 04	0.917075E 00	0.50000E 04	0.434046E 01	0.111867E 01
0.490000E 00	0.466708E 04	0.925604E 00	0.50000E 04	0.434629E 01	0.111867E 01
0.500000E 00	0.466123E 04	0.934133E 00	0.50000E 04	0.435212E 01	0.111867E 01
0.510000E 00	0.465538E 04	0.942662E 00	0.50000E 04	0.435795E 01	0.111867E 01
0.520000E 00	0.464953E 04	0.951191E 00	0.50000E 04	0.436378E 01	0.111867E 01
0.530000E 00	0.464368E 04	0.959720E 00	0.50000E 04	0.436961E 01	0.111867E 01
0.540000E 00	0.463783E 04	0.968249E 00	0.50000E 04	0.437544E 01	0.111867E 01
0.550000E 00	0.463198E 04	0.976778E 00	0.50000E 04	0.438127E 01	0.111867E 01
0.560000E 00	0.462613E 04	0.985307E 00	0.50000E 04	0.438710E 01	0.111867E 01
0.570000E 00	0.462028E 04	0.993836E 00	0.50000E 04	0.439293E 01	0.111867E 01
0.580000E 00	0.461443E 04	0.100415E 01	0.50000E 04	0.439876E 01	0.111867E 01
0.590000E 00	0.460858E 04	0.101944E 01	0.50000E 04	0.440459E 01	0.111867E 01
0.600000E 00	0.460273E 04	0.103473E 01	0.50000E 04	0.441042E 01	0.111867E 01
0.610000E 00	0.459688E 04	0.105002E 01	0.50000E 04	0.441625E 01	0.111867E 01
0.620000E 00	0.459103E 04	0.106531E 01	0.50000E 04	0.442208E 01	0.111867E 01
0.630000E 00	0.458518E 04	0.108060E 01	0.50000E 04	0.442791E 01	0.111867E 01
0.640000E 00	0.457933E 04	0.109589E 01	0.50000E 04	0.443374E 01	0.111867E 01
0.650000E 00	0.457348E 04	0.111118E 01	0.50000E 04	0.443957E 01	0.111867E 01
0.660000E 00	0.456763E 04	0.112647E 01	0.50000E 04	0.444540E 01	0.111867E 01
0.670000E 00	0.456178E 04	0.114176E 01	0.50000E 04	0.445123E 01	0.111867E 01
0.680000E 00	0.455593E 04	0.115705E 01	0.50000E 04	0.445706E 01	0.111867E 01
0.690000E 00	0.455008E 04	0.117234E 01	0.50000E 04	0.446289E 01	0.111867E 01
0.700000E 00	0.454423E 04	0.118763E 01	0.50000E 04	0.446872E 01	0.111867E 01
0.710000E 00	0.453838E 04	0.120292E 01	0.50000E 04	0.447455E 01	0.111867E 01
0.720000E 00	0.453253E 04	0.121821E 01	0.50000E 04	0.448038E 01	0.111867E 01
0.730000E 00	0.452668E 04	0.123350E 01	0.50000E 04	0.448621E 01	0.111867E 01
0.740000E 00	0.452083E 04	0.124879E 01	0.50000E 04	0.449204E 01	0.111867E 01
0.750000E 00	0.451498E 04	0.126408E 01	0.50000E 04	0.449787E 01	0.111867E 01
0.760000E 00	0.450913E 04	0.127937E 01	0.50000E 04	0.450370E 01	0.111867E 01
0.770000E 00	0.450328E 04	0.129466E 01	0.50000E 04	0.450953E 01	0.111867E 01
0.780000E 00	0.449743E 04	0.130995E 01	0.50000E 04	0.451536E 01	0.111867E 01
0.790000E 00	0.449158E 04	0.132524E 01	0.50000E 04	0.452119E 01	0.111867E 01
0.800000E 00	0.448573E 04	0.134053E 01	0.50000E 04	0.452702E 01	0.111867E 01
0.810000E 00	0.447988E 04	0.135582E 01	0.50000E 04	0.453285E 01	0.111867E 01
0.820000E 00	0.447403E 04	0.137111E 01	0.50000E 04	0.453868E 01	0.111867E 01
0.830000E 00	0.446818E 04	0.138640E 01	0.50000E 04	0.454451E 01	0.111867E 01
0.840000E 00	0.446233E 04	0.140169E 01	0.50000E 04	0.455034E 01	0.111867E 01
0.850000E 00	0.445648E 04	0.141698E 01	0.50000E 04	0.455617E 01	0.111867E 01
0.860000E 00	0.445063E 04	0.143227E 01	0.50000E 04	0.456200E 01	0.111867E 01
0.870000E 00	0.444478E 04	0.144756E 01	0.50000E 04	0.456783E 01	0.111867E 01
0.880000E 00	0.443893E 04	0.146285E 01	0.50000E 04	0.457366E 01	0.111867E 01
0.890000E 00	0.443308E 04	0.147814E 01	0.50000E 04	0.457949E 01	0.111867E 01
0.900000E 00	0.442723E 04	0.149343E 01	0.50000E 04	0.458532E 01	0.111867E 01
0.910000E 00	0.442138E 04	0.150872E 01	0.50000E 04	0.459115E 01	0.111867E 01
0.920000E 00	0.441553E 04	0.152401E 01	0.50000E 04	0.459698E 01	0.111867E 01
0.930000E 00	0.440968E 04	0.153930E 01	0.50000E 04	0.460281E 01	0.111867E 01
0.940000E 00	0.440383E 04	0.155459E 01	0.50000E 04	0.460864E 01	0.111867E 01
0.950000E 00	0.439798E 04	0.156988E 01	0.50000E 04	0.461447E 01	0.111867E 01
0.960000E 00	0.439213E 04	0.158517E 01	0.50000E 04	0.462030E 01	0.111867E 01
0.970000E 00	0.438628E 04	0.160046E 01	0.50000E 04	0.462613E 01	0.111867E 01
0.980000E 00	0.438043E 04	0.161575E 01	0.50000E 04	0.463196E 01	0.111867E 01
0.990000E 00	0.437458E 04	0.163104E 01	0.50000E 04	0.463779E 01	0.111867E 01
1.000000E 00	0.436873E 04	0.164633E 01	0.50000E 04	0.464362E 01	0.111867E 01
0.010000E 00	0.436288E 04	0.166162E 01	0.50000E 04	0.464945E 01	0.111867E 01
0.020000E 00	0.435703E 04	0.167691E 01	0.50000E 04	0.465528E 01	0.111867E 01
0.030000E 00	0.435118E 04	0.169220E 01	0.50000E 04	0.466111E 01	0.111867E 01
0.040000E 00	0.434533E 04	0.170749E 01	0.50000E 04	0.466694E 01	0.111867E 01

# PERFORMANCE

THROAT	ISP	VAC	FT/SEC	CSTAR	FT/SEC
	0.924010E	04	0.761168E	04	
THROAT	ISP	VID	FT/SEC	CSTID	FT/SEC
	0.917499E	04	0.747335E	04	
MO	LBF-SEC/FT		MO	LBF-SEC/FT	
	0.120618E	00		0.122818E	00
CD	DISCHARGE	COEFFICIENT	=	0.982089E	00
THROAT	ISP	VAC	ISP	VID	
	0.100710E	01			
CSTAR	CSTID	=	0.101824E	01	

CASE 4

ZONE MASS FLOWS FIXED--2 ZONE--FROZ--FROZ--MDTI(1)=1,MDTI(2)=0.025  
GAS INJECTION--RC/RT=0.5--STRIATED FLOW--INJ VELOCITIES FIXED--80/20 STRIATION

ZONE	EST-GANMA	EST-MW	EST-TO
1	0.120920E 01	0.129690E 02	0.608900E 04
2	0.137920E 01	0.302400E 01	0.146000E 04

LOOP= 2 RC/RT= 0.500000E 00 MDDECH= 1 MGORLI= 1 NADRW= 2 NCEC71= 0  
NSPPG= 0 MTOTMX= 0 LETOUT= 2 NINCH= 2

RT= 0.100000E 00 RTCALC= 0.999724E-01 PG= 0.296703E 05 EPSC= 0.400000E 01 CLP= 0.211065E 05

INJECTOR PARAMETERS

ZONE PSI LIMITS =0.0 0.8000E 00  
ZONE PSI LIMITS =0.8000E 000.1000E 01

ZONE	PI	TIFU TIOX	AIFU AIOX	WIFU WIOX	RHOIFU RHOIOX	RIFU RIOX	MDTIFU MDTIOX	PRF PRQ
1	0.302083E 05	0.537000E 03	0.368433E-01	0.170000E 03	0.228071E-02	0.246650E 05	0.142857E-01	0.302754E 05
1		0.537000E 03	0.139283E-01	0.170000E 03	0.361993E-01	0.155400E 04	0.857142E-01	0.312758E 05
2	0.302083E 05	0.537000E 03	0.121794E-01	0.600000E 03	0.228071E-02	0.246650E 05	0.166667E-01	0.310461E 05
2		0.537000E 03	0.383678E-03	0.600000E 03	0.361993E-01	0.155400E 04	0.833333E-02	0.435006E 05

BURNED GAS PARAMETERS

PGC	TOG	CPG	GAMG	TG	AG	WG	RHOG	MDTI
0.300212E 05	0.408900E 04	0.221607E 05	0.120920E 01	0.607663E 04	0.106041E 00	0.740483E 03	0.127354E-02	0.100000E 00
0.303260E 05	0.146000E 04	0.598042E 05	0.137920E 01	0.145125E 04	0.196550E-01	0.102296E 04	0.128339E-02	0.250000E-01

THROAT PLANE

R	P	PSI	T	W	M	GAM
0.0	0.211065E 05	0.0	0.572893E 04	0.399442E 04	0.775152E 00	0.120920E 01
0.200700E-02	0.211058E 05	0.385942E-03	0.572890E 04	0.399499E 04	0.775187E 00	0.120920E 01
0.400300E-02	0.211029E 05	0.154382E-02	0.572877E 04	0.399576E 04	0.775346E 00	0.120920E 01
0.59999E-02	0.210969E 05	0.347385E-02	0.572844E 04	0.399732E 04	0.775659E 00	0.120920E 01
0.799999E-02	0.210874E 05	0.617642E-02	0.572800E 04	0.399980E 04	0.776181E 00	0.120920E 01
0.999999E-02	0.210741E 05	0.965216E-02	0.572741E 04	0.400325E 04	0.776891E 00	0.120920E 01
0.120000E-01	0.210569E 05	0.132020E-01	0.572661E 04	0.400771E 04	0.777812E 00	0.120920E 01
0.160200E-01	0.210101E 05	0.247285E-01	0.572440E 04	0.401989E 04	0.780328E 00	0.120920E 01
0.200700E-01	0.209458E 05	0.386679E-01	0.571713E 04	0.403660E 04	0.783778E 00	0.120920E 01
0.240000E-01	0.208629E 05	0.557360E-01	0.571744E 04	0.405906E 04	0.788215E 00	0.120920E 01
0.280000E-01	0.207604E 05	0.759524E-01	0.571257E 04	0.408440E 04	0.793708E 00	0.120920E 01
0.320000E-01	0.206368E 05	0.993406E-01	0.570675E 04	0.411647E 04	0.800314E 00	0.120920E 01
0.360000E-01	0.204904E 05	0.125927E 00	0.569965E 04	0.415409E 04	0.808125E 00	0.120920E 01
0.400000E-01	0.203192E 05	0.155743E 00	0.569130E 04	0.419798E 04	0.817257E 00	0.120920E 01
0.440000E-01	0.201205E 05	0.189820E 00	0.568171E 04	0.424871E 04	0.827837E 00	0.120920E 01
0.480000E-01	0.198911E 05	0.225194E 00	0.567045E 04	0.430703E 04	0.840033E 00	0.120920E 01
0.520000E-01	0.196270E 05	0.264899E 00	0.565736E 04	0.437391E 04	0.854063E 00	0.120920E 01
0.55999E-01	0.193234E 05	0.307969E 00	0.564212E 04	0.445044E 04	0.870180E 00	0.120920E 01
0.599999E-01	0.189742E 05	0.354437E 00	0.562435E 04	0.453805E 04	0.888712E 00	0.120920E 01
0.639999E-01	0.195721E 05	0.404324E 00	0.560354E 04	0.463855E 04	0.910076E 00	0.120920E 01
0.679999E-01	0.181076E 05	0.457639E 00	0.557904E 04	0.475416E 04	0.934806E 00	0.120920E 01
0.719999E-01	0.175692E 05	0.514369E 00	0.554998E 04	0.488774E 04	0.963583E 00	0.120920E 01
0.75999E-01	0.169420E 05	0.574464E 00	0.551519E 04	0.504303E 04	0.997330E 00	0.120920E 01
0.79999E-01	0.162072E 05	0.637811E 00	0.547304E 04	0.522495E 04	0.103728E 01	0.120920E 01
0.83999E-01	0.153411E 05	0.704205E 00	0.542179E 04	0.544004E 04	0.108512E 01	0.120920E 01
0.87999E-01	0.142311E 05	0.773289E 00	0.535622E 04	0.569737E 04	0.114329E 01	0.120920E 01
0.89999E-01	0.140245E 05	0.790918E 00	0.533791E 04	0.576949E 04	0.115983E 01	0.120920E 01
0.90999E-01	0.137208E 05	0.809015E 00	0.531739E 04	0.584917E 04	0.117362E 01	0.137920E 01
0.90499E-01	0.135546E 05	0.818571E 00	0.529003E 04	0.588917E 04	0.114329E 01	0.137920E 01
0.90493E-01	0.134711E 05	0.823302E 00	0.526803E 04	0.590932E 04	0.114817E 01	0.137920E 01
0.909999E-01	0.133867E 05	0.828034E 00	0.524603E 04	0.592969E 04	0.115313E 01	0.137920E 01
0.912493E-01	0.133014E 05	0.832766E 00	0.522398E 04	0.595030E 04	0.115815E 01	0.137920E 01
0.914993E-01	0.132150E 05	0.837510E 00	0.520190E 04	0.597120E 04	0.116326E 01	0.137920E 01
0.91999E-01	0.130394E 05	0.847013E 00	0.51763E 04	0.601378E 04	0.117371E 01	0.137920E 01
0.92499E-01	0.128594E 05	0.856550E 00	0.515322E 04	0.605754E 04	0.118452E 01	0.137920E 01
0.92999E-01	0.126750E 05	0.866111E 00	0.512865E 04	0.610250E 04	0.119568E 01	0.137920E 01
0.93499E-01	0.124862E 05	0.875694E 00	0.510392E 04	0.614868E 04	0.120722E 01	0.137920E 01
0.94499E-01	0.120949E 05	0.894908E 00	0.513394E 04	0.624490E 04	0.123149E 01	0.137920E 01
0.95499E-01	0.116844E 05	0.914170E 00	0.512323E 04	0.634667E 04	0.125751E 01	0.137920E 01
0.96499E-01	0.112539E 05	0.933447E 00	0.511170E 04	0.645443E 04	0.128548E 01	0.137920E 01
0.97499E-01	0.108024E 05	0.952709E 00	0.509925E 04	0.656974E 04	0.131563E 01	0.137920E 01
0.99499E-01	0.983281E 04	0.991020E 00	0.507125E 04	0.681940E 04	0.138961E 01	0.137920E 01
0.101400E 00	0.876979E 04	0.102872E 01	0.503802E 04	0.710436E 04	0.146427E 01	0.137920E 01
THROAT WALL						
0.999724E-01	0.958939E 04	0.100000E 01	0.106379E 04	0.68831E 04	0.140158E 01	0.137920E 01

# PERFORMANCE

THROAT ISPVAC,LBF-SEC/LBM CSTAR,FT/SEC  
0.289113E 03 0.755629E 04

THROAT ISPVID,LBF-SEC/LBM CSTID,FT/SEC  
0.286263E 03 0.738404E 04

MD,LBF-SEC/FT MVID,LBF-SEC/FT  
0.125000E 00 0.127916E 00

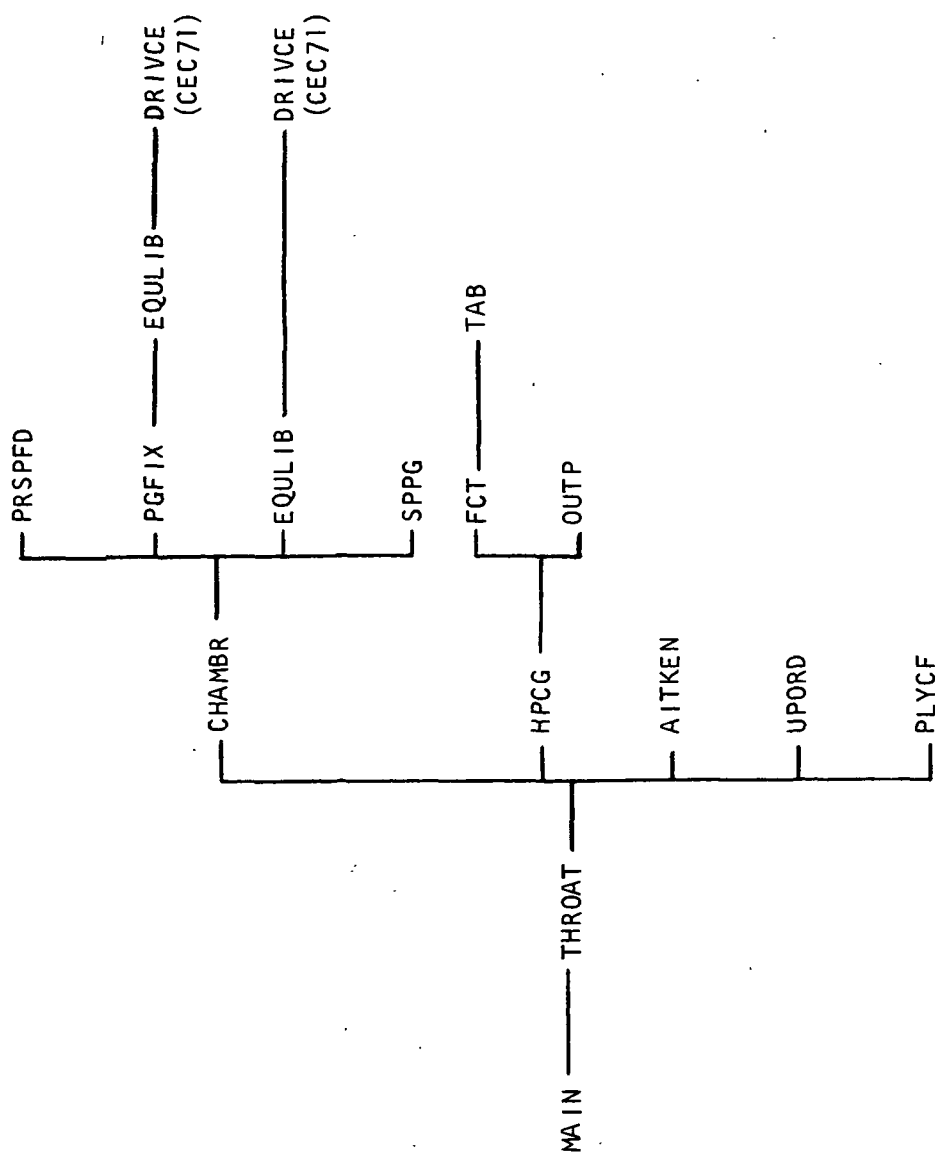
CD,DISCHARGE COEFFICIENT= 0.977205E 00

THROAT ISPVAC/ISPVID= 0.100095E 01

CSTAR/CSTID= 0.102333E 01



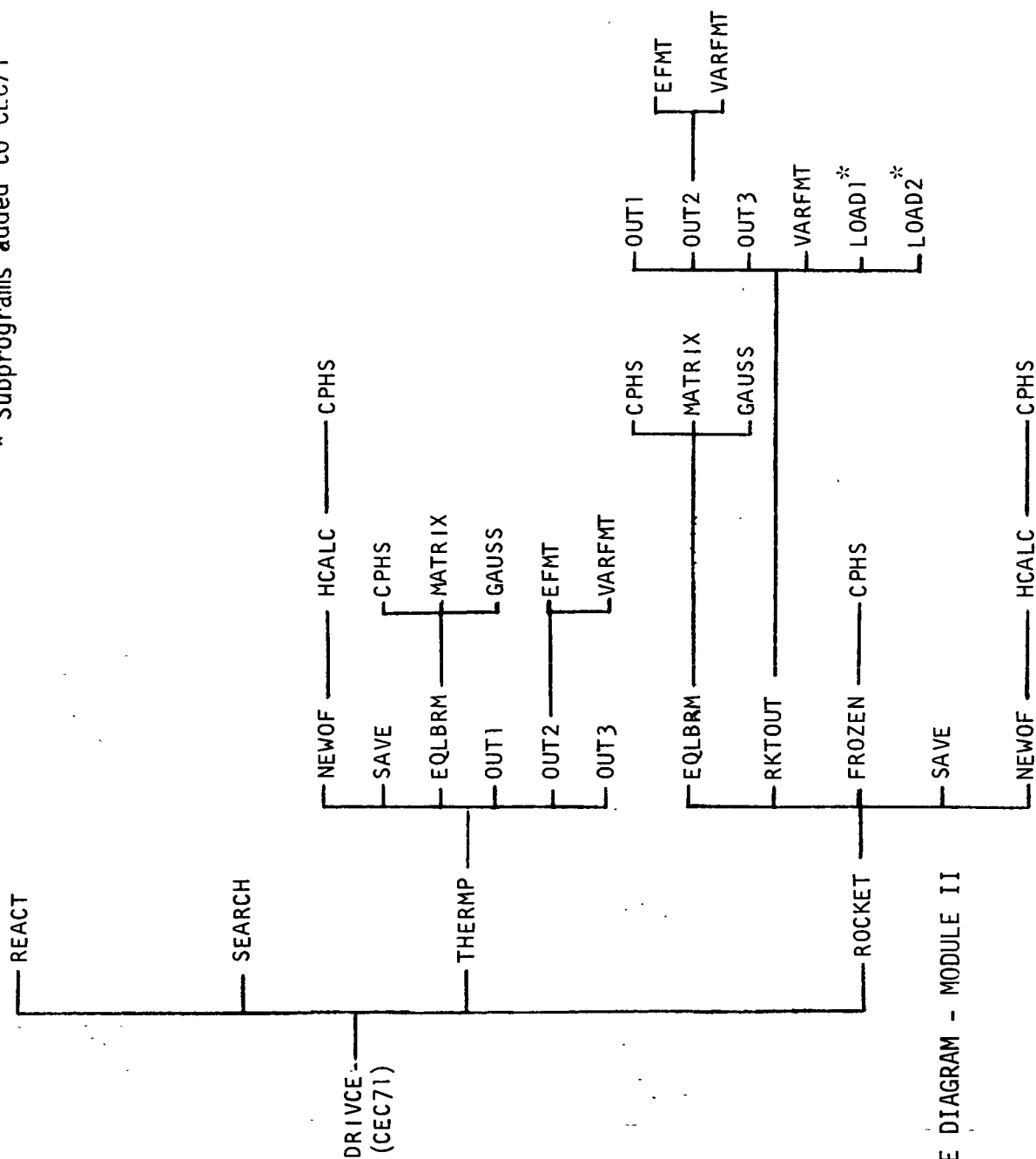
# APPENDIX G



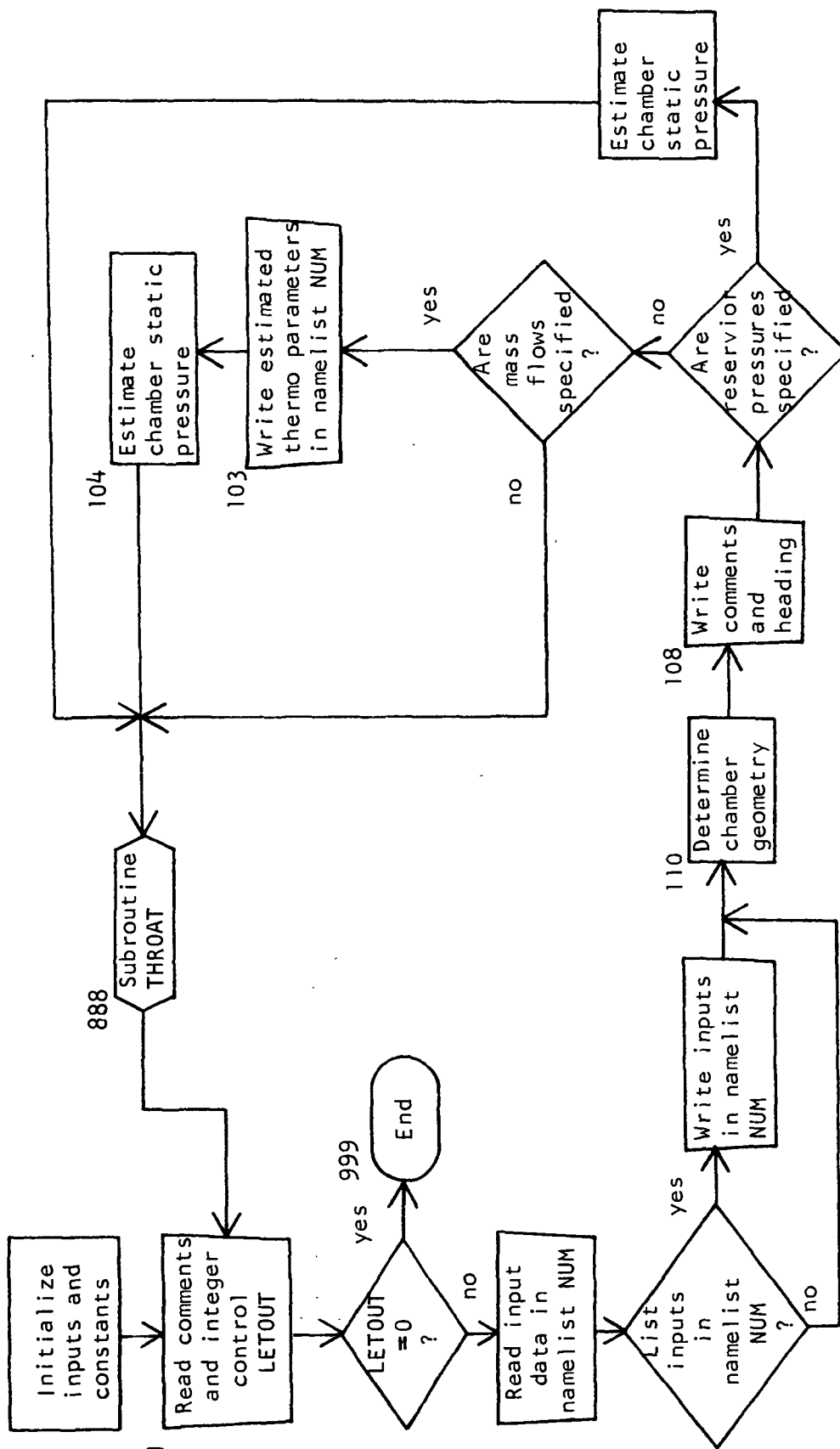
ROUTINE TREE DIAGRAMS - MODULE I

# APPENDIX G (Continued)

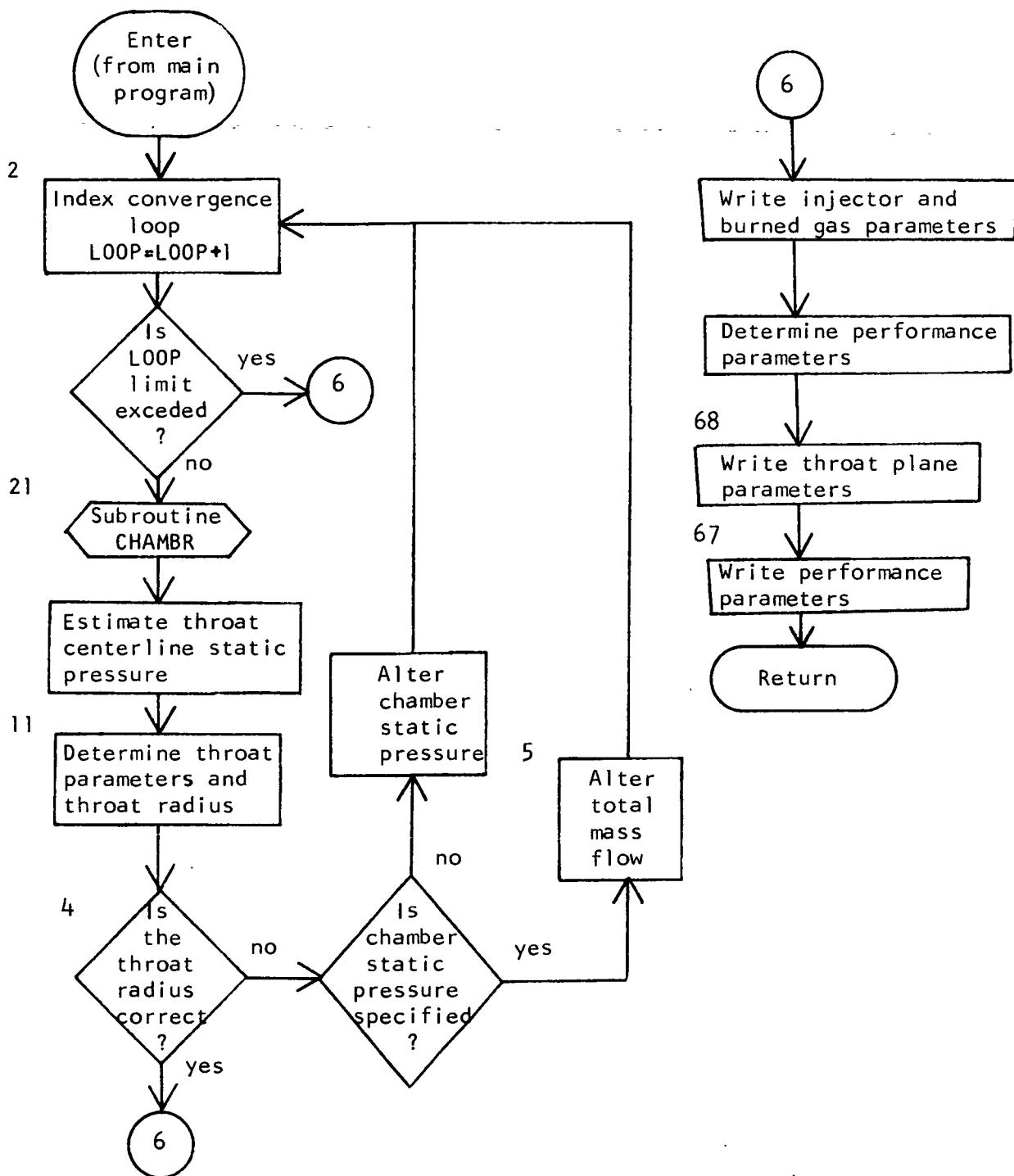
\* Subprograms added to CEC71



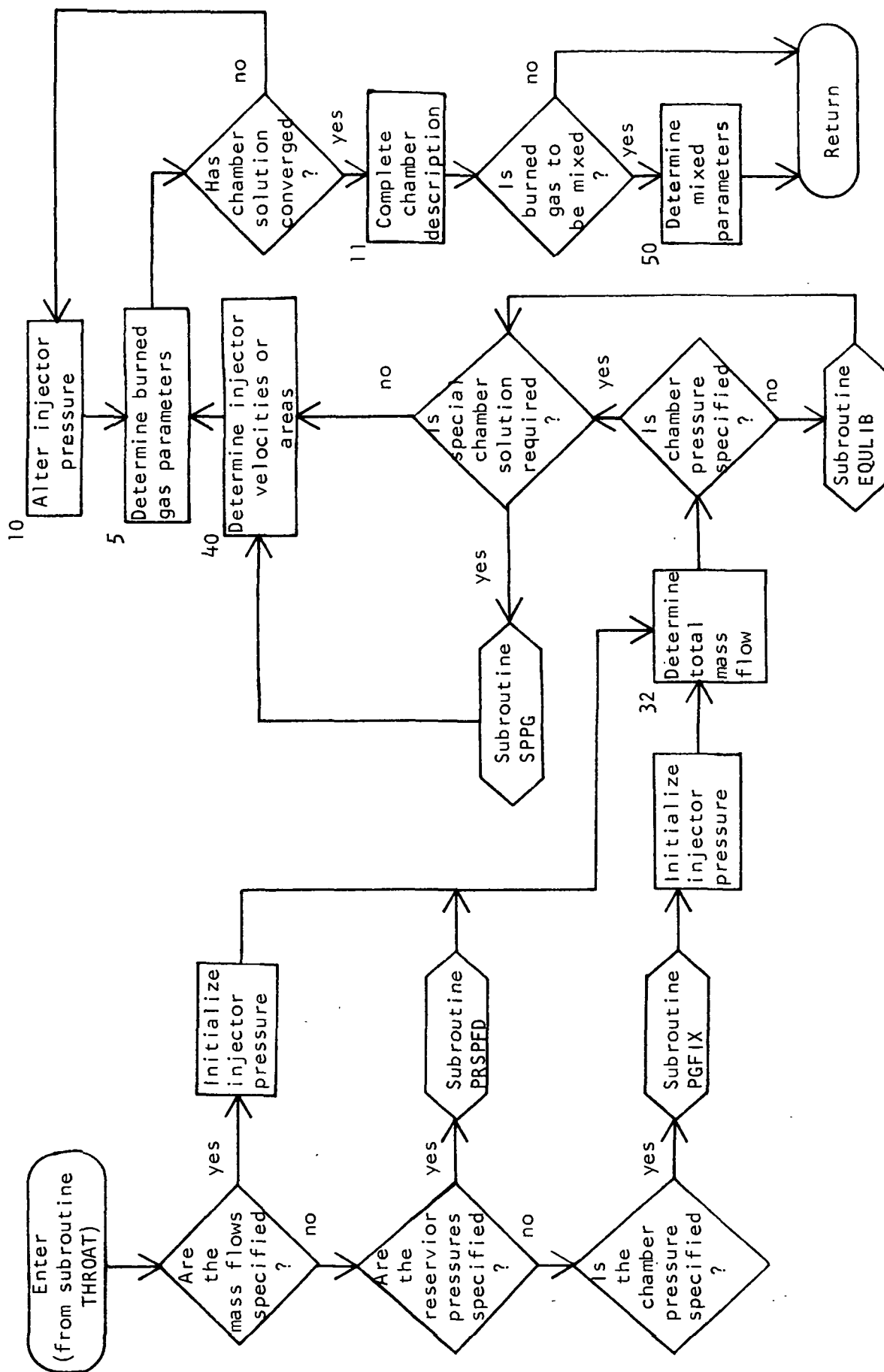
ROUTINE TREE DIAGRAM - MODULE II



Flow diagram for main routine



Flow diagram for subroutine THROAT



Flow diagram for subroutine CHAMBR

## REFERENCES

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TABLE I - PROGRAM INPUT FOR  
PRESELECTED THERMOCHEMICAL  
INPUT DATA

Comment  
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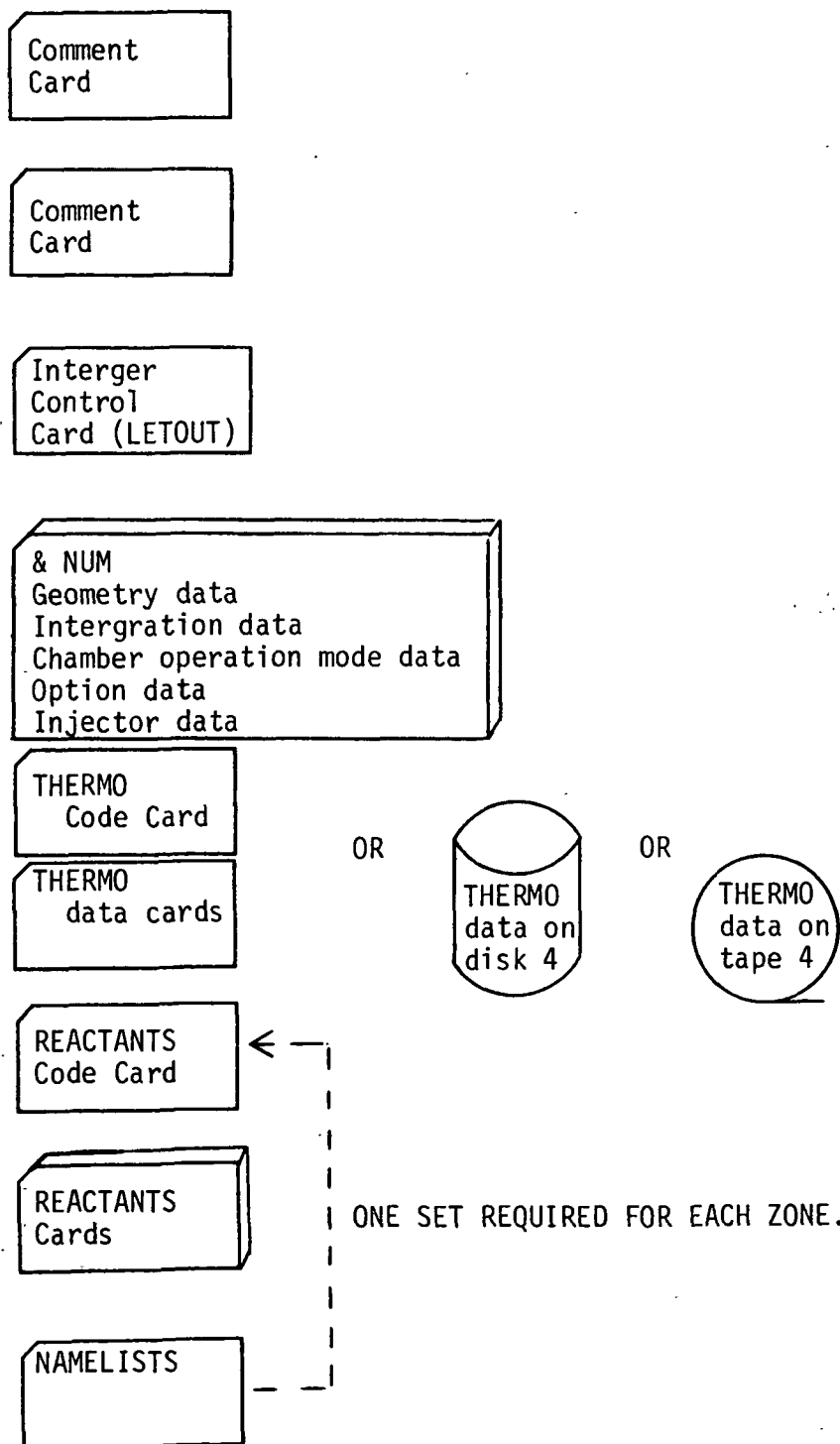
Comment  
Card

Integer  
Control  
Card (LETOUT)

& NUM  
Geometry data  
Integration data  
Chamber operation mode data  
or mass generation data  
Option data  
Injector data  
Initial estimations data  
for variable chamber pressure

& EQU  
TOG  
GAMG  
MWG  
NCHANG

TABLE II - PROGRAM INPUT FOR  
INTERNALLY GENERATED THERMOCHEMICAL DATA





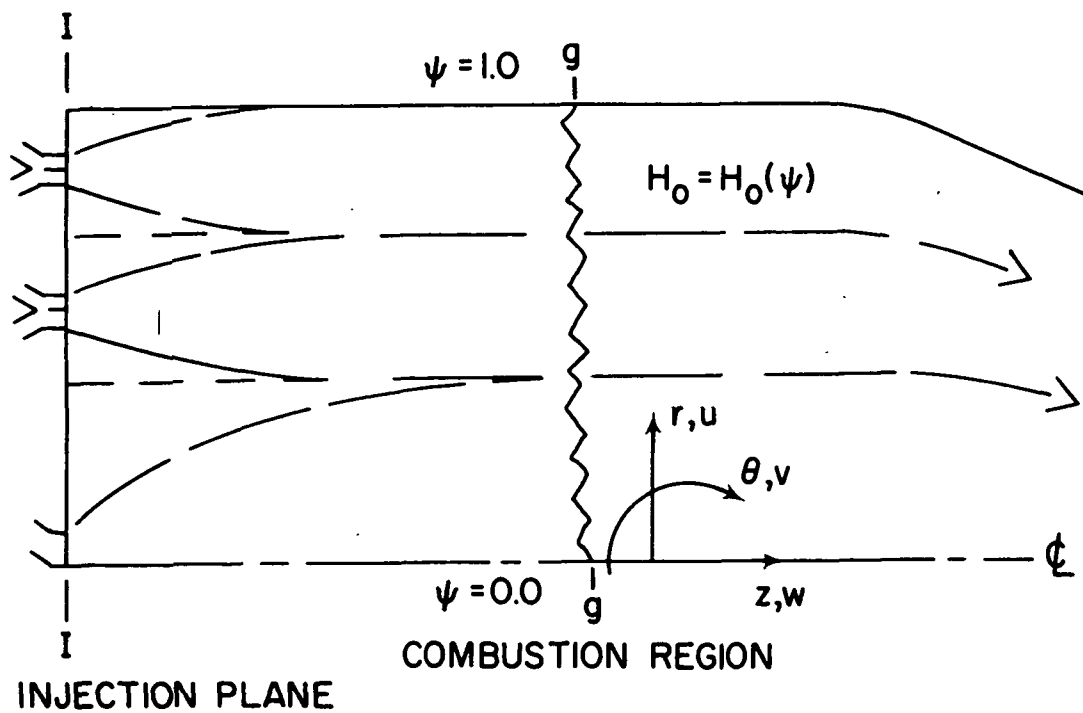


Figure 1a. Schematic of Nozzle Chamber.

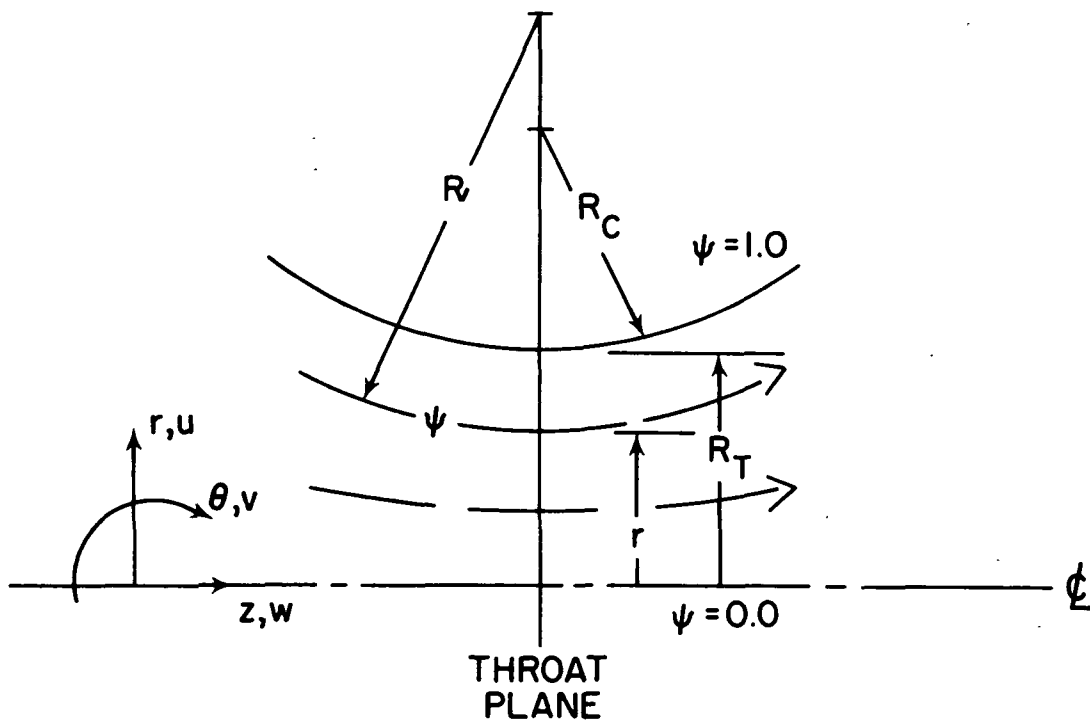


Figure 1b. Schematic of Nozzle Throat.

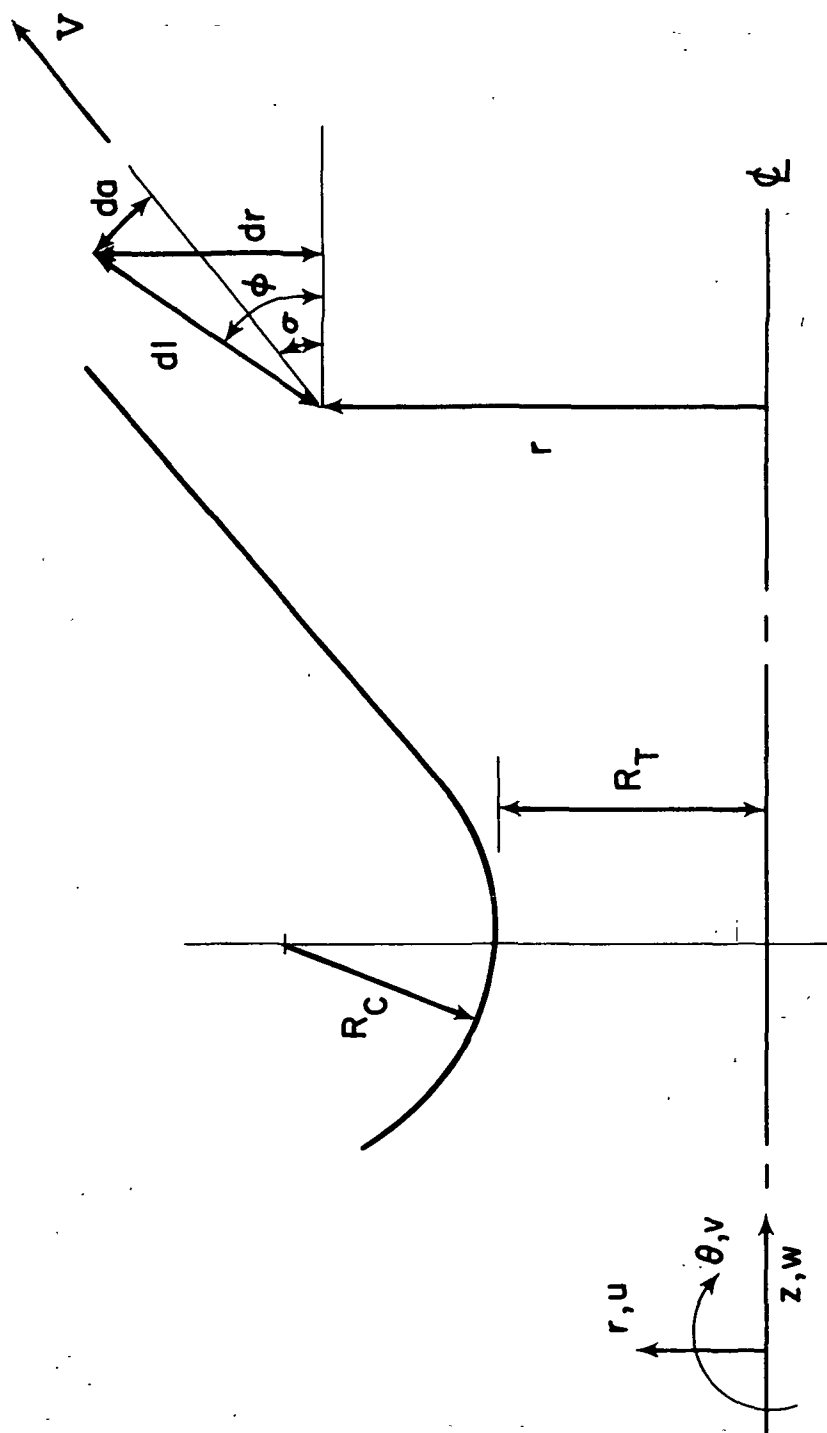


Figure 2. Schematic of Axisymmetric Nozzle for Derivation of Mass Flow.

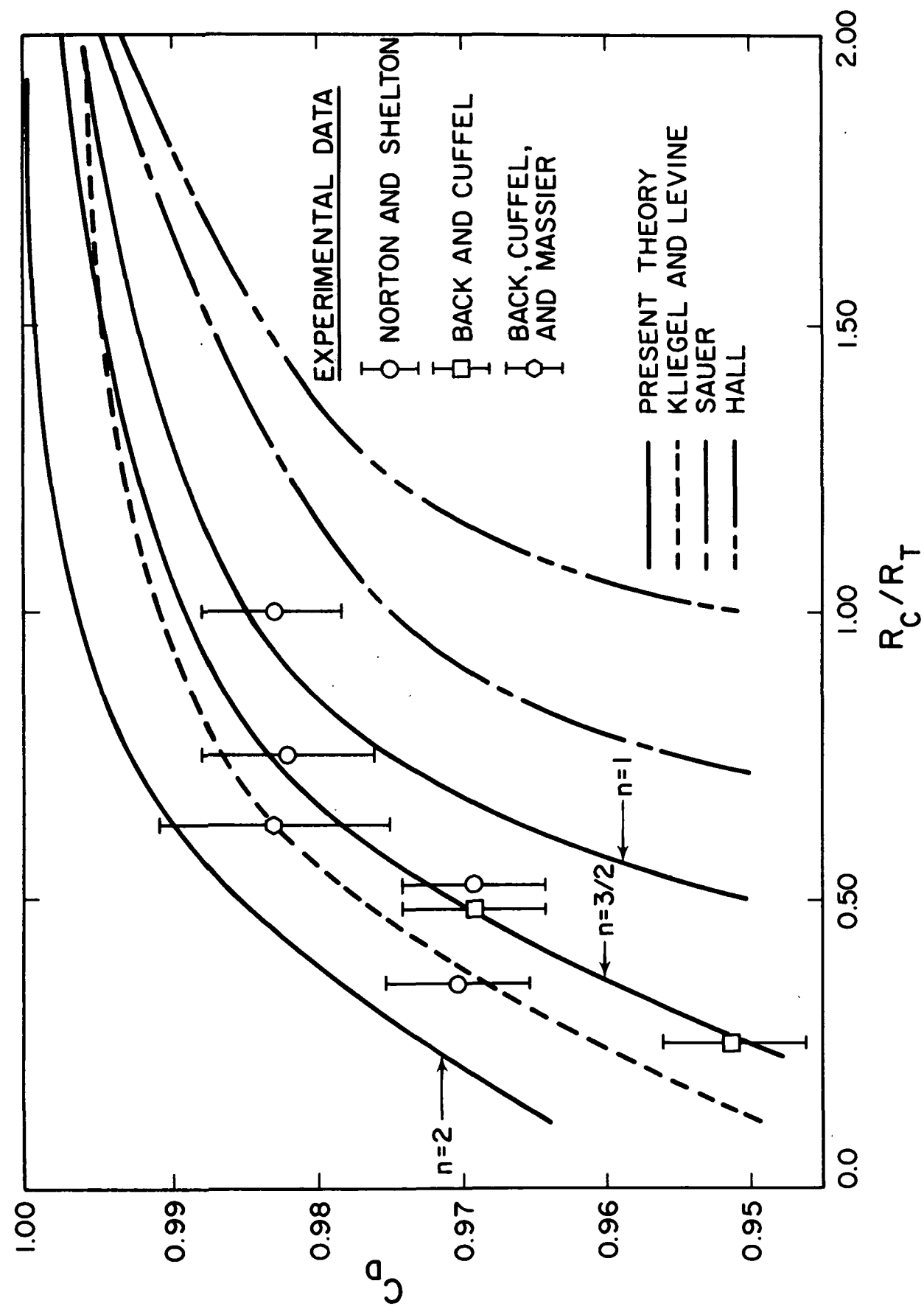


Figure 3. Discharge Coefficient Comparison Between Experimental and Analytical Results.

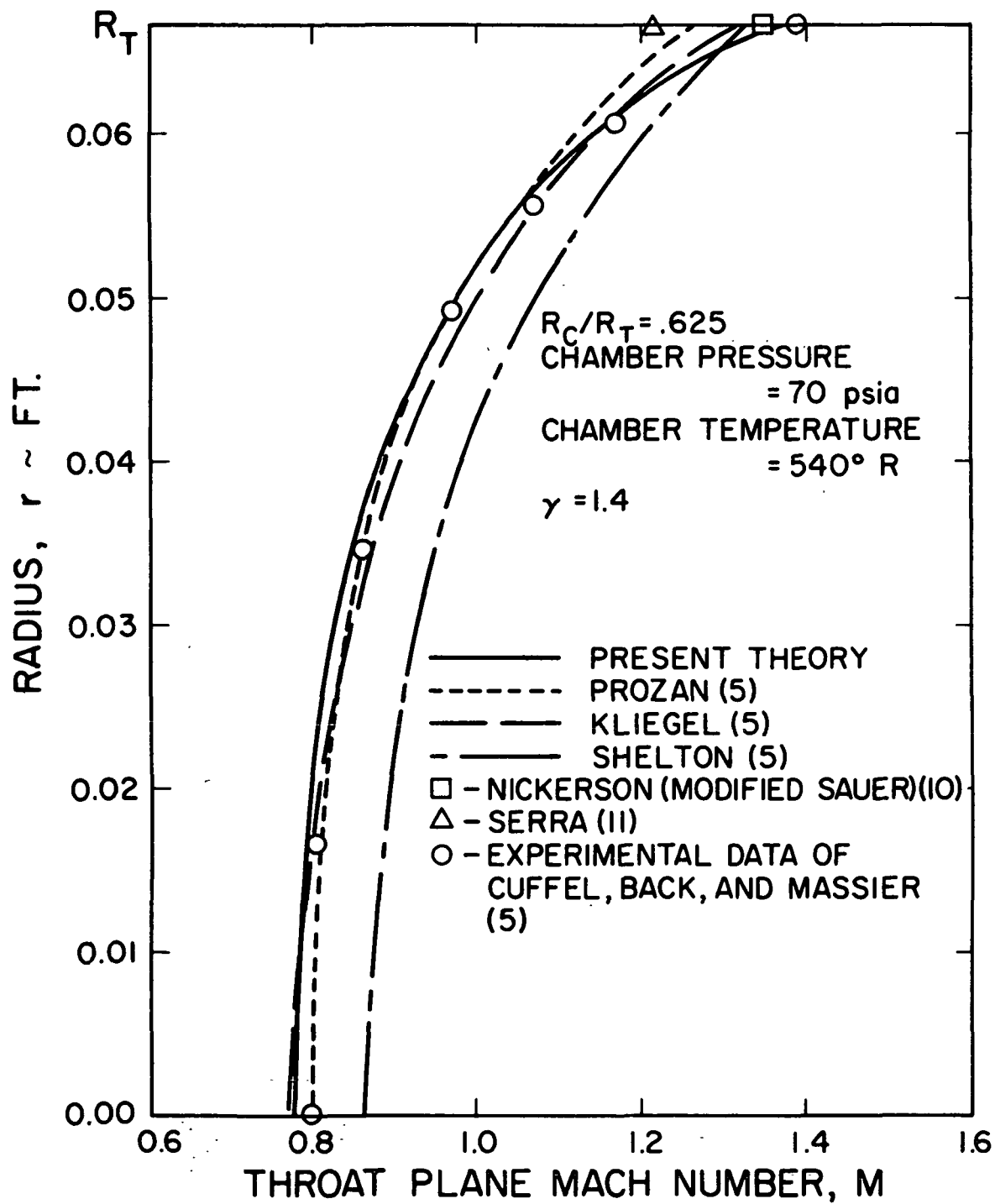


Figure 4. Throat Plane Mach Number Distribution Comparison Between Experimental and Analytical Results.

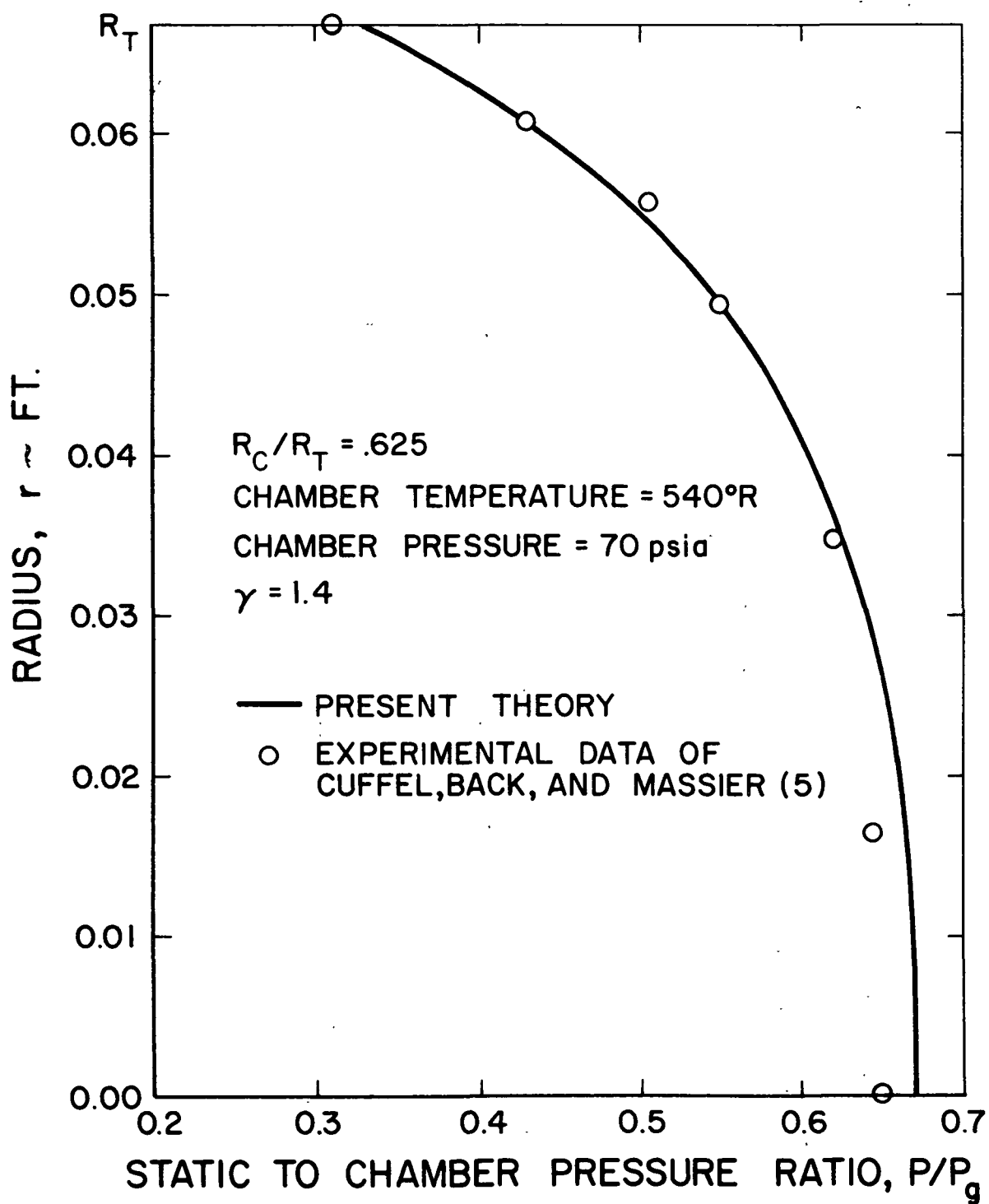


Figure 5. Throat Plane Pressure Ratio Distribution Comparison Between Experimental and Analytical Results.

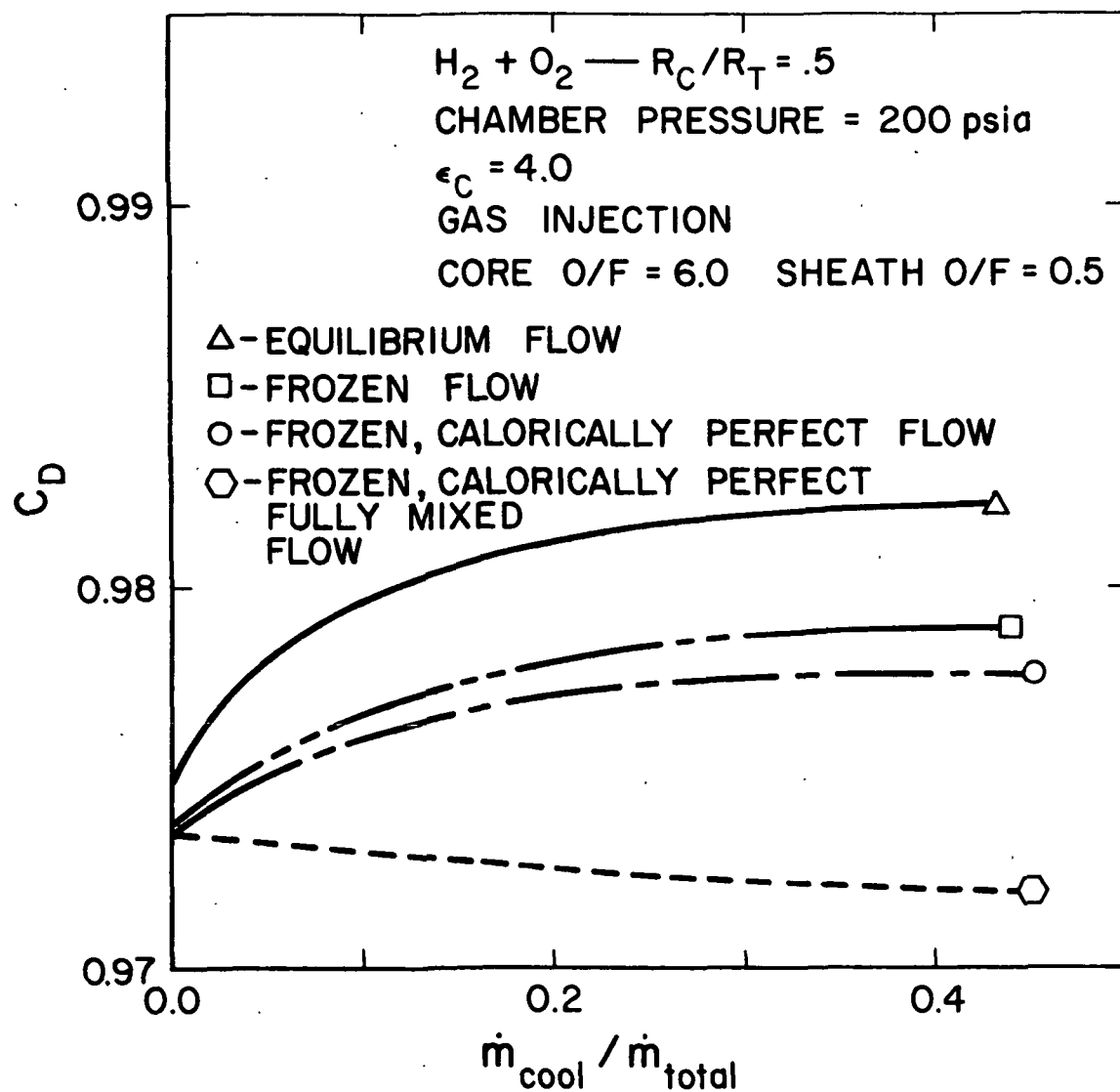


Figure 6. Variation of Discharge Coefficient with Cooling Mass Ratio for  $R_C/R_T = 0.5$ .

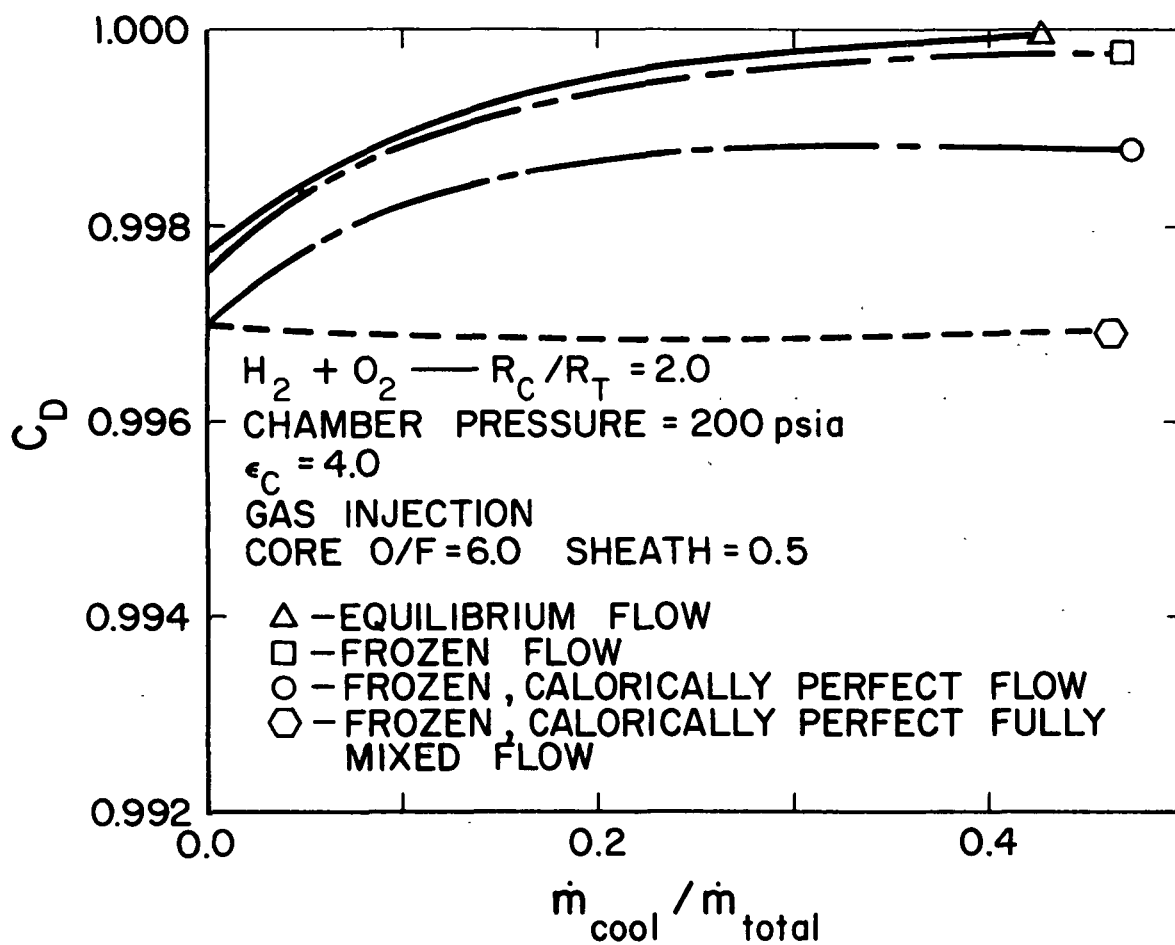


Figure 7. Variation of Discharge Coefficient with Cooling Mass Ratio for  $R_c/R_T = 2.0$ .

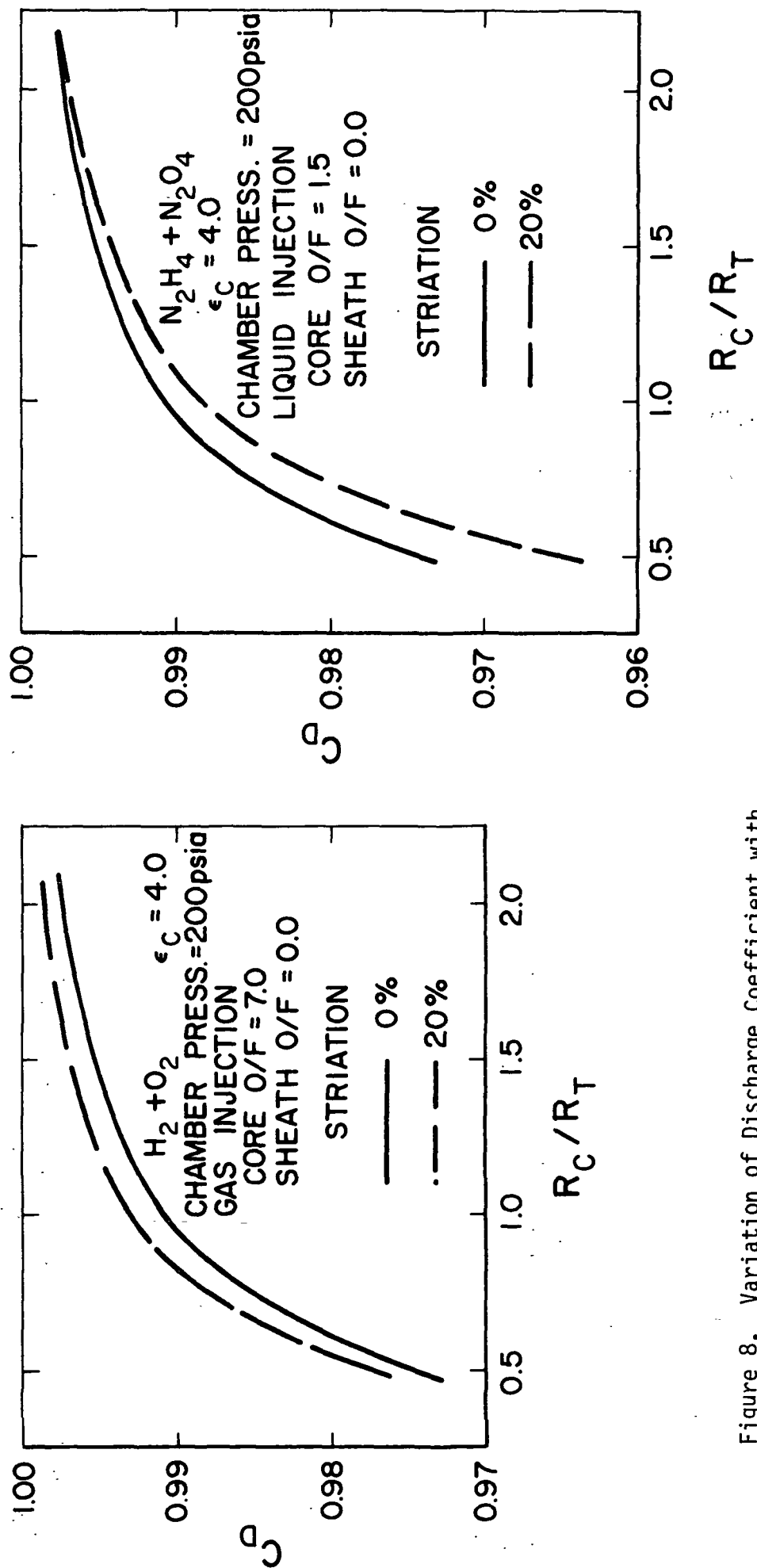


Figure 8. Variation of Discharge Coefficient with  $R_C/R_T$  for Striated and Unstriated Flow Using Different Propellants.



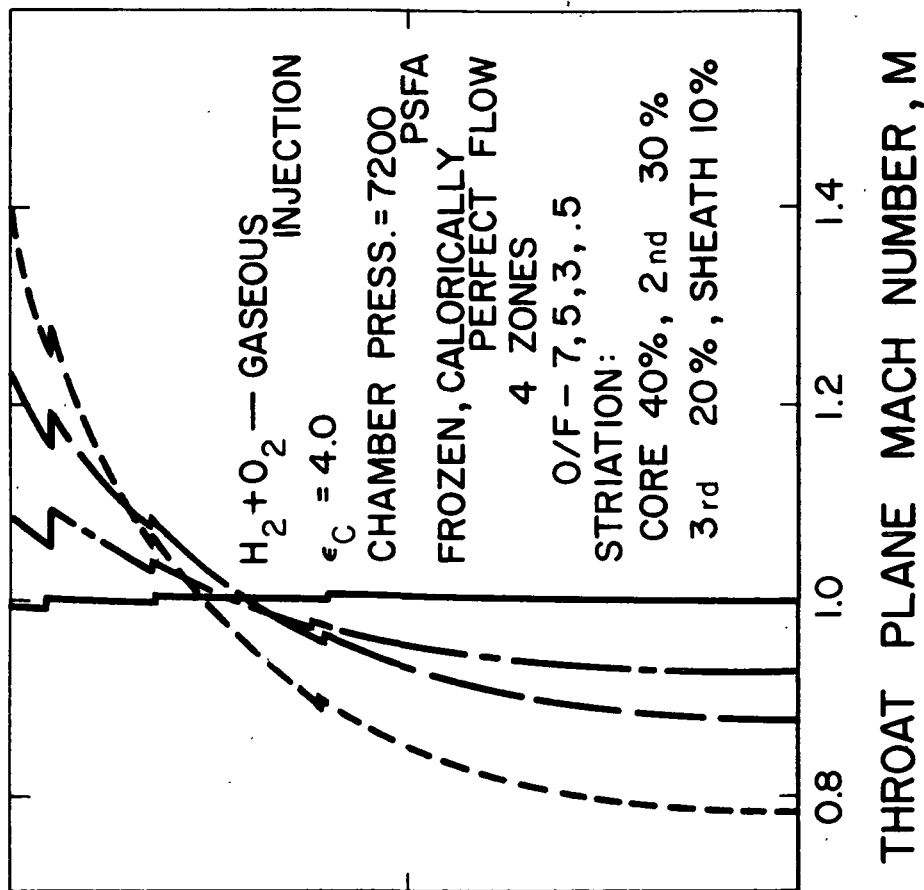
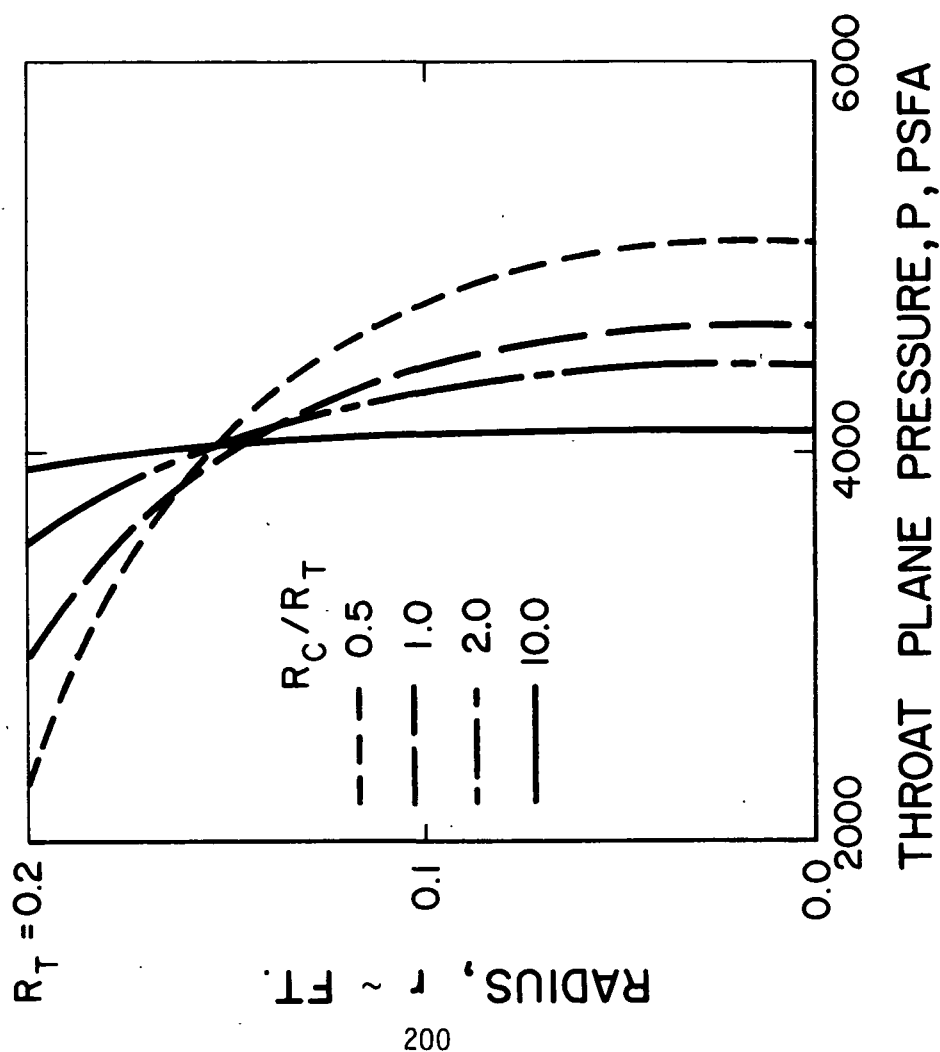


Figure 9. Variation of Throat Plane Pressure and Mach Number with  $R_C/R_T$  for Four Zone Flow.

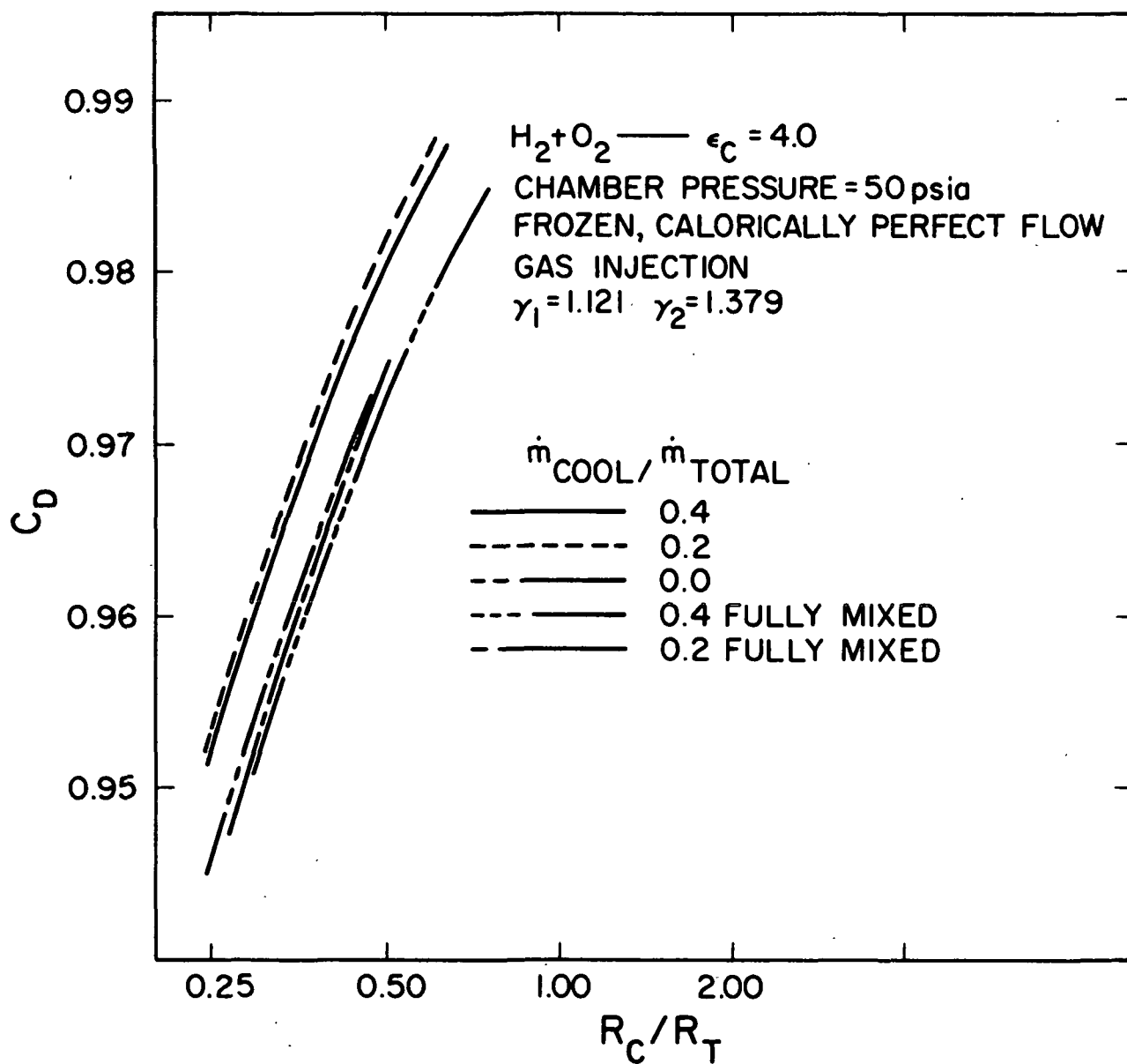


Figure 10. Discharge Coefficient for Low  $R_C/R_T$  with Various Amounts of Cooling Mass Flow.

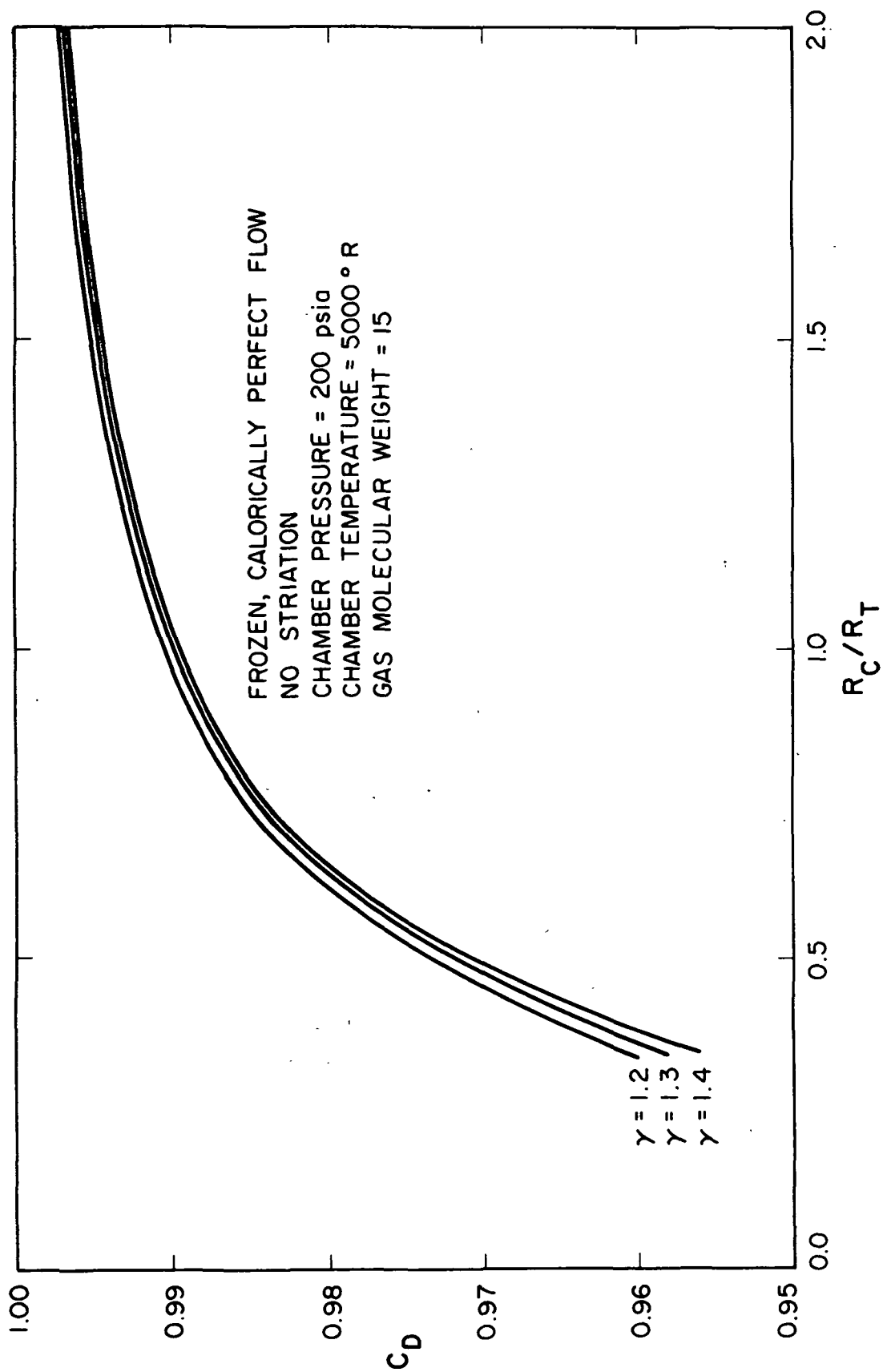


Figure 11. Discharge Coefficient for Ratio of Specific Heats = 1.2, 1.3, and 1.4.

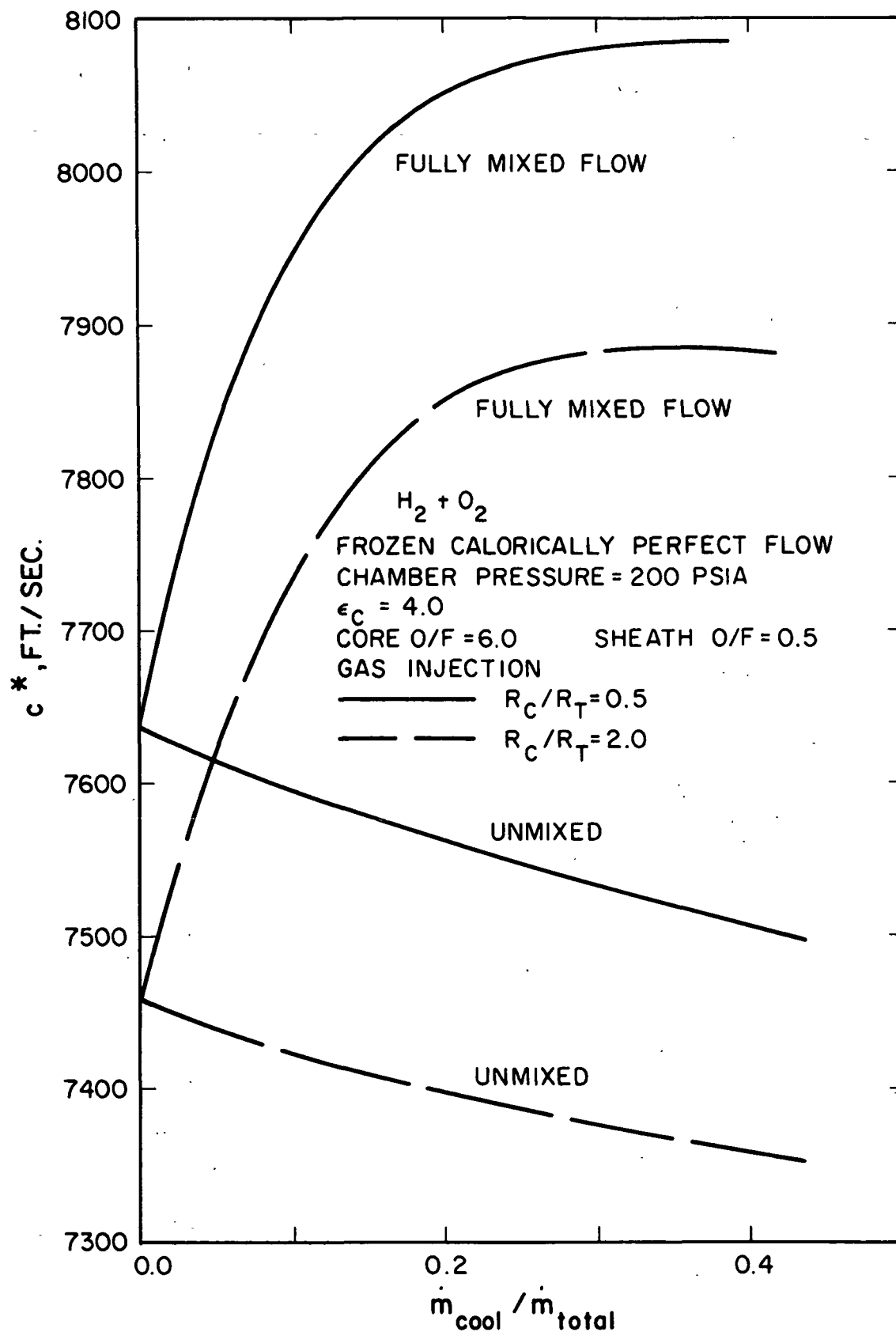


Figure 12: Characteristic Velocity For Mixed and Unmixed Flow With Chamber Static Pressure Fixed.

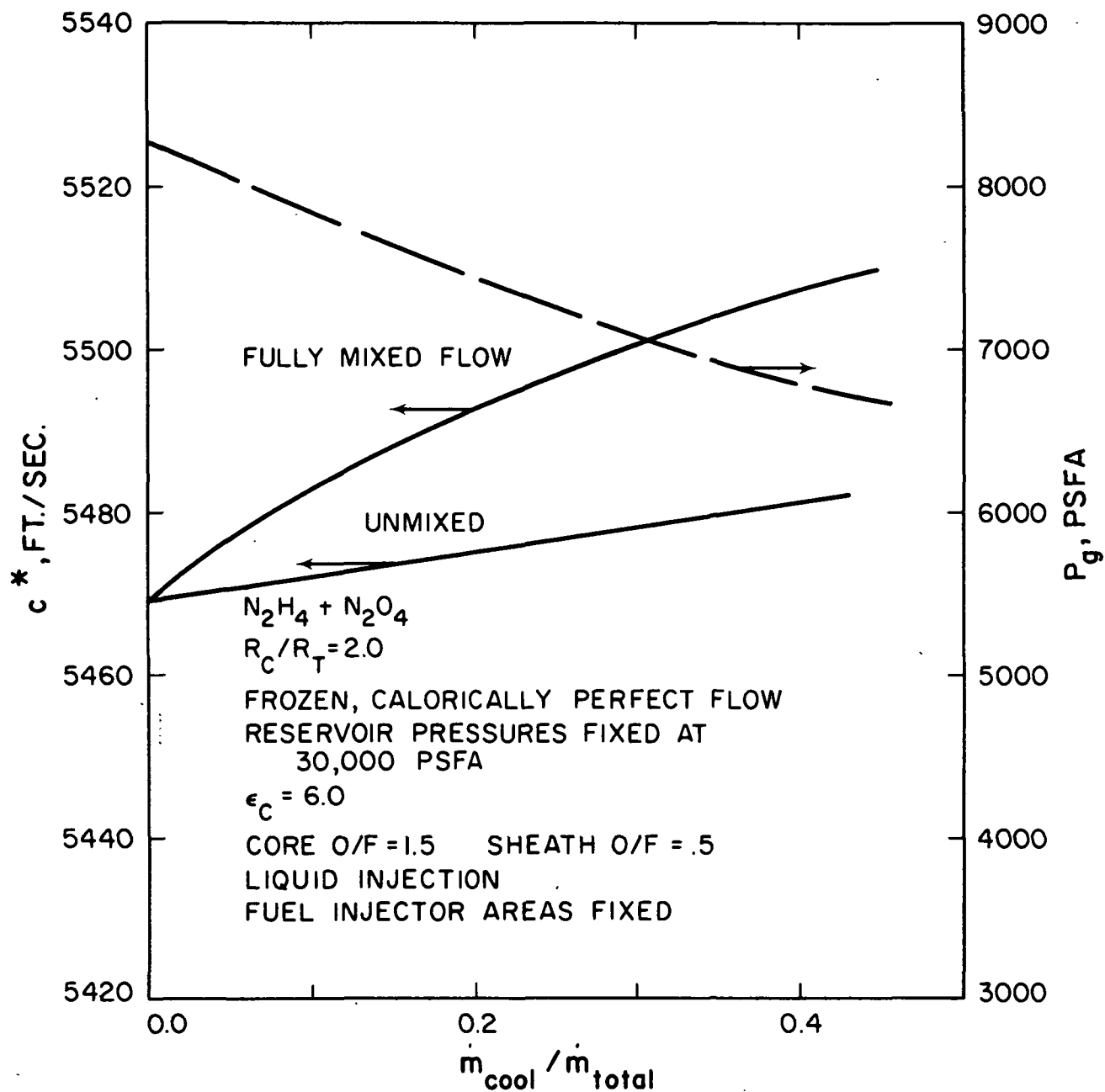


Figure 13. Characteristic Velocity For Mixed and Unmixed Flow With Reservoir Pressures Fixed.